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Design and Operation of a 1000°C Lithium-Cesium Test System

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PREFACE

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ABSTRACT

A 100 kWt cesium-lithium test loop was fabricated of niobium-1% zirconium for experiments on erosion and two-phase system operation at temperatures of 980°C and velocities of 150 m/s. Although operated at design temperature for 100 hours, flow instabilities in the two-phase separator interfered with the achievement of the desired mass flow rates. A modified separator was fabricated and installed in the loop to alleviate this problem. Because of program cancellation, the test system has been placed in standby condition for storage. This report documents the test system.

I INTRODUCTION

Power generation for advanced space missions and central station power by a liquid metal magnetohydrodynamic cycle has been studied extensively (Refs. 1-4). A promising system for power levels above about 100 kWe is based on the two-component separator cycle using lithium and cesium as working fluids (Refs. 5 and 6). Cesium is mixed with lithium at high temperature at the inlet of a nozzle as shown in Fig. 1. The cesium vaporizes and the mixture is accelerated in the nozzle to high velocity. Impingement on an inclined surface produces a low-void fraction stream that is predominantly liquid lithium. This stream is decelerated in an MHD generator, producing electric power, and is subsequently returned by its remaining kinetic energy through the heat source to the nozzle inlet. The other flow leaving the separator is a high-void fraction stream that consists of cesium vapor with carryover of liquid and vaporous lithium. This mixture is condensed and returned by a pump to the nozzle inlet.

The characteristics of this system have been partially determined by analysis (Ref. 6), by component experiments using ambient water-nitrogen, NaK, and NaK-nitrogen mixtures (Refs. 7 and 8), in system experiments with water-nitrogen and NaK-nitrogen mixtures (Ref. 8), and through high-temperature, corrosion-erosion experiments with lithium (Refs. 9 and 10). However, information on the following subjects requires testing with cesium and lithium at the peak system temperatures:

- (1) Erosion of surfaces by lithium impingement at the design velocity of 150 m/s.
- (2) Performance of a two-phase nozzle with a cesium-lithium mixture.
- (3) Condensation characteristics of cesium-lithium mixtures.

(4) Nonequilibrium behavior of cesium-lithium flows where solution or dissolution are occurring.

In order to investigate these subjects a flow system was fabricated from niobium-1% zirconium alloy to operate with cesium-lithium at a peak temperature of 980°C. Erosion can be determined by measuring the depth of attack or deposit on a wedge with an optically flat surface which was located in the flow stream at the nozzle exit. Nozzle performance can be derived from the measured thrust produced by the flow on a target cone which was designed to turn the flow by 90 deg. Cesium condensation coefficients can be determined by measurements on the NaK-cooled compact condenser. Nonequilibrium behavior would be inferred by deviations from the thermodynamic cycle calculations.

The test system was operated with simultaneous cesium and lithium flow at the design temperature of 980°C for about 100 hours. Figure 2 is a photograph of operation at high temperature and low flow rates. Flow instability prevented attainment of the design mass flow rates and impingement velocities. Modifications to the separator component to eliminate the instability were nearly completed when the NASA liquid metal MHD project was cancelled. The test system has been placed in a standby condition pending further investigations oriented toward commercial power generation.

Appendixes A, B, C, and D present, respectively, loop operating procedures, test system schematics, fabrication drawings of the test system, and loop operating characteristics.

II. DESCRIPTION OF TEST SYSTEM

The two-component liquid metal MHD system being studied and the Cs-Li test system are most closely related to the Rankine cycle. The flow paths and processes can be illustrated by reference to Fig. 3, which is a schematic of the liquid metal circuits of the test system. Lithium is heated to the maximum temperature in the heater component and flows to the nozzle, where it is injected at point 1.

Cesium liquid is also injected in the nozzle at point 2. Part of the cesium vaporizes and the remainder goes into solution with the lithium, which remains mostly in the liquid state. The cesium vapor is accelerated

to high velocity and low pressure in the nozzle. As the pressure decreases, more cesium comes out of solution and vaporizes. Shear and pressure forces resulting from the expanding cesium vapor cause breakup and acceleration of the lithium droplets to high velocity. The mixture impinges on the target and on a mesh separator within the receiver component. The lithium pump increases the pressure to the maximum of the cycle and returns the flow to the heater. The cesium vapor leaves the receiver vessel and flows to the desuperheater. Subcooled liquid cesium is injected at that point to reduce the cesium vapor (which is highly superheated) to the saturated state. The vapor then enters the condenser, where the heat of vaporization is removed by flowing NaK, is condensed, and returns to the cesium pump. The pump pressurizes the cesium and returns it to the nozzle and through a cooler to the desuperheater.

Figure 4 is a photograph of the cesium and lithium circuits prior to testing. All components and piping were fabricated from Nb-1%Zr. All weldments were performed in a high-purity argon atmosphere. This part of the test system was mounted on the door of a getter-ion pumped vacuum chamber which was operated in the 10⁻⁷ torr range to protect the refractory metals from oxidation during high-temperature operation. Description of the test system components and their performance is summarized below.

A. Two-Phase Nozzle

The two-phase nozzle for the test system was designed to provide cesium and lithium flow over a range of conditions. The design pressure gradient was established from the pressure variation measured on a larger nozzle, using water-nitrogen and freon-water flows. This gradient was used in the two-phase, two-component nozzle program to calculate the contour. The resulting geometry is summarized in Fig. 5. Figure 6 is a photograph of the nozzle prior to final welding.

The nozzle was calibrated with water and nitrogen to compare the exit velocity with that calculated by the computer program. The test setup is given in Fig. 7. As shown in Fig. 8, the agreement between the calculated and measured exit velocity was quite good. The computer program was then used to calculate the nozzle flow rates as a function of inlet temperature and mass ratio with the result shown in Fig. 9. At saturated Cs vapor conditions at the inlet, there is a unique relation between the cesium and

lithium flow rates. The information from Fig. 9 was used to determine the flow rates and operating conditions of the test system for the desired values of mass ratio and nozzle inlet temperature.

B. Thrust Target and Separator

The relation of the nozzle and thrust target is given by Fig. 10. The two-phase lithium-cesium flow impinging on the thrust target is turned by 90 deg. The thrust produced is transmitted through a stainless-steel beliows which is joined to the Nb-1%Zr alloy by a coextruded joint. The measured thrust thus provides an indication of the nozzle exit velocity. The separated lithium falls to the bottom of the separator and is returned to the lithium pump. The cesium vapor is separated from the lithium by a mesh-type separator and flows to the desuperheater.

The thrust target with the erosion specimen mounted in place is shown in Figs. 11 and 12. The erosion specimen is an optically flat wedge which extends beyond the nozzle exit diameter. Erosion depth was to have been measured with a traversing microscope as was done on a previous test (Ref. 10). The basic wedge is Nb-1%Zr alloy; the insert, which was electron-beam-welded to the Nb-1%Zr, is T-111 alloy.

Figure 13 shows the thrust target mounted in the separator body. The Nb-1%Zr mesh was wrapped on the outside of the perforated annulus as shown in the assembly drawing of Fig. 14.

The entire unit was assembled and tested with water-nitrogen flows. The thrust measured by the thrust target agreed to within ±5% with the values measured for the nozzle alone. The nozzle exit velocity was varied from 90 to 155 m/s for these measurements. Liquid carryover in the gas exit ranged from 2-7% of the primary liquid flowrate, acceptable values for the high-temperature flow system. Complete separation of gas from the liquid outlet flow was made possible by adding baffles, as shown in Fig. 15. However, these same baffles resulted in excessive lithium holdup during the lithium-cesium tests.

In order to eliminate this holdup problem a cyclone separator was designed for the lithium-cesium test system. A model was tested (Fig. 16) with water and nitrogen with a liquid carryover in the gas outlet of less than

0.1% and gas-free flow at the liquid outlet. Figure 17 shows the cyclone separator fabricated of Nb-1%Zr ready for installation in the test system.

C. Lithium Pump

The lithium pump is a helical induction electromagnetic pump. The pumping element shown in Fig. 18 is a Nb-1%Zr structure that fits within a stainless-steel, thermally-insulated sleeve. The electromagnetic body forces are supplied through the stainless-steel sleeve by an air-cooled, three-phase motor stator shown in Fig. 19. The pump was operated for more than 1000 h at temperatures exceeding 1000°C and for more than 4000 h above 650°C.

The calculated performance curve is given in Fig. 20. Previous tests with lithium flow nozzles at 1100°C gave measured performance data which agreed quite closely with the calculated performance (Ref. 9). A serious limitation of the pump which became apparent during the testing was the tendency of vapor to accumulate within the pump body and cause flow oscillations. Extensive shakedown testing was required to evolve a startup procedure that minimized this problem. Although vapor accumulation was a problem, the pump was able to operate with a negative suction head. The most successful two-phase startup procedure consisted of injecting cesium while the pump operated with lithium flow at 980°C and zero pressure at the inlet.

D. Lithium Heater

The heater to raise the lithium to the maximum temperature of 980°C consisted of four "cal-rod" type elements welded in a Nb-1%Zr shell. Figures 21 and 22 are photographs of this unit before final welding. The heating elements are tantalum center conductors with beryllia insulation and swaged Nb-1%Zr sheaths. The beryllia was removed to a depth of 6 mm to enable the Nb-1%Zr sheaths to be TIG-welded to the Nb-1%Zr shell without degrading the ceramic insulation. As shown in Fig. 21, the body and elements are curved to provide flexibility to accommodate thermal stresses. The unit was operated for over 3000 h, heating lithium at temperatures ranging from 650-1000°C. After this time a small leak occurred at one of the sheath weldments. The leak was repaired and the unit was to have been used on succeeding tests. Electron-beam welding of the sheaths rather than TIG

welding would have enabled a greater depth of penetration, which probably would have eliminated this problem.

E. Lithium Flowmeter

The electromagnetic flowmeters used for the lithium and cesium are shown in Fig. 23. The calculated characteristics of the lithium flowmeter are given by Fig. 24. Calibration of this flowmeter with 1100°C lithium flow nozzles showed the measured flow to agree to within ±5% of the calculated values.

F. Cesium Pump

The cesium pump is of similar construction to the lithium pump. The stator is seen in Fig. 19, adjacent to the stator for the lithium pump. The flow was controllable with a throttling valve during the periods of operation at lower flow rates. Attempts to run the pump at higher pressure rise with a low inlet pressure and low flow rate resulted in excessive temperature rise and vaporization of the cesium at the pump inlet. A small jet pump was fabricated which should have eliminated this problem when installed.

G. Cesium Flowmeter

The cesium flowmeter of Fig. 23 was used only at very low flow rates. The calculated output curve is given in Fig. 25.

H. Cesium Desuperheater

The cesium vapor leaving the separator is highly superheated and has a very poor heat transfer coefficient. The desuperheater of Fig. 26 was designed to lower the temperature to saturated vapor conditions by injection of subcooled cesium liquid. The large surface area afforded by the small liquid metal droplets more than compensates for the poor coefficients.

An alternative method to desuperheat the Cs vapor is a heat exchanger with large internal surface area. A radiant heat exchanger with internal Nb-1%Zr fins was fabricated (Fig. 27) to replace the original desuperheater. This would enable the subcooled cesium bypass flow to be used for the cesium jet pump discussed previously.

I. Cesium Condenser

The condenser for the cesium was constructed of both Nb-1%Zr and stainless steel. The niobium alloy is required for the condensing cesium, while stainless steel is the material of construction for the NaK cooling system that rejects the latent heat of vaporization from the cesium.

The condenser assembly is shown in Fig. 28 before welding and in Fig. 29 after final assembly. The transition between the stainless-steel tees and center section and the niobium end pieces that weld to the Nb-1%Zr cesium tubing was achieved by brazing with a cobalt-nickel alloy. The condenser performed satisfactorily at the low Cs vapor flow rates tested.

J. NaK Heat Rejection Loop

The NaK heat rejection loop was constructed of type 316 stainless steel. NaK flow is produced by an electromagnetic AC conduction pump. The flow piping enters the vacuum chamber through a thermal sleeve. The entering NaK removes heat from the cesium subcooler and condenser and exits the vacuum chamber through another thermal sleeve. It flows through an expansion tank, heater, and air-blast heat exchanger (to reject the heat) back to the pump. The function of the heater was to control the NaK temperature during low-load operation and to heat the NaK during purification operations. A titanium-zirconium hot trap was provided for initial purification. The heat rejection system is shown in Fig. 30 before insulation.

K. Vacuum Chamber

The vacuum chamber and getter-ion pump are shown in Fig. 31. The chamber is heated so that the temperatures of all liquid metal lines can be maintained at at least 200°C to prevent solidification. All ports have bakeable metal seals. The main door seal is Viton-A cooled to less than 100°C. During testing the chamber operated in the 10⁻⁷ torr range, with the liquid metal system at 980°C and the chamber at 250°C.

L. Instrumentation and Controls

Liquid metal pressure was measured directly with bonded strain gage transducers. The transducers and pressure lines were maintained at 230°C to prevent solidification. Installation of the transducers in the heated enclosure is shown in Fig. 32. Valving was provided to enable calibration during operation of the test system.

Chromel-alumel thermocouples were used for temperature measurement. Attachment to the Nb-1%Zr piping and components was made by welding the wires to a tantalum foil which, in turn, was welded to the niobium alloy. Only two thermocouples of 53 failed during more than 3000 hours of testing.

All instrumentation readout and control of the loop was accomplished remotely. Figure 33 shows the control console and alarm system which was used during the test. Schematic diagrams of the instrumentation and control circuits are given in Appendix B.

III. Operating Experience

The test system was operated for over 3000 h with liquid metal flow to determine the proper startup sequencing and flow characteristics with cesium and lithium. Achievement of stable flow with both liquid metals was very difficult and tedious. For proper functioning with cesium condensation in the condenser, no cover gas (argon) could be tolerated. Yet it was found that heating the evacuated system from ~200 to ~650°C while lithium was flowing always caused argon to evolve from the lithium. Attempts to reduce the pressure while circulating lithium produced instabilities and the loss of the pumping action unless extremely gradual reductions in pressure were used $(\sim 0.1 - 0.2 \text{ atm/day})$. Another problem which occurred early in the test sequence was lack of control of the cesium flow rate. Attempts to start the cesium pump at a low flow rate and without a control valve inevitably resulted in injection of a cesium flow which was too large for the conditions of lithium temperature and flow. The result was entrainment of cesium in the lithium circuit and the subsequent loss of the lithium pump due to cesium vaporization in the pump. This latter problem was eliminated by installation of a valve in the cesium line and an externally controlled cesium injection system for startup.

With these modifications, relatively stable cesium and lithium flow was obtained at lower flow rates (~0.1 kg/s). Attempting to further increase the lithium flow resulted in severe flow oscillations, cesium entrainment, and loss of the lithium pump. The reason for the flow oscillations is the holdup of lithium in the separator because of the baffles which were installed after hydraulic testing. Use of the centrifugal separator of Fig. 17 should

eliminate this problem and enable the attainment of higher flow rates. Figure 34 is a schematic of the test loop as it should appear after the above modifications are made.

IV. SUMMARY

The cesium-lithium test system proved to be a reliable installation for obtaining lithium and cesium flow at 980°C. However, stability problems were encountered as the flow rates were increased above about 0.1 kg/s. Minor modifications to the separator should enable attainment of the 0.4-kg/s design flow rate with stable operation.

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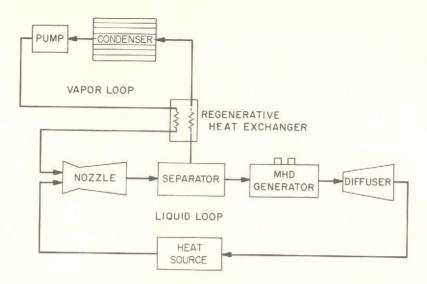


Fig. 1. Schematic diagram of cesium-lithium MHD power system

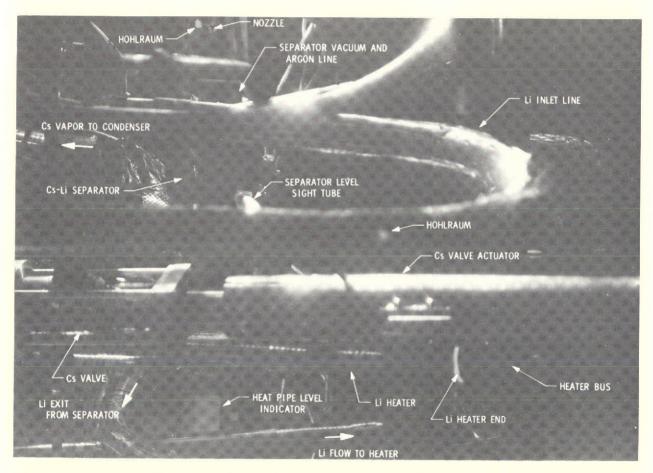


Fig. 2. Cesium-lithium erosion loop at 980°C

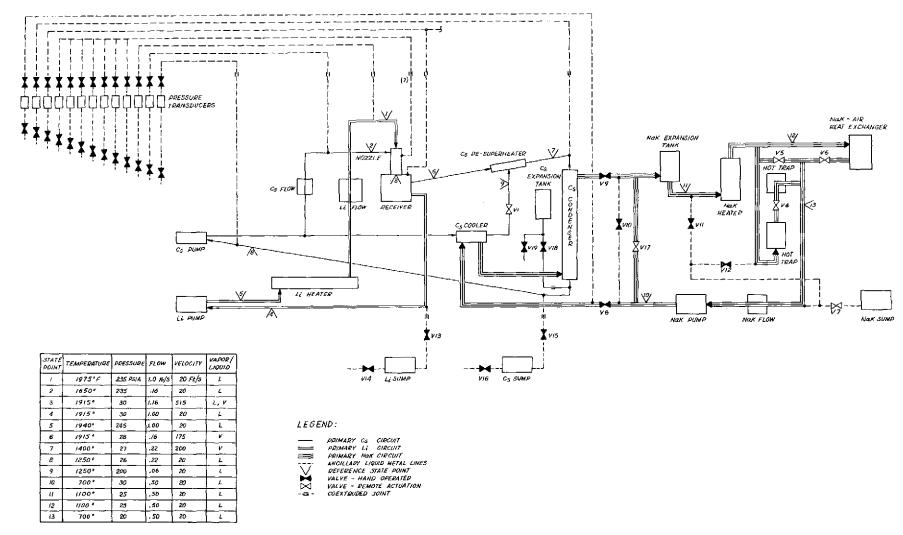


Fig. 3. 100-kW erosion loop liquid metal circuits schematic diagram

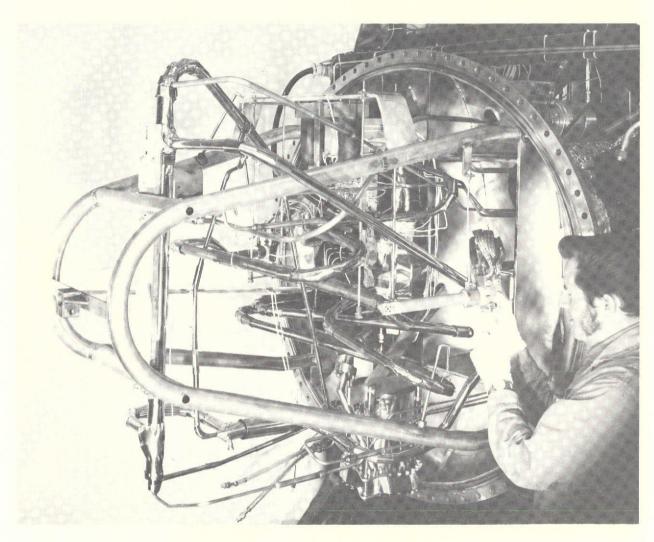
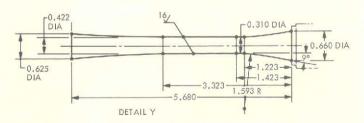


Fig. 4. Cesium-lithium test circuits before activation



DIMENSIONS ARE IN INCHES

Fig. 5. Cesium-lithium nozzle geometry

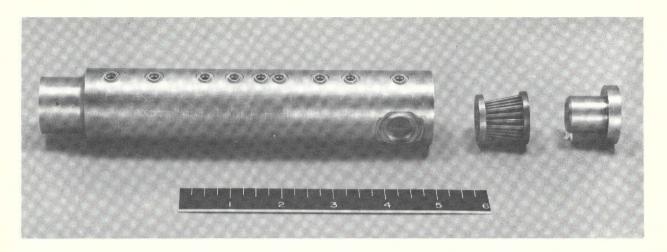


Fig. 6. Cesium-lithium nozzle before welding

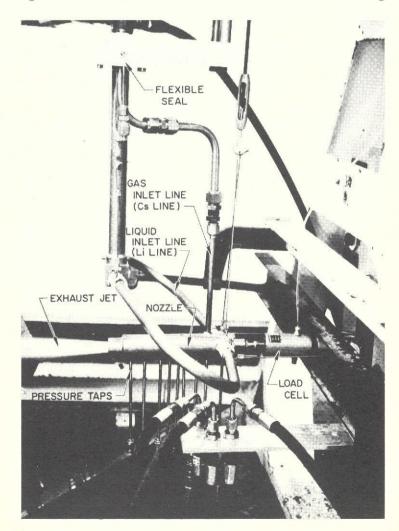


Fig. 7. Water-nitrogen test of nozzle for cesium-lithium loop

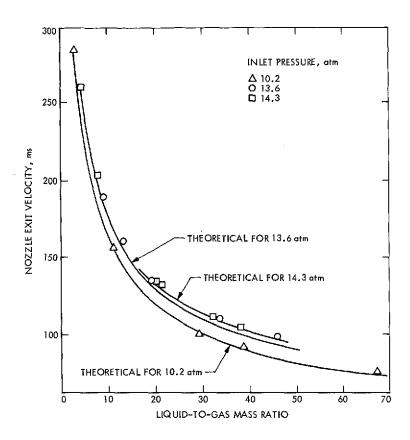


Fig. 8. Comparison of experimental and theoretical exit velocities for cesium-lithium loop nozzle operating with nitrogen and water

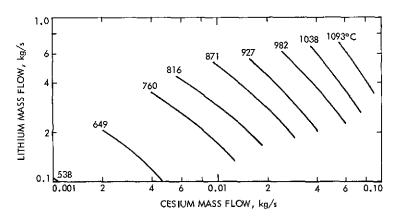


Fig. 9. Cesium-lithium nozzle flow for different nozzle inlet temperatures (saturated vapor)

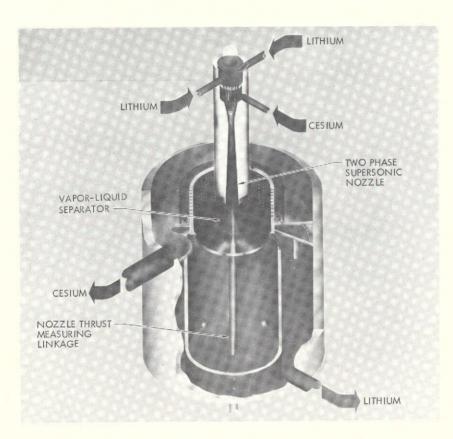


Fig. 10. Nozzle-separator assembly

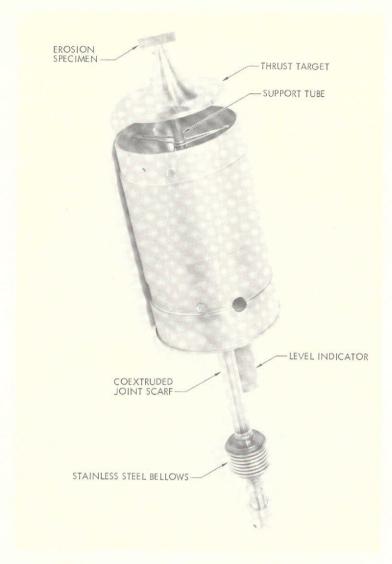


Fig. 11. Thrust target assembly

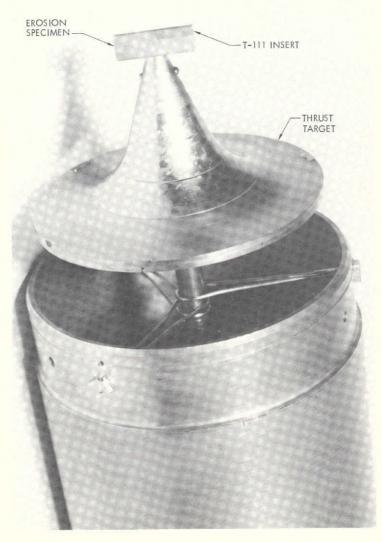


Fig. 12. Erosion specimen mounted on thrust target

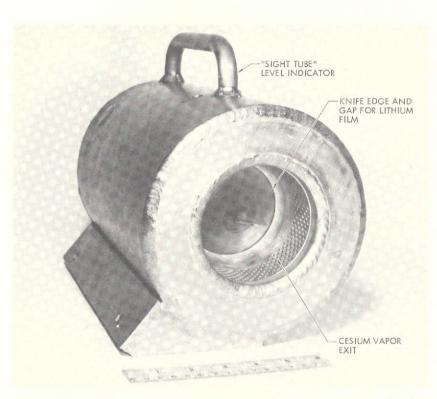


Fig. 13. Thrust target mounted in separator body

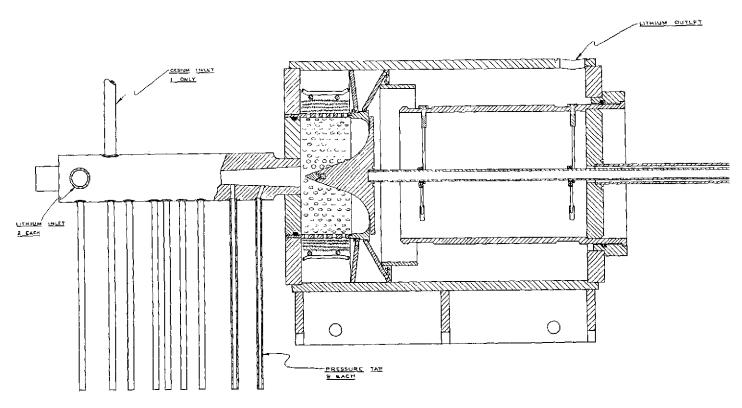


Fig. 14. Separator assembly

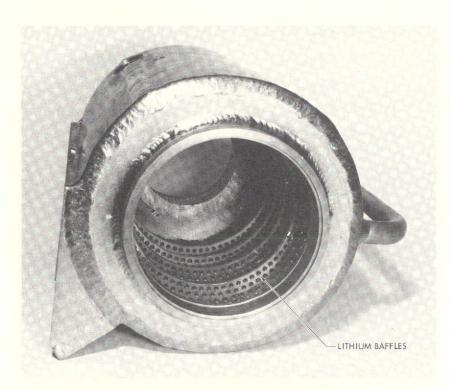


Fig. 15. Lithium baffles

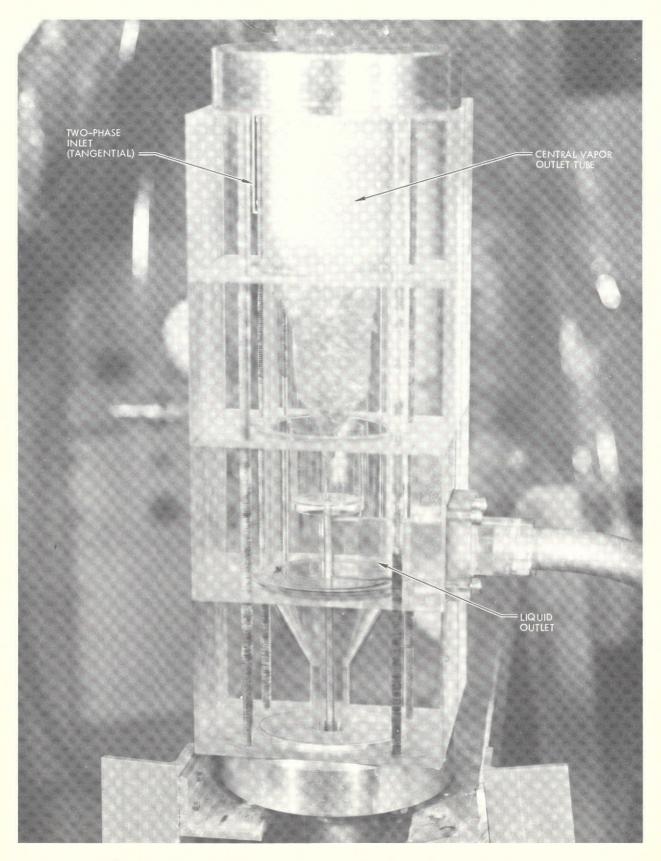


Fig. 16. Two-phase cyclone separator operating with $\rm H_2O$ and $\rm N_2$

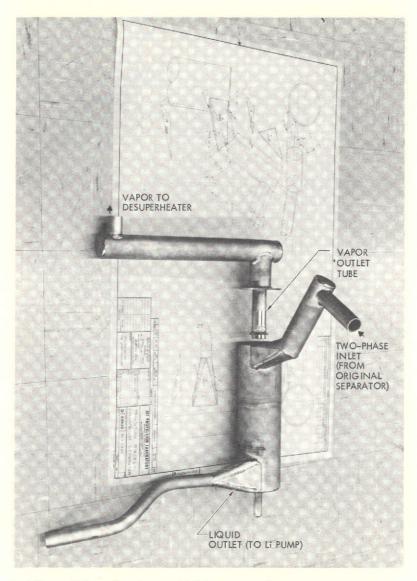


Fig. 17. Cesium-lithium cyclone separator

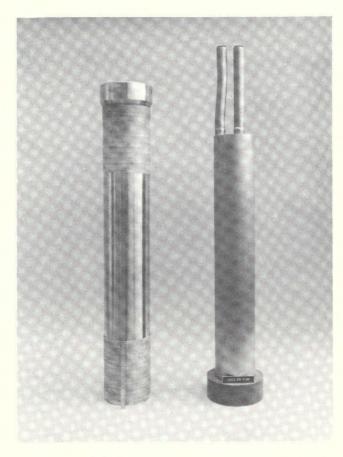


Fig. 18. Pumping element for lithium pump

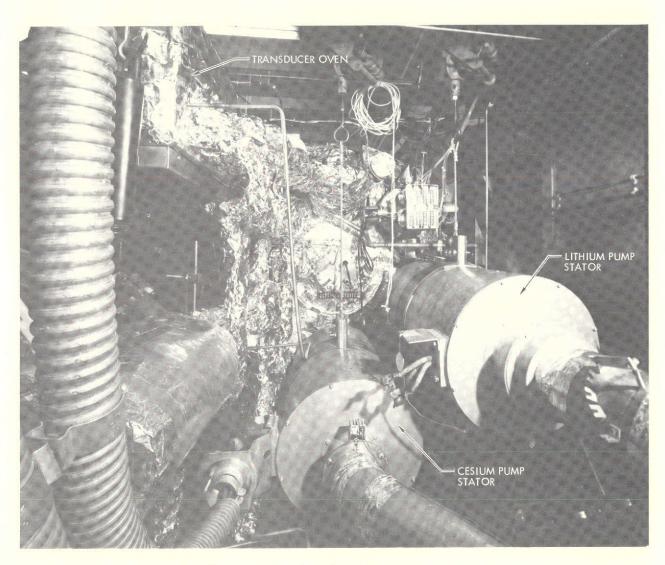


Fig. 19. Helical induction pump stators

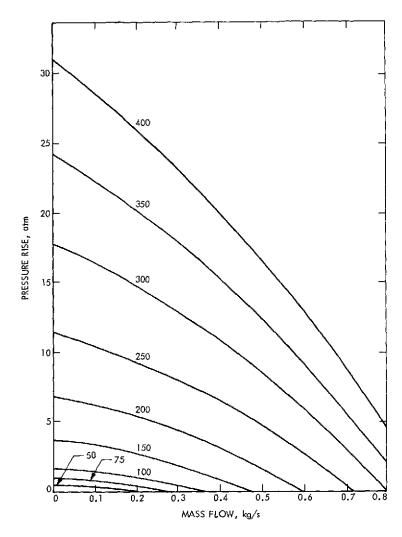


Fig. 20. Lithium pump characteristic at $980\,^{\circ}\,\mathrm{C}$

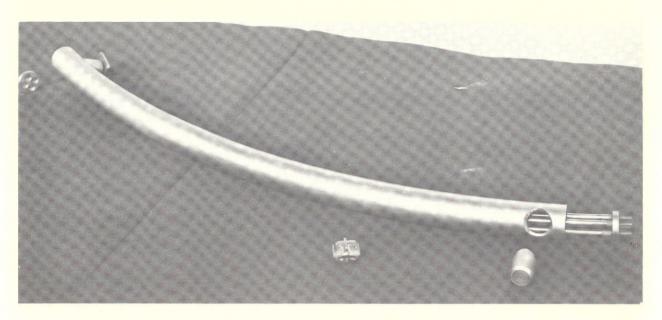


Fig. 21. Lithium heater before welding

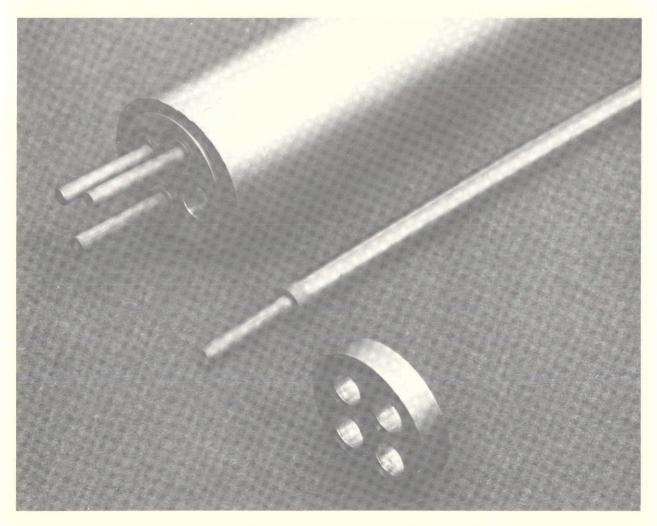


Fig. 22. Lithium heater end before welding

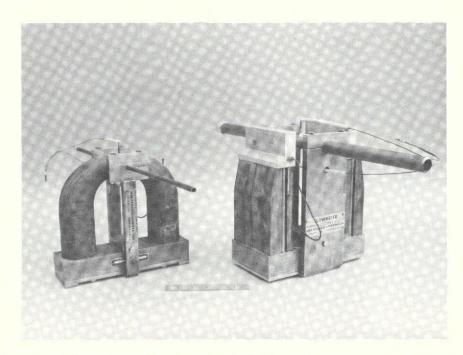


Fig. 23. Cesium and lithium flowmeters

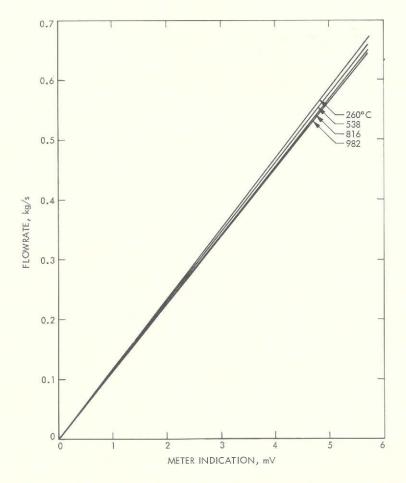


Fig. 24. Lithium flowmeter calibration (776 gauss)

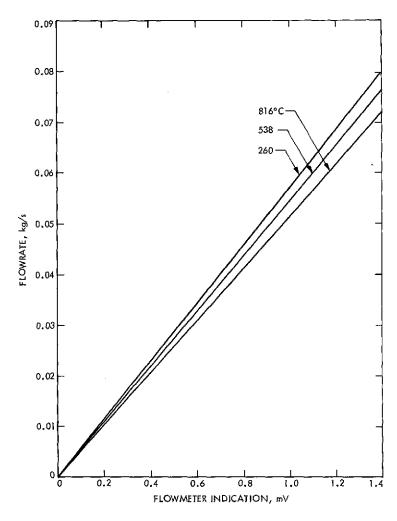


Fig. 25. Cesium flowmeter calibration (2355 gauss)

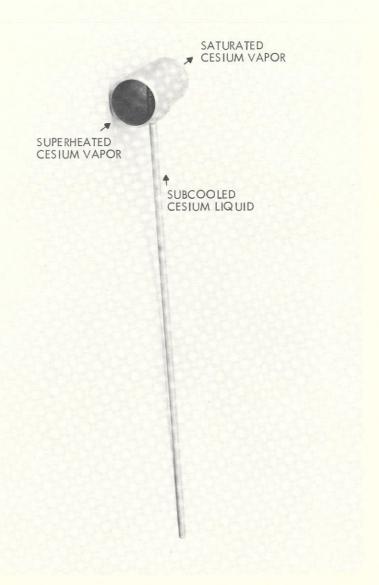


Fig. 26. Cesium desuperheater

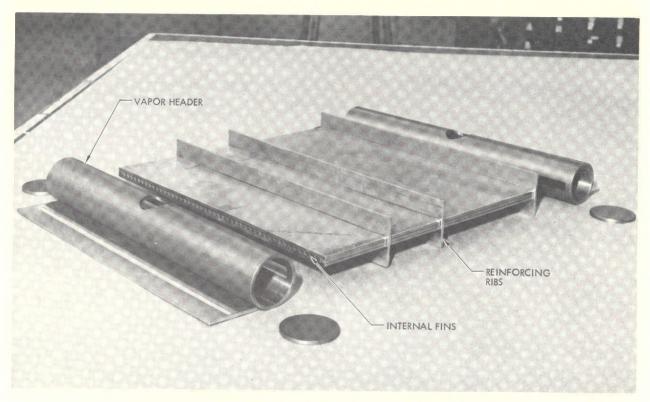


Fig. 27. Radiant cesium desuperheater before welding

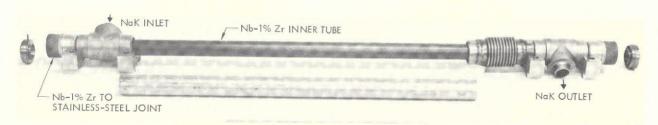


Fig. 28. Cesium condenser before welding

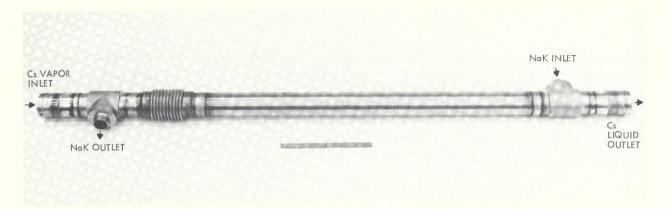


Fig. 29. Cesium condenser after welding

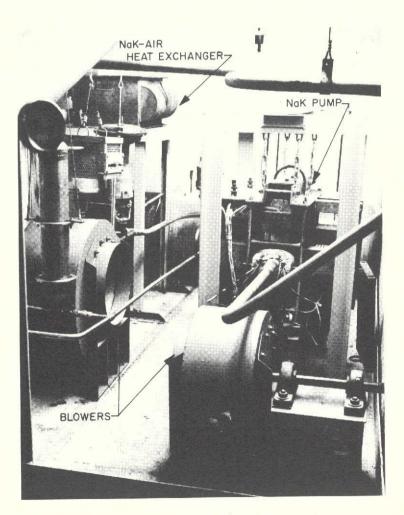


Fig. 30. NaK heat rejection system before insulation

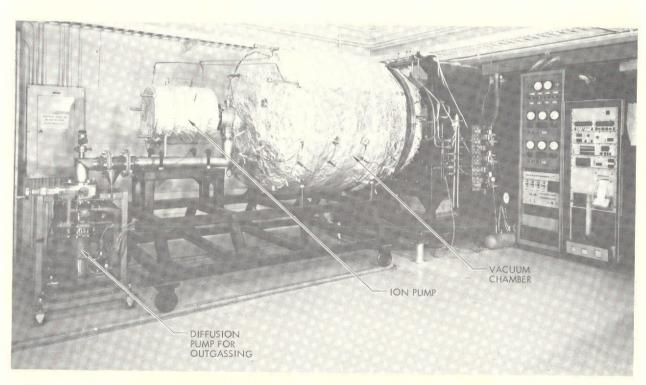


Fig. 31. Vacuum chamber and ion pump for cesium-lithium erosion loop

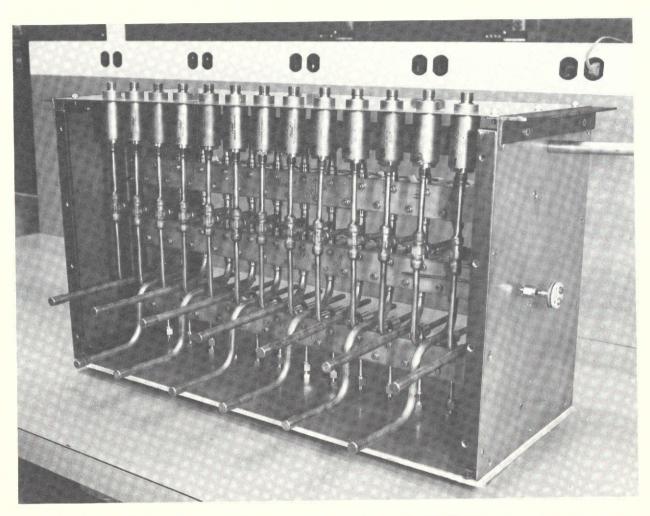


Fig. 32. Pressure transducer installation

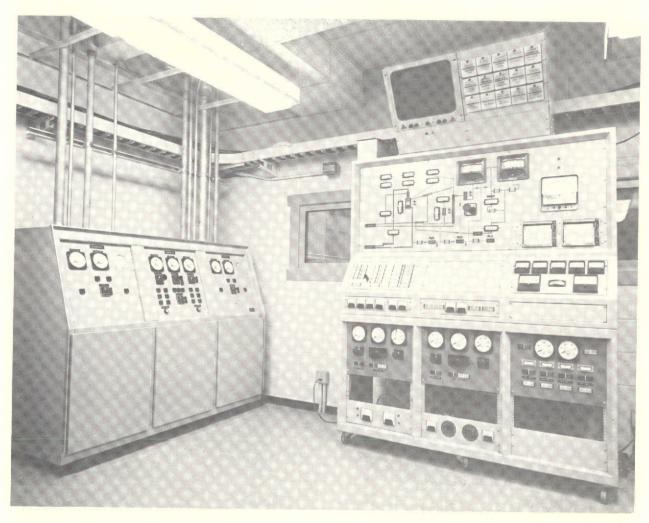


Fig. 33. Control console for cesium-lithium test system

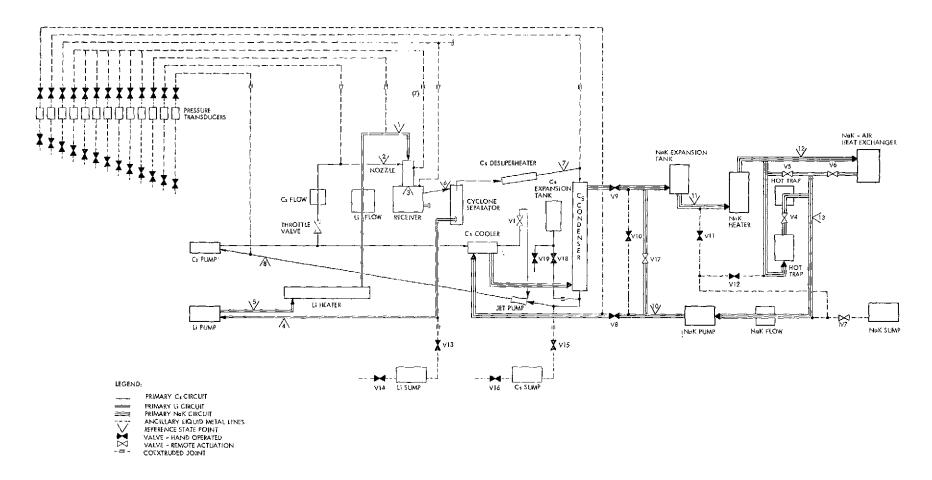


Fig. 34. Modified version of cesium-lithium erosion loop

APPENDIX A

LOOP OPERATING PROCEDURES

The startup and shutdown procedures used for the test loop are summarized below. The main modification required was installation of a cesium injection system and its actuation prior to starting the cesium pump (step 17). Full flow (steps 18-22) was not realized because of the problems discussed in the text. Values of temperatures, pressures, and flows are given in English units since the instrumentation and gauges are all in these units.

STARTUP PROCEDURES FOR Cs-Li LOOP

Startup Step

- Evacuate loop to less than 10 microns by opening manual valves HT-1 and HV-1.
 Evacuate chamber to less than 10 microns by opening vacuum valve MV-1 to roughing manifold. Turn on load cell and O-ring cooling air flange, and bus cooling water.
 Turn on makeup air in NaK room.
- 2. Turn on the chamber heaters to 5 A in each leg. Increase by 5-A steps over 10-12 h time until current is 20 A. Continue pumping until pressure is below 10 microns again. Close all transducer valves to loop. Backfill with argon to 75 mm.
- Start diffusion pump; open to chamber; close vacuum valve MV-1 to roughing manifold. Close manual values HT-1 and HV-1.
- Adjust pressure on lithium sump to 15 psig. Heat to 500°F.
- Actuate Li pump. Adjust voltage until T-9 reads 450°F. Shut off pump.
- Open lithium fill valve, V13, slowly. Monitor TC-3 to determine when receiver is filled to proper level. When TC-3 actuates, close V13.
- Adjust pressure on cesium sump to 15 psig. Heat to 200°F.
- Actuate Cs pump, Adjust voltage until T-21 reads 300°F. Shut off pump,
- Open cesium fill valve, V15, slowly. Monitor TC16 to determine when cesium leg is filled to proper level. Close V15 and V1.
- Evacuate NaK loop through HV5. Open V8, V9, and V17; continue evacuation while vacuum manifold is <10 microns. Close HV5.
- 11. Increase the argon on the supply tank to 8 psig; open the auxiliary drain valves (VII and V12), then the main drain valve (V7), slowly and only enough to insure flow. It is best to fill the system slowly. When the liquid level has reached the desired level in the expansion tank, close the drain valves (V7, V11, and V12), then the heat exchanger bypass valve (V5), the exit valve on the heat exchanger (V6), the hot trap bypass valve (V4), and the Cs-Li loop bypass valve (V10), Open the two loop valves V8 and V9. Listen for NaK flow in the loop lines. As a final step, adjust the level by adding or draining NaK to the predetermined level as discussed in a previous section. Set the pressure at 10 psig on the reservoir and supply tank.
- 12. Turn the NaK pump powerstat up slowly until the liquid metal is flowing in the loop. Keep a constant watch on the flowmeter. If there is no immediate indication of flow, stop the pump immediately and determine the trouble.

Values of Key Parameters

Pressure of chamber - 10⁻² torr on multi-torr gauge.

Final chamber temperature ≈ 500 °F. Loop temperature ≈ 450 °F.

Chamber pressure of 10^{-5} torr.

Current setting of 5 A on trace heater to obtain 500°F.

T-9 = 450°F. Li pump voltage ≈ 45 V.

T-3 should raise from 450 to 500°F in 2-3 s when lithium is at the proper level.

Current setting of 3 A on trace heater to obtain 200°F.

T-21 = 300°F. Cs pump voltage ≈ 35 V.

T-16 should lower from 450 to 200°F in 2-3 s when Cs is at the proper level.

Manifold vacuum should be < 10 µm at 4 h.

Level indicator light on Nak reservoir will change from red to yellow at proper level.

CAUTION: This is a high-capacity pump and cannot be operated without flow or liquid metal in the pumping section. In the event that there is no indication of flow, double-check the electrical connection on the flowmeter and pump, all valve settings, and the liquid level. If everything

STARTUP PROCEDURES FOR Cs-Li LOOP (contd)

Startup Step

12. (contd)

13. Turn the NaK immersion heater on and set the temperature for 650°F. Close the valve (V4), isolating the hot trap from the system. Do not circulate cold liquid metal through the hot trap. By adjusting the flow through the heat exchanger, the desired temperature can be reached.

Once the loop temperature has reached 650°F, operate at this point for an hour to ensure that the flowmeter is wet. Set the pump current at 19.5 A for a flow of 0.33 lb/s. The next step is to raise the loop temperature to 1000°F. Actuate the cooling blower for the pump when the loop temperature exceeds 850°F. Circulate at this temperature for a period of 24 h to ensure that oxides and impurities are absorbed in the liquid metal. Maintain as high flow in the heat exchanger as practical in order to ensure that the insides of these tubes are also cleaned.

- 14. Operate the hot trap, starting the flow slowly, 1/4 - 1/2 gpm, through the hot trap by opening the valve (V4). The flow in the main loop should be 1 lb/s through the heat exchanger. All portions of the loop must be at a minimum of 1000°F while hot trapping to ensure that any oxide present is in solution. Maintain the temperature at a minimum of 1000°F and the flowrate through the loop at some reasonable rate (1/2 - 1 lb/s). The time required to reduce the oxide content to an acceptable level is dependent on the quantity present and the operating temperature of the hot trap. The oxide removal rate is greater at 1200 than 1000°F. Experience indicates for a system of this size that a minimum of 12 h would be necessary to initially clean the system. Reduce the heater voltage until the loop temperature is 800°F.
- 15. Start Li pump at 25 V. Gradually increase until flow rate F1 is 0.3 lb/s. Start freeze stem flow at maximum flow rate. Remove insulation from Li pump duct port and Cs pump port.
- Actuate Li heater at 200 A. Increase current until Li inlet temperature TC-1 is 1200°F (100°F/h).
- 17. (a) Set Li pump at 90 V.
 - (b) Start Li pump blower.
 - (c) Start Cs pump at 80 V.
 - (d) Actuate Cs pump blower.
 - (e) Set heater at 9.1 V.

Values of Key Parameters

appears in order, try the pump again. Watch for a flow indication and also use an ammeter to check that the current is flowing to the pump. A humming or buzzing sound will be heard if power is reaching the pump.

The above instructions may seem rather pessimistic, but the most important point to remember is that power must not be left on this pump for more than a few seconds without liquid metal flowing.

1.16 mV on F1 = 0.3 lb/s at 500°F. Pump voltage ≈ 50 V.

E3 = 2.25 V at 200 A. E3 \approx 4.7 V for 1200°F.

Cs flow, F2 = 0.0076 lb/s (0.06 mV) at E2 = 80 V Li flow F1 = 0.3 at 90 V

STARTUP PROCEDURES FOR Cs-Li LOOP (contd)

Startup Step

- 17. (contd) Open valves to transducers. Reduce freeze valve flow until T-26 = 450°F. Actuate load cell motor until the gap is reduced to 0.010
- 18. Increase Li inlet temperature in 100°F steps by first increasing the heater voltage, then the lithium flow, then the cesium flow. Keep chamber pressure in the 10-5 range. Actuate the ion pump when 1800°F is reached and pressure is declining. Valve off diffusion pump. When the Cs pump temperature TC21 reaches 1100°F, evacuate Cs expansion tank through manual valve HV2, close manual valve HT2, open the manual valve V18 to the expansion tank until the first level thermocouple TC-52 is actuated, close the manual valve V18. When Cs temperature TC-21 reaches 1300°F, drain loop through the Cs drain line VI8 until the second level thermocouple TC-53 is actuated.
- 19. Adjust the separator gap until the NaK outlet temperature TC-33 is minimized. Change V1 until saturated vapor is obtained (compare TCI4 and PII).
- 20. Adjust the Li pump and Cs pump, heater and NaK temperature until Pl = 137 psia at a value of F1/F2 = 10.
- 21. Measure nozzle thrust. Vary stem position by +0.010 in. in 0.002-in, increments to determine spring constant.
- 22. Freeze stem by increasing the Dowtherm flow to the full flow rate.

Values of Key Parameters

<u>T1</u>	<u>E1</u>	<u>E2</u>	<u>E3</u>	<u> </u>	
1300 1400 1500 1600 1700 1800	110 136 165 198 231 279	100 125 153 186 236 293	11.2 13.1 15.0 17.0 18.2 21.2	0 0 0 0 .818 .891	C1 = 0.05
1700 1800	233 283	226 277	13, 8 16, 4	. 449	C1 = 0.02

The values under key parameters are for a lithium carryover fraction of 0,05. Different values will result in different heater settings to attain the required temperatures.

VALVE POSITIONS FOR EROSION LOOP STARTUP

Startup Step	_								Val	re N	o. V							_			Val	ve	No.	SA				_		Va.	ve	No.	sv		_	н	<u>r_</u>	_		Ħ	₹		_	MV
	1	4	5	<u>6</u>	7	8	9	<u>10</u>	11	12	<u>13</u>	14	15	<u>16</u>	17	18	<u>19</u>	· <u>1</u>	2	3	4	<u>5</u>	<u>6</u>	7	<u>8</u>	9	<u>10</u>	1	<u>2</u>	3	4	<u>5</u>	<u>6</u>	7	<u>8</u>	1	2	1	<u>2</u>	<u>3</u>	<u>4</u>	<u>5</u>	<u>6</u>	<u>1</u>
ı	0	x	X	x	x	x	X	x	x	x	x	X	x	X	X	0	X	х	X	X	x	X	x	X	x	x	x	X	X	X	X	x	X	X	x	0	0	D	X	X	0	x	x	0
2	0	X	X	X	X	x	X	X	x	x	X	X	x	X	x	O	X	x	X	X	x	x	x	x	X	,X	x	x	x	x	x	x	x	X	X	0	0	0	x	X	0	x	X	0
3	X	X	X	X	x	x	X	x	x	x	x	x	x	X	x	x	x	x	x	x	x	x	x	x	x	x	x	x	x	x	x	x	x	x	X	x	x	x	x	x	x	x	x	x
4	x	X	X	x	x	x	X	x	x	x	x	X	x	X	x	x	x	x	x	x	x	x	x	0	x	x	x	x	х	х	x	x	x	x	X	x	x	x	x	x	x	x	x	x
5	x	x	X	x	x	x	X	x	X	x	x	X	x	X	X	x	x	x	X	x	x	x	x	0	x	x	x	X	x	X	x	x	x	x	X	x	x	X	x	x	x	x	x	x
6	x	x	X	x	x	x	x	x	X	x	0/X	X	x	x	x	x	x	x	x	x	x	x	x	0/x	x	x	x	x	x	x	x	x	x	x	X	x	x	x	x	x	x	x	x	x
7	x	X	X	x	X	x	X	X	X	X	x	X	x	X	X	x	x	x	X	x	x	x	0	X	x	x	x	x	x	x	x	x	X	X	X	x	x	x	x	x	x	x	x	x
8	0	X	X	X	X	x	X	x	X	X	x	X	X	X	I	x	X	x	X	x	x	x	0	x	x	x	X.	x	x	X	x	x	X	x	X	x	x	x	x	x	x	x	x	x
9	0/2	X X	X	X	x	x	X	X	X	X	x	x	0/X	X	X	x	X	x	X	x	X	x	x	X	x	x	x	x	x	X	x	x	X	X	x	x	x	x	x	x	x	x	x	x
10	x	X	X	X	x	O	0	X	X	x	x	X	X	X	0	x	x	x	X	x	x	x	x	X	x	x	x	x	X	x	x	x	X	x	x	X	x	x	x	X	x (0/X	x	x
11	x	0/2	(0/	xo/:	x0/x	0	0	0/X	0/X	0/X	x	X	X	X	0	x	X	x	X	X	0/x	0/x	x	X	X	x	x	x	X	X	x	x	x	X	x	X	x ·	x	X	X	X	x	x	X
12	x	x	X	x	x	0	0	x	x	x	x	x	x	x	0	X	X	X	X	x	x	x	x	x	x	x	x	X	X	X	X	x	x	X	X	X	x	x	x	x	x	x	x	x
13	X	X	0	0	X	X	0	X	X	X	x	X	x	X	0	X	X	X	X	X	x	x	x	x	X	x	x	X	X	X	X	x	X	X	X	X	X	x	x	x	x	x	x	x
14	x	0/1	K 0	0	X	X.	0	X	X	X	x	x	x	x	0	x	x	x	X	x	X	x	X	X ·	X	X	x	X	x	X	x	x	X	X	X	X	x	X	x	X	X	X	x	x
15	x	x	X	x	x	0	0	x	x	X	x	X	x	x	0	x	x	x	X	x	x	x	x	X	x	x	x	x	x	X	x	x	X	X	Х	x	x	x	x	x	x	x	x	x
16	x	X	X	x	x	0	0	X	x	X	x	x	X	x	0	x	x	x	X	x	X	x	x	x	x	X	x	X	x	X	x	x	x	x	х	X	х	x	x	X	x	x	x	x
17	x	X	X	X	x	0	0	X	X	X	x	x	X	X	0	x	x	X	X	x	X	X	x	X	x	x	x	X	X	X	X	x	X	X	x	x	x	x	x	X	x	x	x	x
18	0	X	X	x	X	0	0	x	X	X	x	X	x	X	o	O/X	x	x	x	x	x	x	x	x	x	x	x	X	x	x	X	x	X	X	Х	x	x	x	x	X	x	x	x	x
19	0	X	X	X	X	0	0	x	X	X	x	X	X	X	0	x	x	x	X	X	X	x	x	x	x	x	x	X	x	X	x	x	X	x	x	X	x	x	x	x	x	x	x	x
20	0	X	X	X	X	0	0	X	X	X	x	x	x	X	0	x	X	x	X	x	X	x	x	x	x	x	x	X	x	X	x	x	x	X	x	x	x	x	x	X	x	X	x	X
21	0	X	X	x	x	0	0	x	x	x	x	x	x	x	0	x	x	x	X	x	x	x	x	x	x	x	x	x	X	x	x	x	x	X	x	x	X	x	x	x	x	x	x	x
22	0	X	X	x	x	0	0	X	X	X	X	x	X	X	0	x	X	x	X	x	x	x	x	x	x	X	X	x	X	x	x	X	X	X	X	X	X	x	X	x	x	x	x	x

X Closed

⁰ Open

NORMAL SHUTDOWN FOR EROSION LOOP

- 1. Decrease the Li pump and Cs pump voltages concurrently by 25-V steps until a Li pump flow rate of 0.3 lb/s is reached. Reduce flow to freeze valve and increase gap to 0.045 in.
- 2. Decrease the Cs pump voltage further until a setting of 25 V is reached.
- 3. Decrease the Li heater power until a lithium inlet temperature of 1000°F is reached (100°F/hr).
- 4. Turn off cesium pump.
- 5 Turn off Li heater.
- 6. Decrease Li pump voltage by 25-V increments until it is off.
- 7. Turn off NaK flow.
- 8. Set Li sump pressure to 5 psig and loop pressure to 15 psig. Open SA3 manual valve HT1 and V13 to drain lithium. Drain until sump pressure rises. Repeat for Cs sump using SA3 manual valve HT1 and V15. Close SA3 and drain valves V13 and V15. Evacuate loop through SV6 and manual valve HV1. Close SV6 and manual valves HV1 and HT1.
- 9. Evacuate both sumps through HV3 and HV4. Close HV3 and HV4.
- 10. Heat both sumps to 400°F. Heat chamber and pumps to 800°F. Open V13 and V15. Monitor fill and dump line temperature TC-43. When TC-43 drops to ~400°F the loop is drained. Close V13 and V15. Turn off all heaters.

EMERGENCY PROCEDURES FOR EROSION LOOP

Emergency	Function	Location of Function
1. Liquid metal leak in	a. Turn off Li, Cs, NaK pumps, Li heater, ion pump.	CR
chamber	b. Close manual dp valve (if open).	нв
	c. If O-ring temperature rises to 300°F, open argon flood for chamber, SA-8.	нв
,	 d. Increase cooling flow on chamber to limit temperature rise. 	НВ
	e. If NaK level drops, pressurize NaK reservoir to 10 psig, and drain through V7 to NaK sump. Watch chamber pressure.	CR
	f. Keep system under observation as temperature cools.	CR/HB
2. Liquid metal leak in NaK	a. Turn off Li, Cs, NaK pumps, Li heater, bus cooling water.	CR
room	b. Turn off heat exchanger blower and makeup air blower.	CR
	c. Close heat exchanger damper by setting controller on 1400°F.	CR
	d. Pressurize NaK reservoir to 10 psig, drain through V7 to NaK sump.	CR
	e. When leak stops, extinguish fire if safe.	НВ
3. Liquid metal leak in door	a. Turn off Li, Cs, NaK pump, Li heater, bus cooling water.	CR
area	b. Turn off heat exchanger blower and makeup air blower.	CR
	c. Close heat exchanger damper by setting controller on 1400°F.	CR
	d. If safe, turn off flange water and trans- ducer oven.	НВ
	e. If NaK level drops, pressurize NaK reservoir to 10 psig and drain through V7 to NaK sump.	CR
<u>}</u>	f. If leak is from transducer box, valve off all transducers, if safe.	НВ
	g. When safe, extinguish fire.	HB
CR = control ro HB = high bay	om	

APPENDIX B

TEST SYSTEM SCHEMATIC DIAGRAMS

All instrumentation, control, flow, argon and vacuum, and electrical schematics for the test system are contained in this appendix (see Figs. B-I through B-30).

The following manufacturers' manuals are available at the Jet Propulsion Laboratory, care of Section 383 files, Mr. L. H. Huebner.

- 1. Technical Manual, Helical Induction Electromagnetic Pump, Model 5KY414PK1 (Lithium), General Electric Company.
- 2. Technical Manual, Helical Induction Electromagnetic Pump, Model 5KY414PJ1 (Cesium), General Electric Company.
- 3. Instruction Manual, TrioVac, 500 liter/s Triode Ion Pump, Model 22TP300, General Electric Company.
- 4. Instruction Book, Type WSH-Arc Welder, 1000A, Westinghouse Electric Company.
- 5. Miscellaneous instrumentation and auxiliary component calibration sheets and instruction manuals.

INSTRUMENTATION FUNCTIONS

Transducer Connections

	Inside Chamber	TC Pan	el 1		Outside Chamber		TC Par	<u>1e12</u>
TC - 1	Nozzle inlet - lithium	1.8	2	TC -33	NaK exit piping		65 δ	k 66
10-1	Nozzle inlet - cesium	1 &	4	34	Expansion tank	. •	67	68
3	Receiver lithium fill	5	6	35	Heater	•	69	70
4	Receiver cesium exit	7	8	36	Hot trap		71	72
5	Receiver lithium exit	9	10	37	Hot trap flowmeter		73	74
6	Lithium pump return line	11	12	38	Heat exchanger out		75	76
1 -	Lithium pump exit	13	14	39	Main flowmeter		77	78
7 8	Lithium pump duct A	15	16	40	Pump outlet		79	80
9	Lithium pump duct B	17	18	41	NaK pump windings		81	82
10	Heater bus A	19	20	42	Pressure tap lines		83	84
10	Heater bus B	21	22	43	Fill and dump lines		119	120
12	Heater body	23	24	44	Lithium pump windings		121	122
13	Lithium flowmeter magnet	25	26	45	Cesium pump windings		123	1.24
13	Condenser, cesium inlet	27	28	46	Transducer oven		125	126
15	Condenser, cesium exit	29	30	47	Heater feedthru A		127	128
16	Condenser, cesium fill	31	32	48	Heater feedthru B		129	130
17	Cesium line, cooler to de-sup	33	34	49	Chamber body		131	132
18	Cesium pump return line	35	36	50	Ambient		133	134
19	Cesium pump exit	37	38	51	Thermocouple ambient		135	136
20	Cesium pump duct A	39	40	∜ 52	-		137 ชื่	138
21	Cesium pump duct B	41	42					
22	Cesium flowmeter magnet	43	44					
23	Receiver level indicator	45	46					
24	Co-extruded joint, pressure taps	47	48					
25	Co-extruded joint, loop vacuum	49	50					
26	Co-extruded joint, load cell stem	51	52			•		
27	Receiver	53	54					
28	Nozzle inlet lithium	55	56					
29	Nozzle inlet cesium	57	58					
30	Nozzle body	59	60					
31	Sight glass, 3-1/4 in. high	61	62					
y 32	Sight glass, 4-1/2 in. high	63 V	,					
¥ J.Z.	orene grass, 4 1/4 1ml with	'						

Instrumentation Functions Transducer Connections (contd)

	Pressure Functions	Pressure Panel Amp. Out Connections
P- 1	Nozzle, lithium inlet	l to amplifier 105 & 106
2	Nozzle, cesium inlet	2 to amplifier 107 & 108
3	Receiver pressure	8 to amplifier 109 & 110
4	Nozzle tap A	3
5	Nozzle tap B	4
6	Nozzle tap C	5
7	Nozzle tap D	6
8	Nozzle tap E	7
9	Nozzle tap F	12
10	Nozzle tap G	13
11	Condenser cesium inlet	9 to amplifier 111 & 112
12	Cesium pump inlet	10
√ 13	NaK bypass	11 to amplifier 139 $\&$ 140

	Flowmeter Functions	Flowme	eter a	and Feedthru
F-1	Lithium flow	85 &	86	95 & 96
la	Lithium flow (standby)	87	88	97 98
2	Cesium flow	89	90	99 100
√ 2a	Cesium flow (standby)	91	92	1.01 1.02
		93	94	103 ∳ 104
F-3	Main NaK flow	113	114	(outside)
F-4	Hot trap flow	115	116	(outside)
F-5	NaK bypass flow	117 ↓	118	(outside)

Instrumentation Functions

Meter - Relays

Cable No.	71	to Main Control	Pane 1	(CBA)	Meter No.	Cable No	<u>. 71</u>	to	Contro	11	ers	Controlle	er No.
Subcable	1	AK 27 &	28		1	Subcable	22	Cl			70	22	
Ì	2	AM 1	2		2	Subcable	23	C2	75	&	76	23	
}	3	AP 3	4		· 3	Subcable	24	C3	125	&	126	24	
]	4	DDX 115	116		4								
	5	FDX 113	114		5								
	6	CHX 111	112		6								
	7	BKX 109 ¥	110		7								
1	8	EJX			8								
	9	GOX 85 &	86		9								
	10	BMX 105	106		10								
	11	ENX 45	46		11								
	12	BPX 107	108		12								
+	13	EPX 89 ¥	90	-	13								

Cable No. 71	to Secondary 1	Panel (CBD)	Meter No.	Cable No. 72 to Strip Chart
Subcable 14	AC 81 &	82	14	Subcable 1 No. 1 5 & 6
1 15	AF 121	122	1 .5	2 No. 2 31 & 32
l 16	AM 123	124	16	3
17	BD 127	128	17	4 pair 7 - bus shunt
18	BN 131	132	18	5 53 & 54
19	EK 15	16	19	6 61 & 62
20	AK 39	40	20	Ý 7 63 & 64
21	AP 143 V	144	21	<i>,</i>

Instrumentation Functions Meter - Relays (contd)

	Mu	Cable No Iti-Point Re			<u>Mult</u>	Cable Ni-Point		der 2
Channel	1-26	P4 :	(pressure)		Char	nel 1	23	§ 24
1	2-27	P5 4			ļ	2	1	2
	3~28		5	pressure		. 2 . 3	9	10
	4-29		; /	cable	ļ	4	11	12
1	5-30	P8 .	į	number		5	17	13
1	6-35	P9 1:				6	17	18
1	7-36	P10 13				7	13	14
l	8-33	P12 10		•		8	37	38
1	9-34	139 & 140	•			9	3	4
-	10	19 20				10	7	3
1	11	21 22				11	27	28
1	12	25 26				12	29	30
ļ	13	43 44				13	35	36
į	14	77 78				14	41	42
{	15	73 74			ļ	15	33	34
i S	16	129 ¥ 130			į	16	75	76
ĺ	17		load cell e	nc. temp.		17	79	80
*	18					18	65	66
1	19	125 & 126				19	67	68
1	20	47 48	•			20	69	70
į	21	49 50			5	21	71	72
cyal Company	22	51 🐓 52	•		, i	22	83	84
	23	•	vacuum		ŀ	23	119	/ 120
A	24	135 & 136	•		4	24		

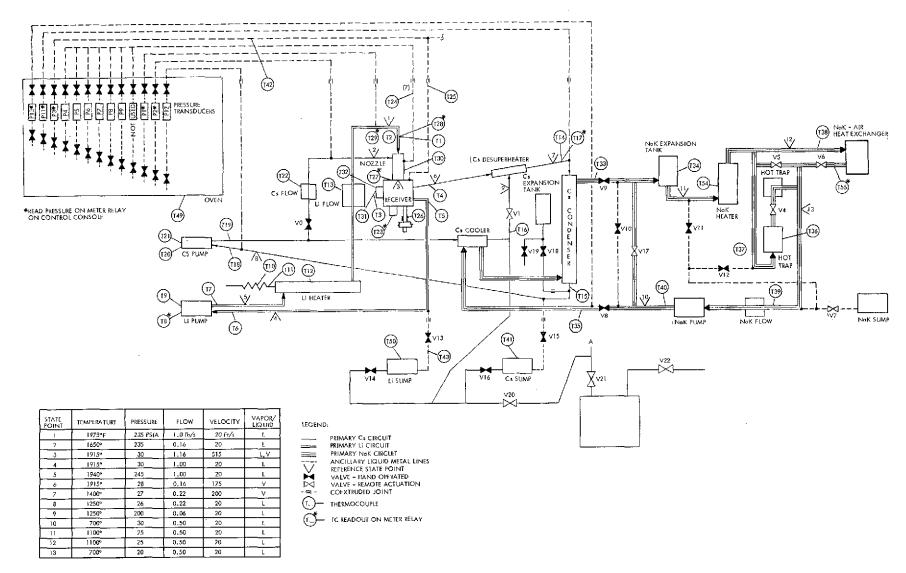


Fig. B-1. 100-kW erosion loop liquid metal circuits schematic diagram

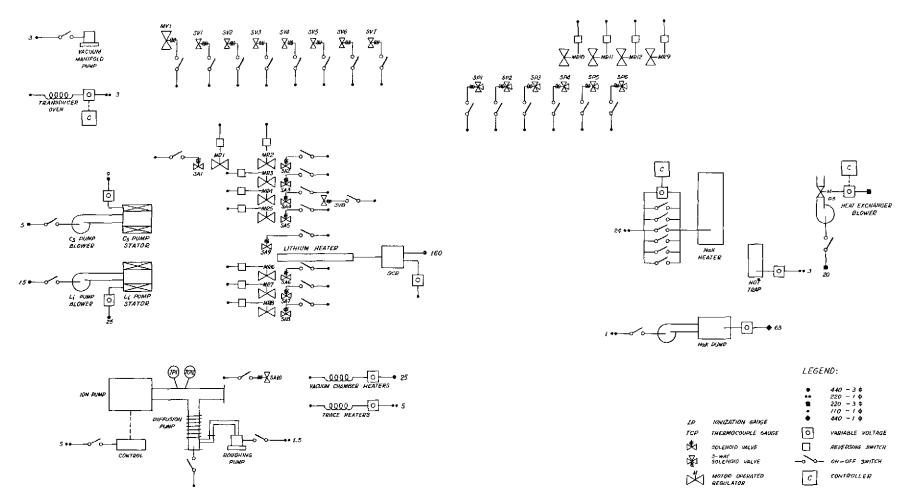


Fig. B-2. 100-kW erosion loop electrical schematic diagram

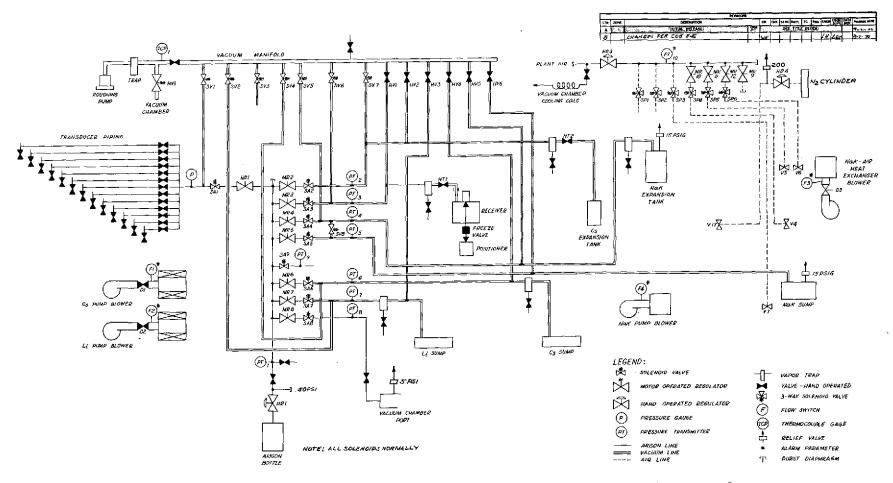


Fig. B-3. 100-kW erosion loop argon, vacuum, and air circuits schematic diagram

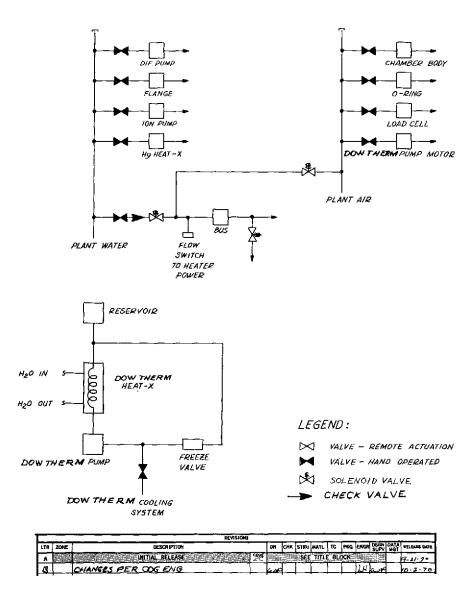


Fig. B-4. 100-kW erosion loop cooling circuits schematic diagram

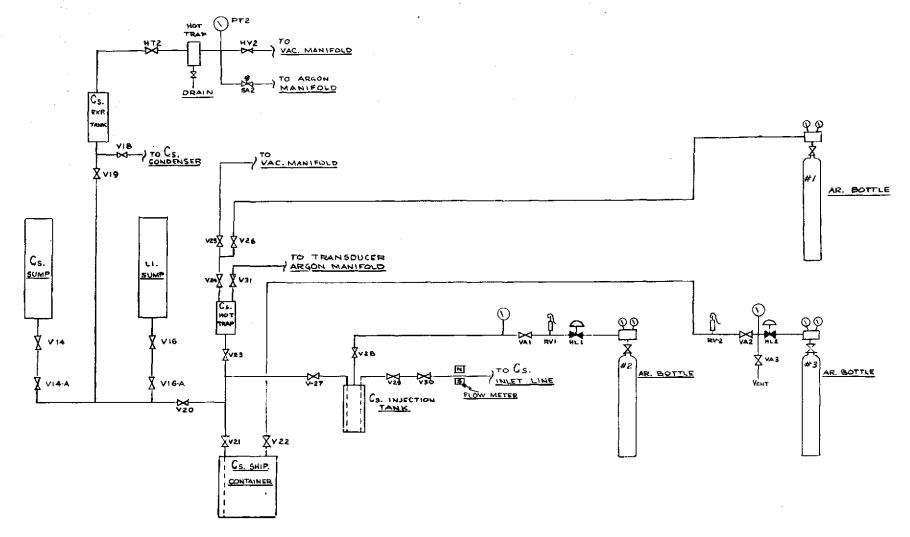


Fig. B-5. 100-kW erosion loop Cs injection and separation circuit schematic diagram



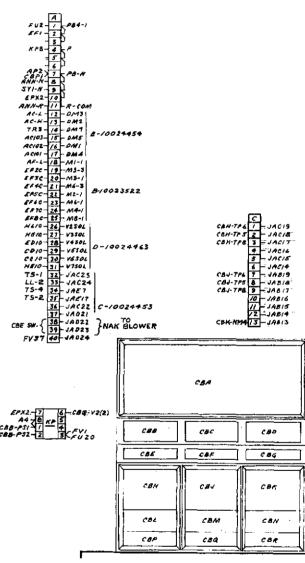
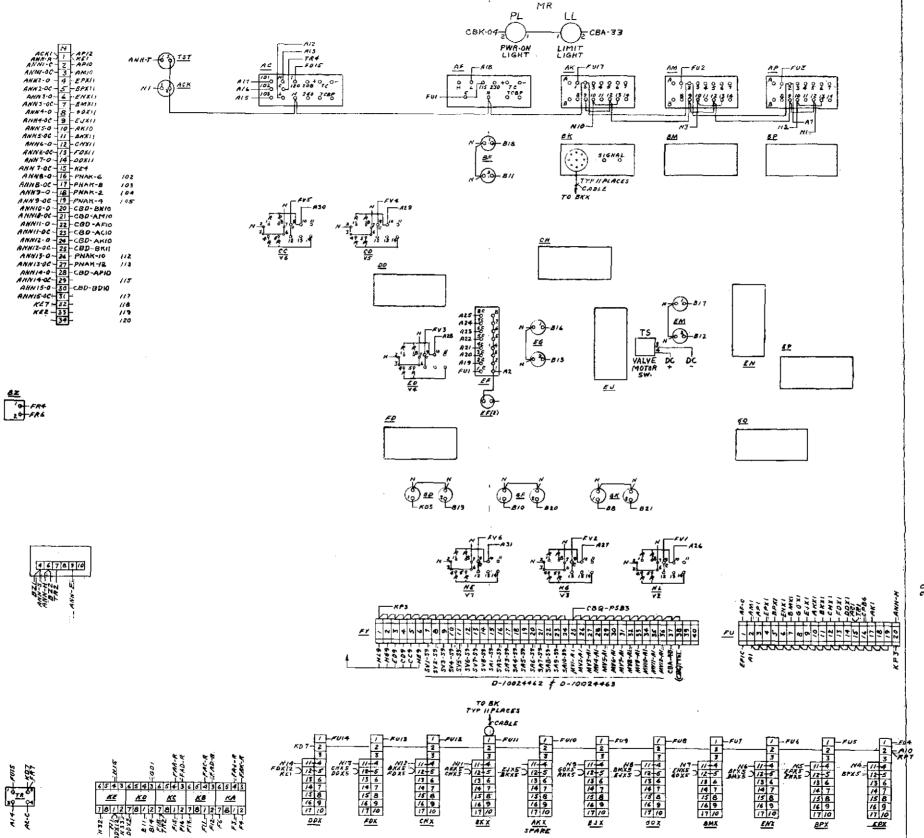
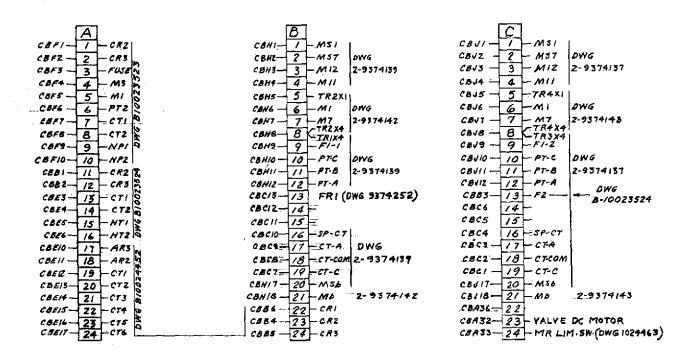
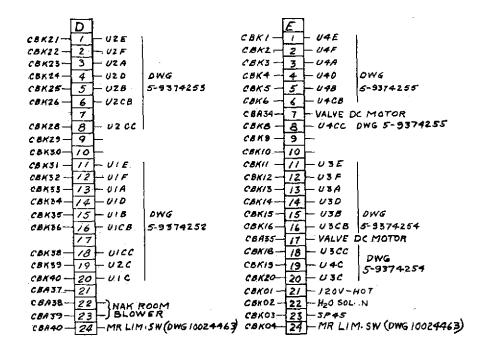


Fig. B-6. Building 148 panel CBA wiring diagram



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				Ŀ		
C	10-5-70	CHANGED B13, C23, C24, D22-23-24, E7-17-24	LG		LH	anp.
B	11-11-48	CHANGED WIRES AT BIA, BIS, BIT, BIB & CIA, CIS, CITCHE	DGH		1034	LA
A	11-20-67	ISSUED FOR CONSTRUCTION	DGH	ATS	ASH!	LH
LETTER	BATE	CHANOS	NT	CHE	Elife	APTO

Fig. B-7. Building 148 junction box JA interconnection diagram

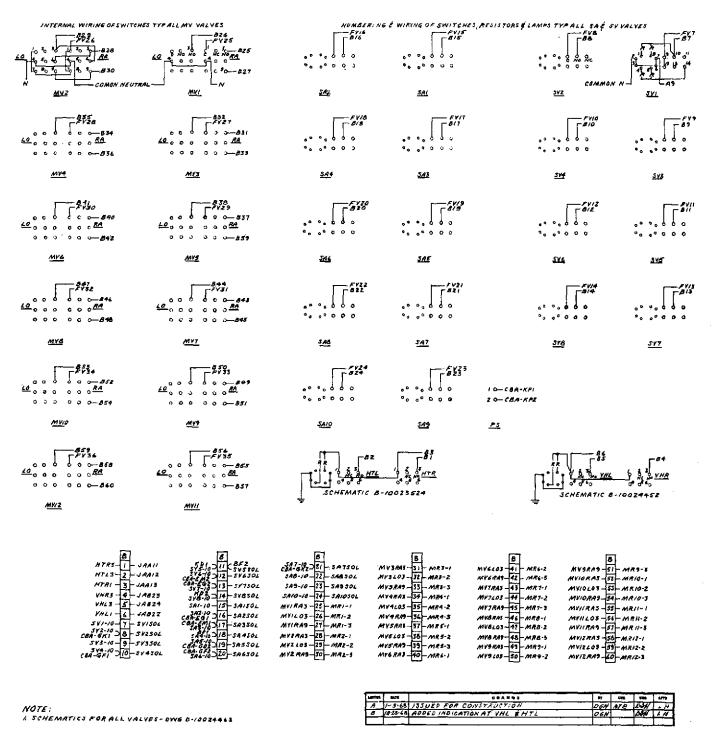


Fig. B-8. Building 148 panel CBB wiring diagram

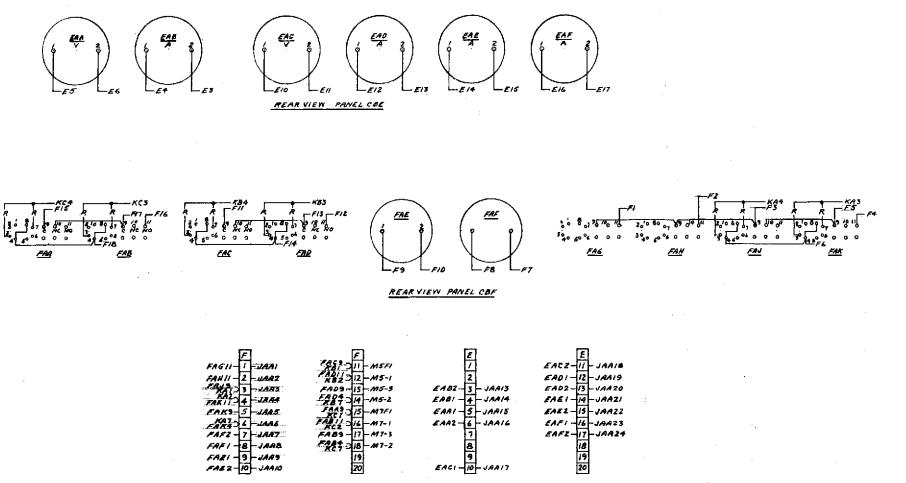


Fig. B-9. Building 148 panels CBE and CBF wiring diagram

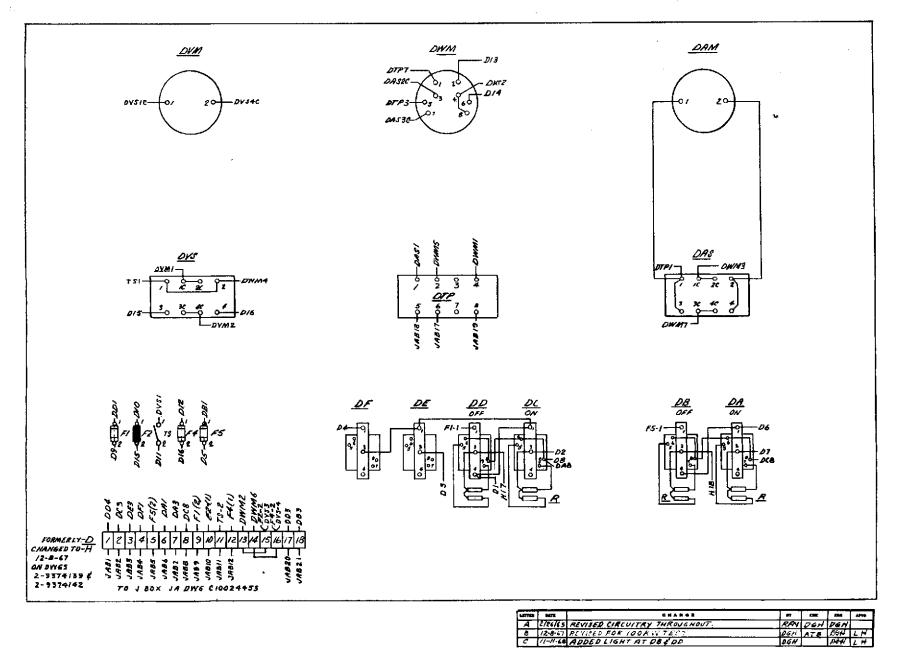


Fig. B-10. Magnetohydrodynamic facility panel CBH wiring diagram

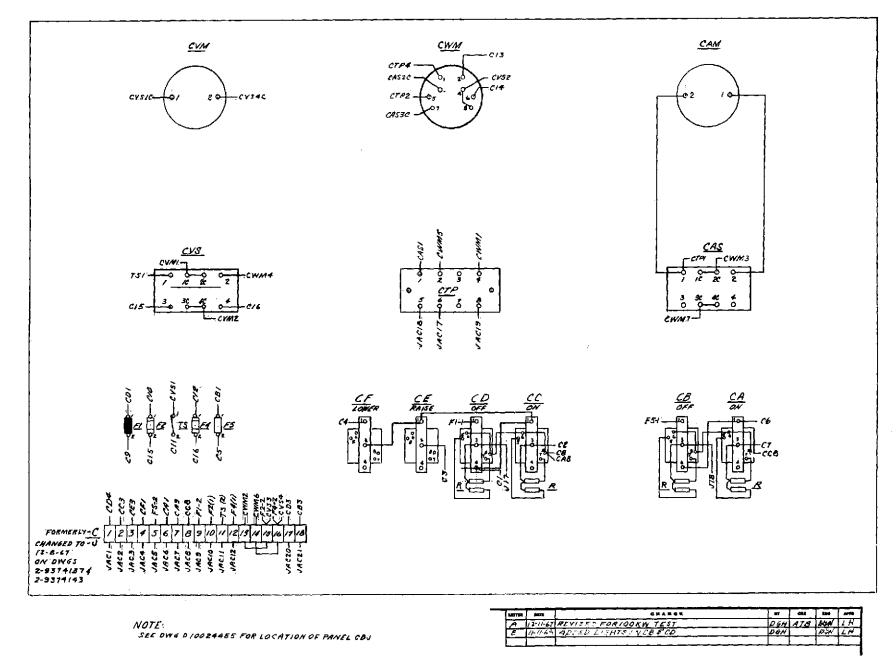


Fig. B-11. Magnetohydrodynamic facility panel CBJ wiring diagram

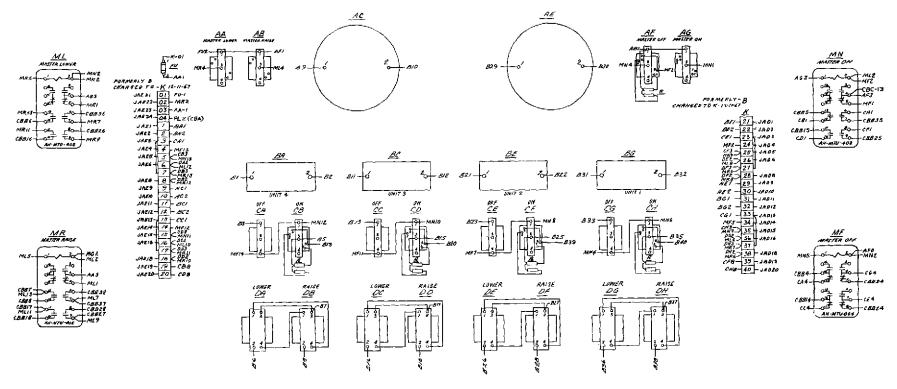
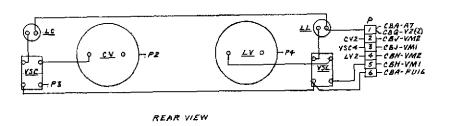


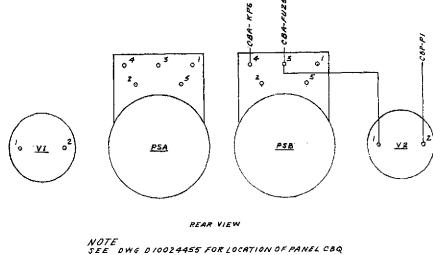
Fig. B-12. Magnetohydrodynamic facility panel CBK wiring diagram



NOTE SEE DWG DIOOZ4455 FOR LOCATION OF PANEL CBP

L A	11-11-68	CHANGED CALLOUT AT PI	DGH		054	44
A	8-5-68	AS BUILT	DGH		DGH	
REV	DATE	CHANGE	DWN	CHK	ENG	APPYD

Fig. B-13. Building 148 panel CBP wiring diagram



B WORE CHANGED HODKUP OF PSB DGH DGH LM
A 8-5-68 AS BUILT DGH DGH LM
REV DATE CHANGE DWN CHK ENG APPYO

Fig. B-14. Building 148 panel CBQ wiring diagram

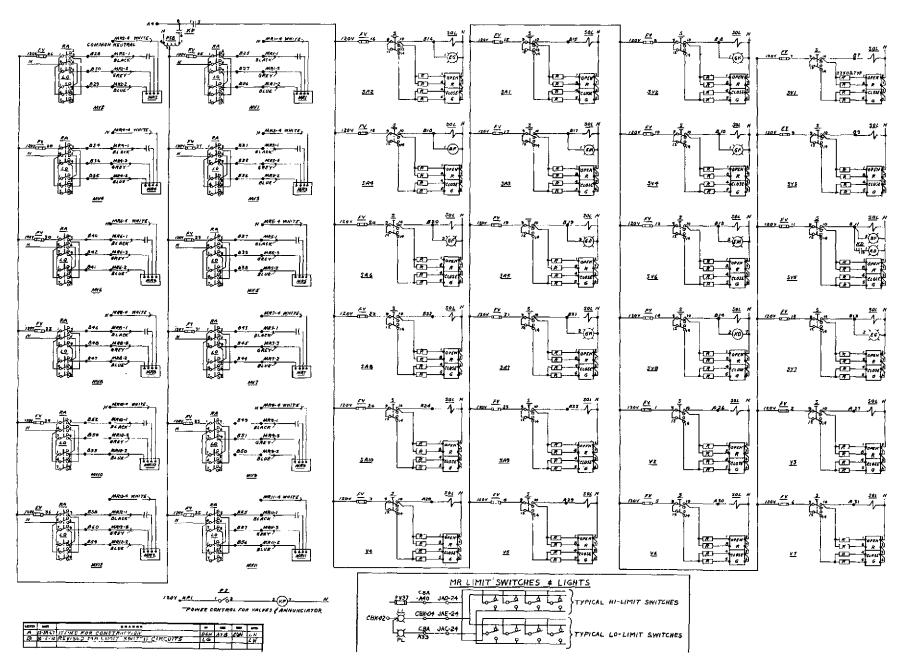
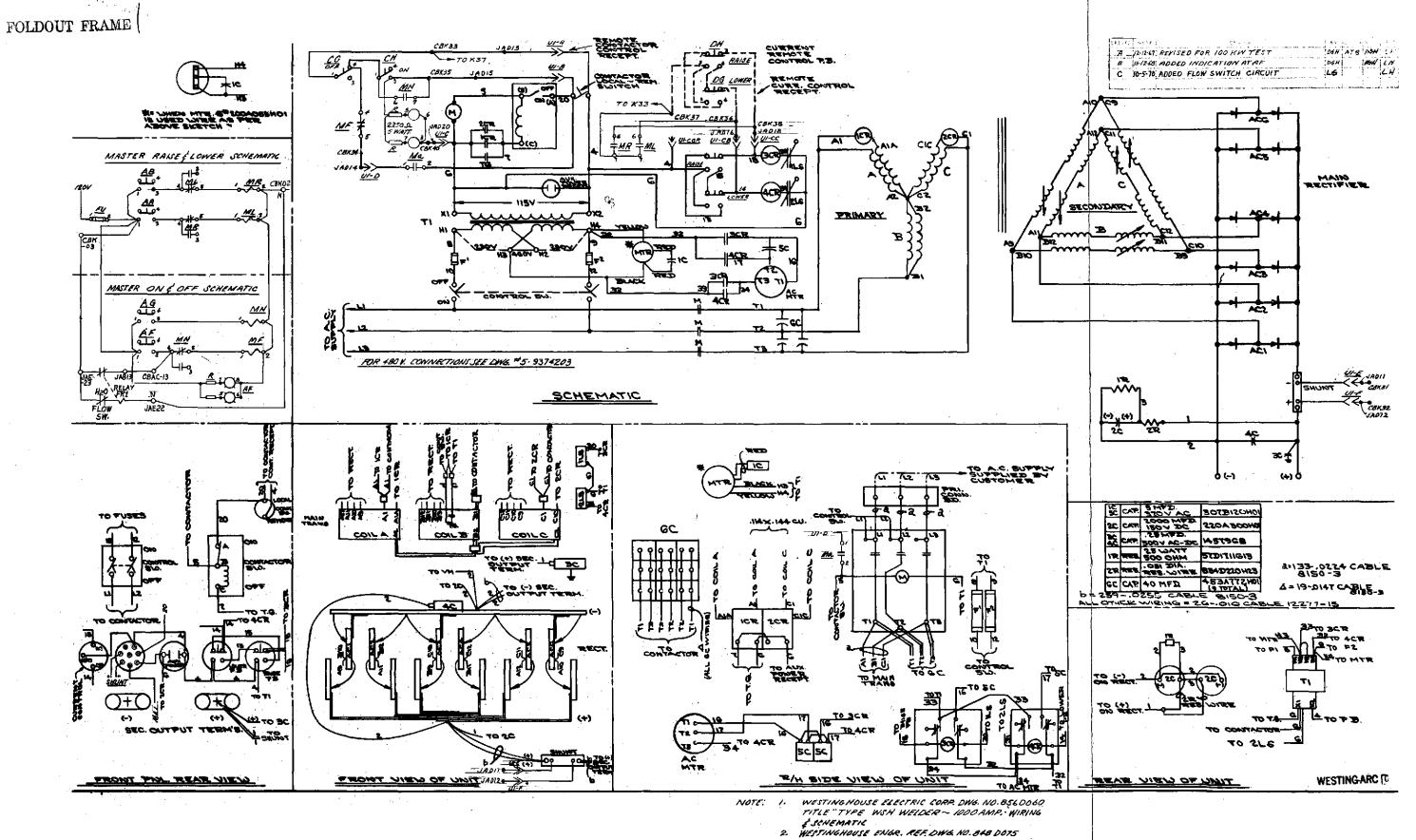


Fig. B-15. Building 148 100-kW test valves schematic diagram



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Fig. B-16. Magnetohydrodynamic facility type WSH welder 1000 A, unit 1, wiring and schematic

NOTES: I REF NO. WESTINGHOUSE ELECTRIC CORP DWG NO. 856D059
TITLE "WSH WELDER ~ 1000 AMP - WIRING &
SCHEMATIC"
2 WESTINGHOUSE ENGR. REF DWG NO.848D075

Fig. B-17. Magnetohydrodynamic facility type WSH welder 1000 A, unit 2, wiring and schematic

FRONT PAL. REAR VIELD

WESTING-ARC (15)

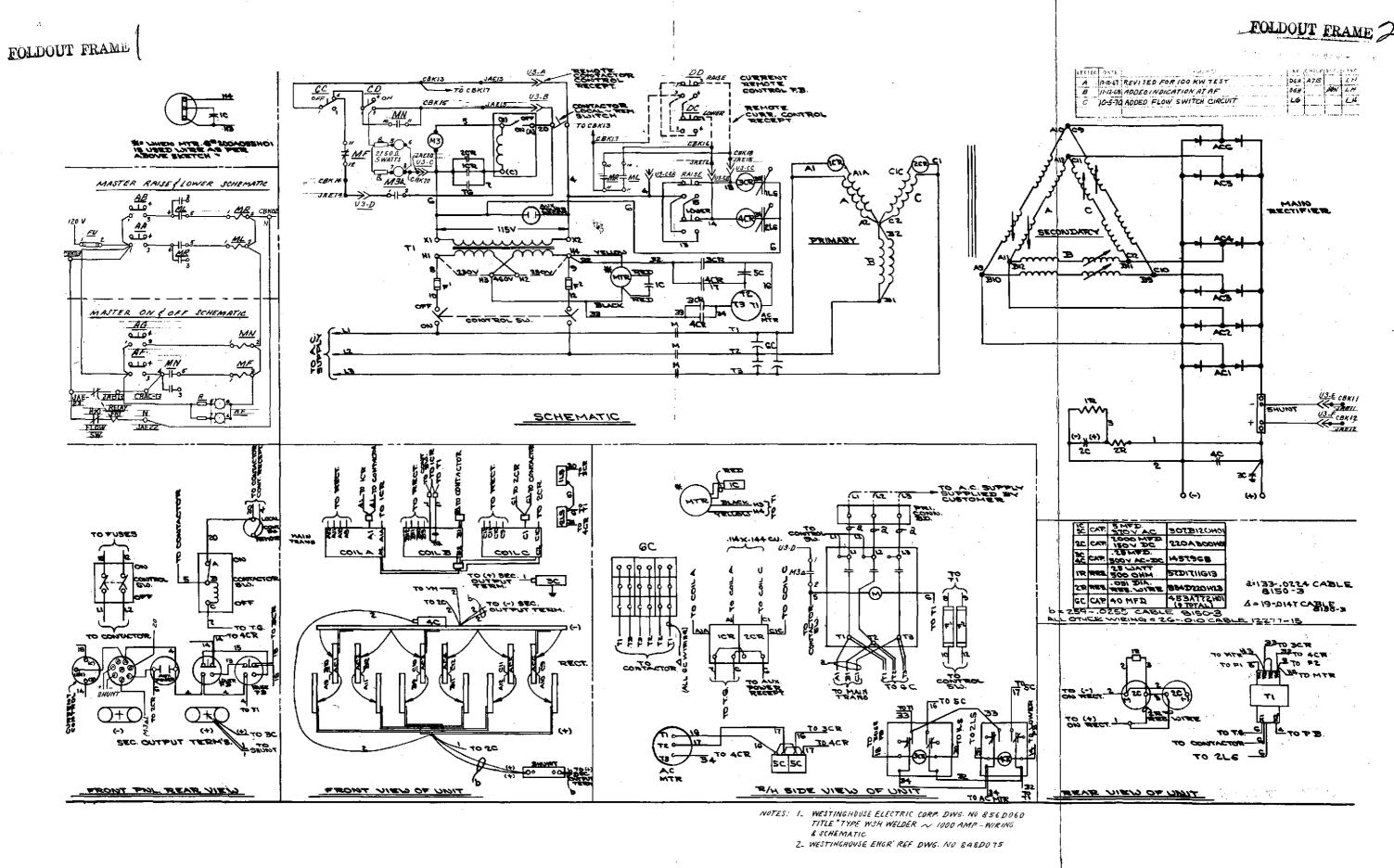
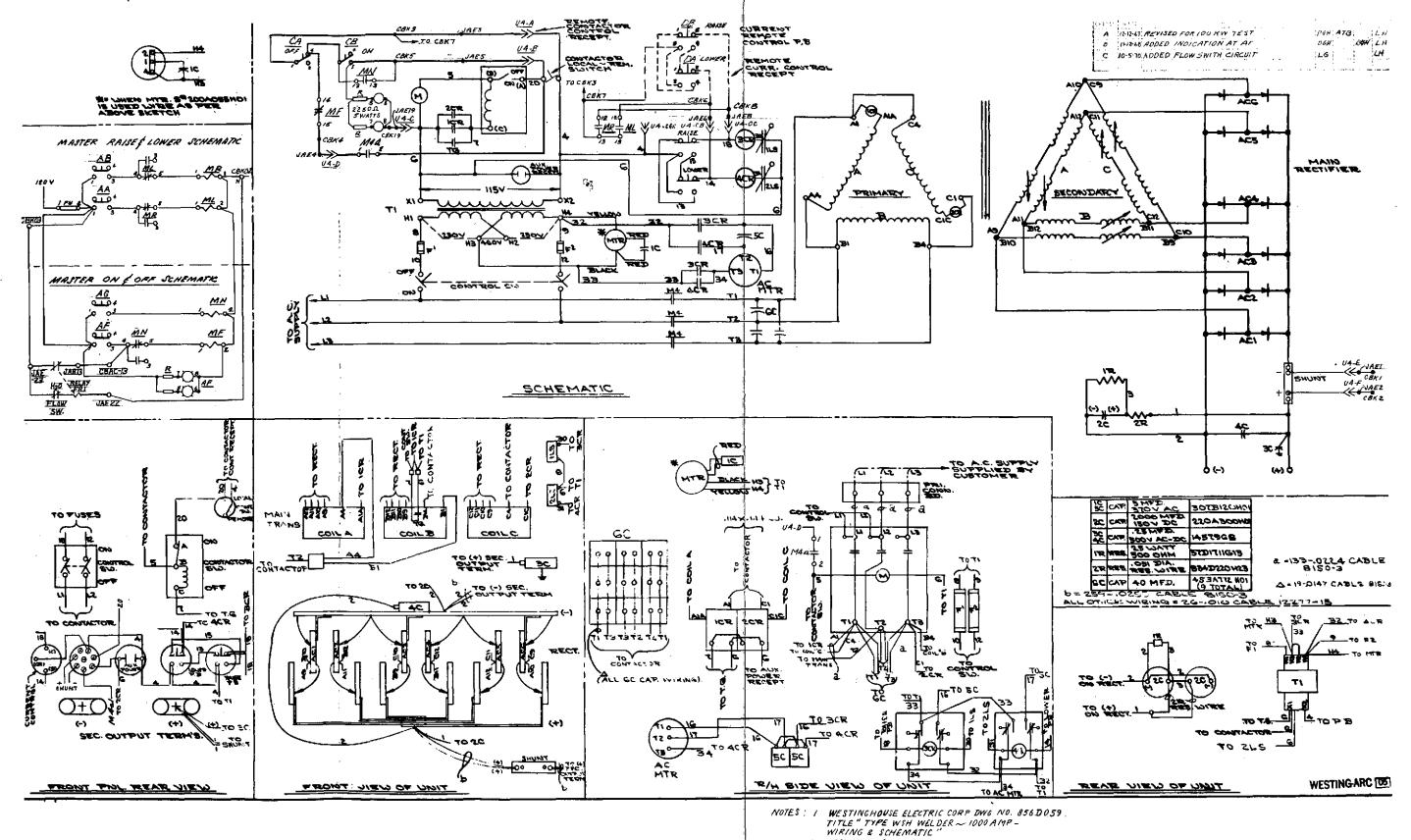


Fig. B-18. Magnetohydrodynamic facility type WSH welder 1000 A, unit 3, wiring and schematic



2 WESTINGHOUSE ENGR REF DWG.NO 848D075

Fig. B-19. Magnetohydrodynamic facility type WSH welder 1000 A, unit 4, wiring and schematic

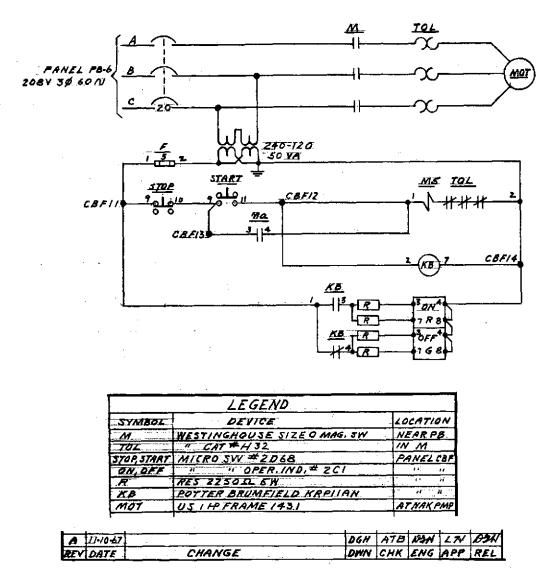


Fig. B-20. Building 148 NaK pump blower schematic diagram

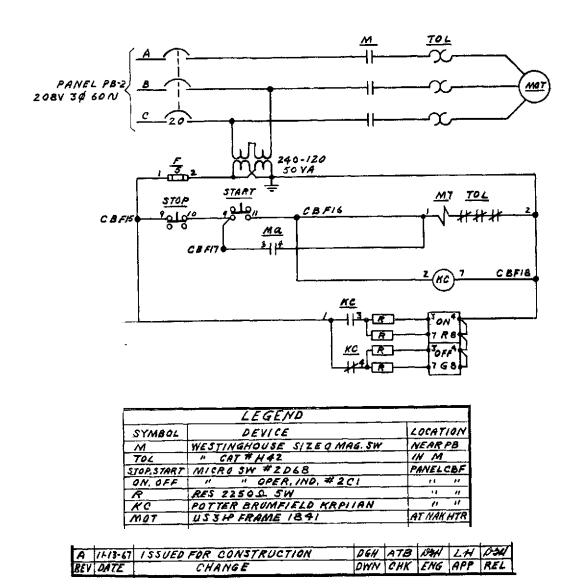


Fig. B-21. Building 148 heat exchanger blower schematic diagram

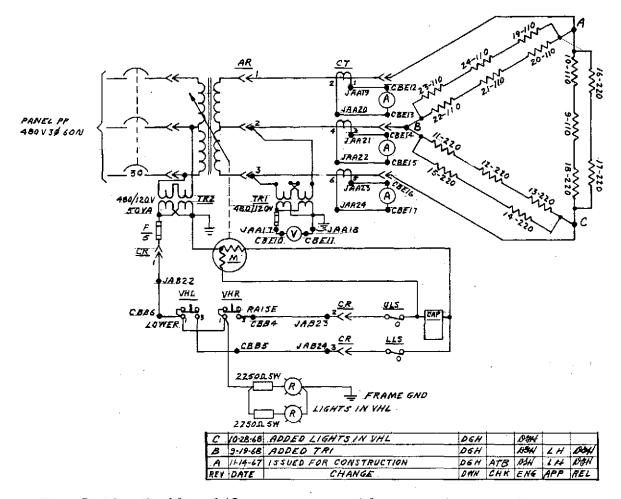


Fig. B-22. Building 148 vacuum vessel heater schematic diagram

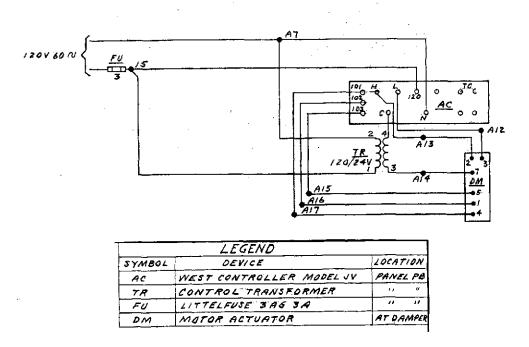
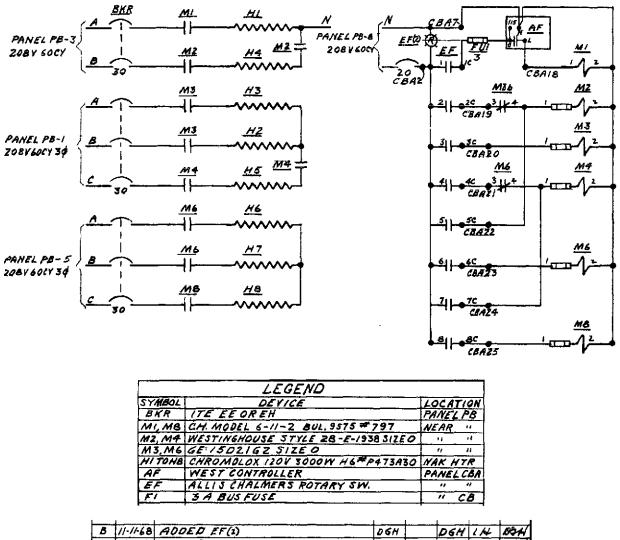
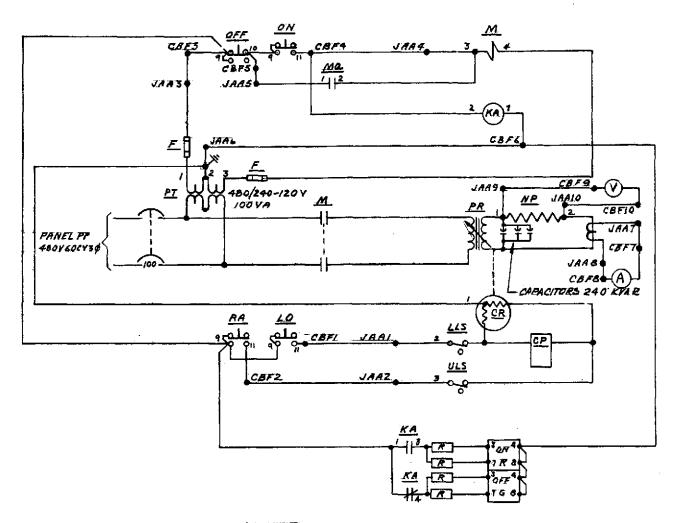


Fig. B-23. Building 148 damper control schematic diagram



	F	I 3 A BUS FUSE			" C	8	
B	11-11-68	ADDED EF(1)	DGH		DGH	14	834
A	11-3-67	ISSUED FOR CONSTRUCTION	DGH	ATB	DGH	LH	DON
REV	DATE	CHANGE	DWN	CHK	ENS	APP	REL

Fig. B-24. Building 148 100-kW test, NaK heater schematic diagram



MOTES

L. CAPACITORS CONSIST OF 2 BANKS OF 480V. 16 UNITS (TOTAL DE 240 KVAR)
MOUNT, BANKS ON EAST WALL DE RECTIFIER
ALCOVE IMMEDIATELY UNDER GUTTER,
CONNECT TO SECONDARY TERMINALS
OF VARIABLE TRANSFORMER W/
2 - # 4/0 CABLE IN 1/2" FLEX CONDUIT.

- 2. CHECK OUT CAPACITORS PRIOR TO COMMECTION
- 3. RECONNECT EXIST CARACITORS
 FOR LITHTUM PUMP AND CESIUM
 PUMP AS REQUIRED.

C	10-5-70	CHANGED CAPACITORS TO 240 KVAR	LG.		414	WP	LH
		ADD CAPACITORS TO NAK PUMP	RVS				
A	11.667	ISSUED FOR CONSTRUCTION	DGH	ATB	1344	ZH	DGN
REY	DATE	CHANGE	DWN	CHK	ENG.	APPY	REL

Fig. B-25. Building 148 NaK pump schematic diagram

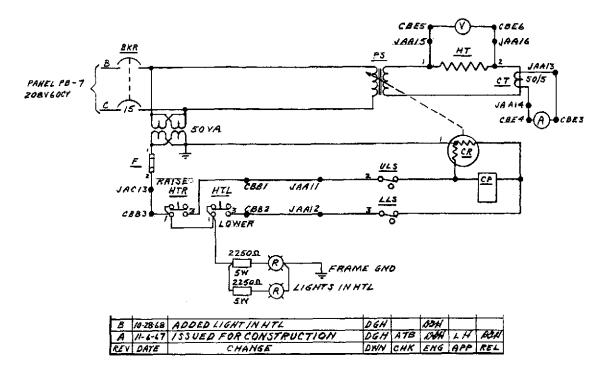


Fig. B-26. Building 148 hot trap schematic diagram

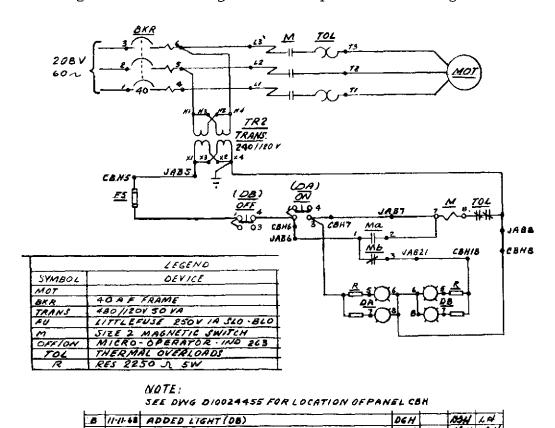
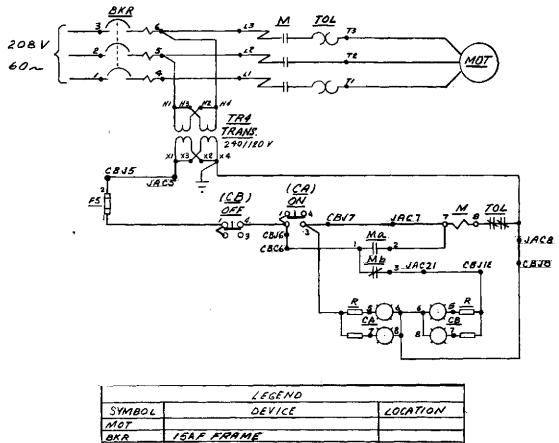


Fig. B-27. Magnetohydrodynamic facility 15-hp blower schematic diagram

CHANGE

A 12-8-67 REVISED FOR JOOKY TEST

DON ATB WAN BAN



	LEGEND									
SYMBOL	DEVICE	LOCATION								
MOT										
BKR	ISAF FRAME									
TRANS	480/120V 50VA									
F5	LITTLE FUSE IA SLO- BLO	PANEL CBC								
M	SIZE I MAGNETIC SWITCH									
CAFCB	MICRO-SWITCH 2068	PANEL CBC								
TOL	THERMAL OVERLOADS									
R	RES. 2250 SL 5W	PANEL CBC								
PO	MICRO - OPERATOR - IND 2CI	22 21								

NOTE:

SEE DWG DIOOZ4455 FOR LOCATION OF PANEL CBI

1	8	11-11-68	ADDED LIGHT (CB)	DGH		1954	LH	DON
	A	12-8-67	REVISED FOR 100 KW TEST	DGH	ATE	DON	LH	1034
	REY	DATE	CHANGE	DWN.	CHK	ENG	APP	REL

Fig. B-28. Magnetohydrodynamic facility 1-1/2-hp blower schematic diagram

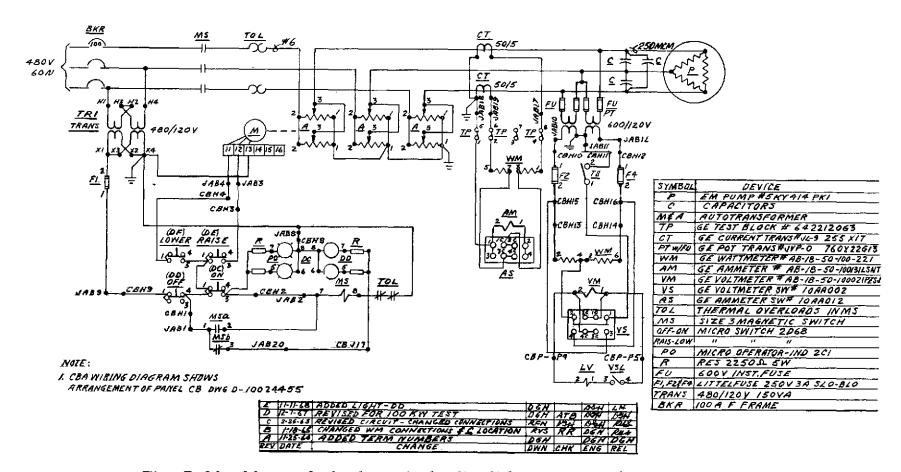


Fig. B-29. Magnetohydrodynamic facility lithium pump schematic diagram

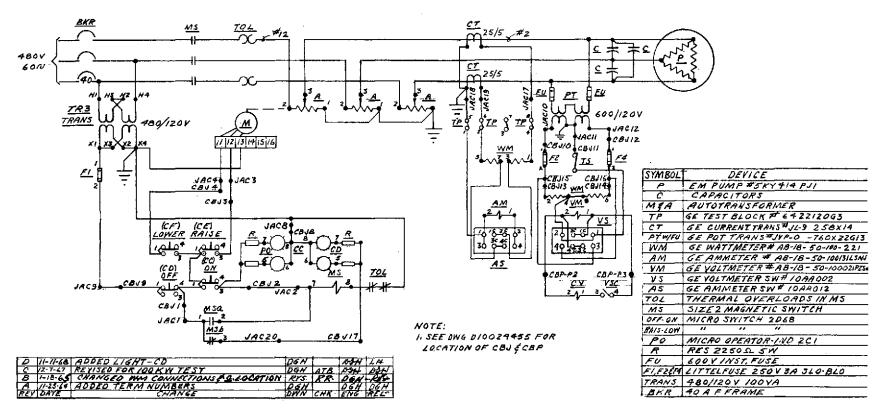
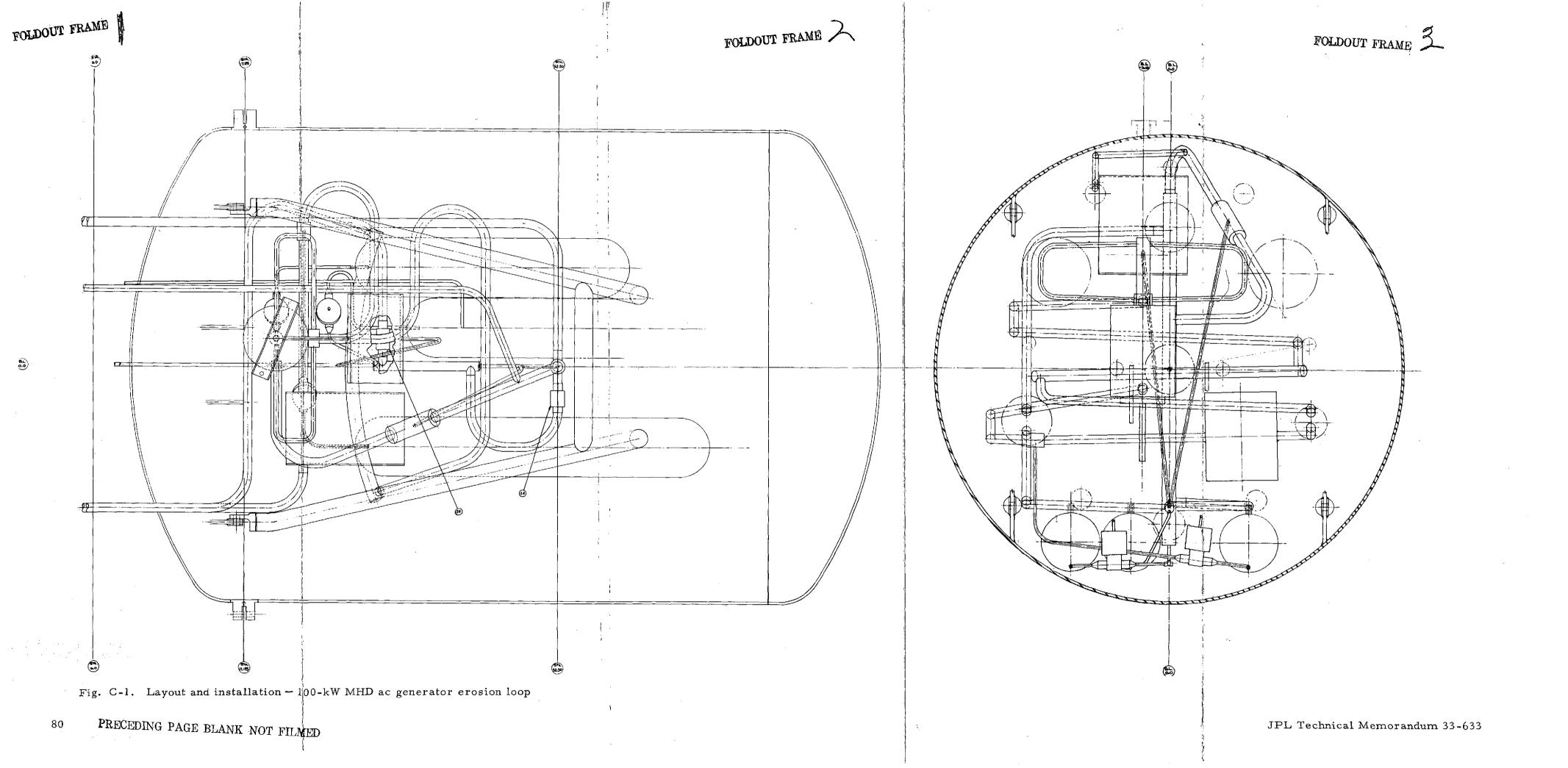


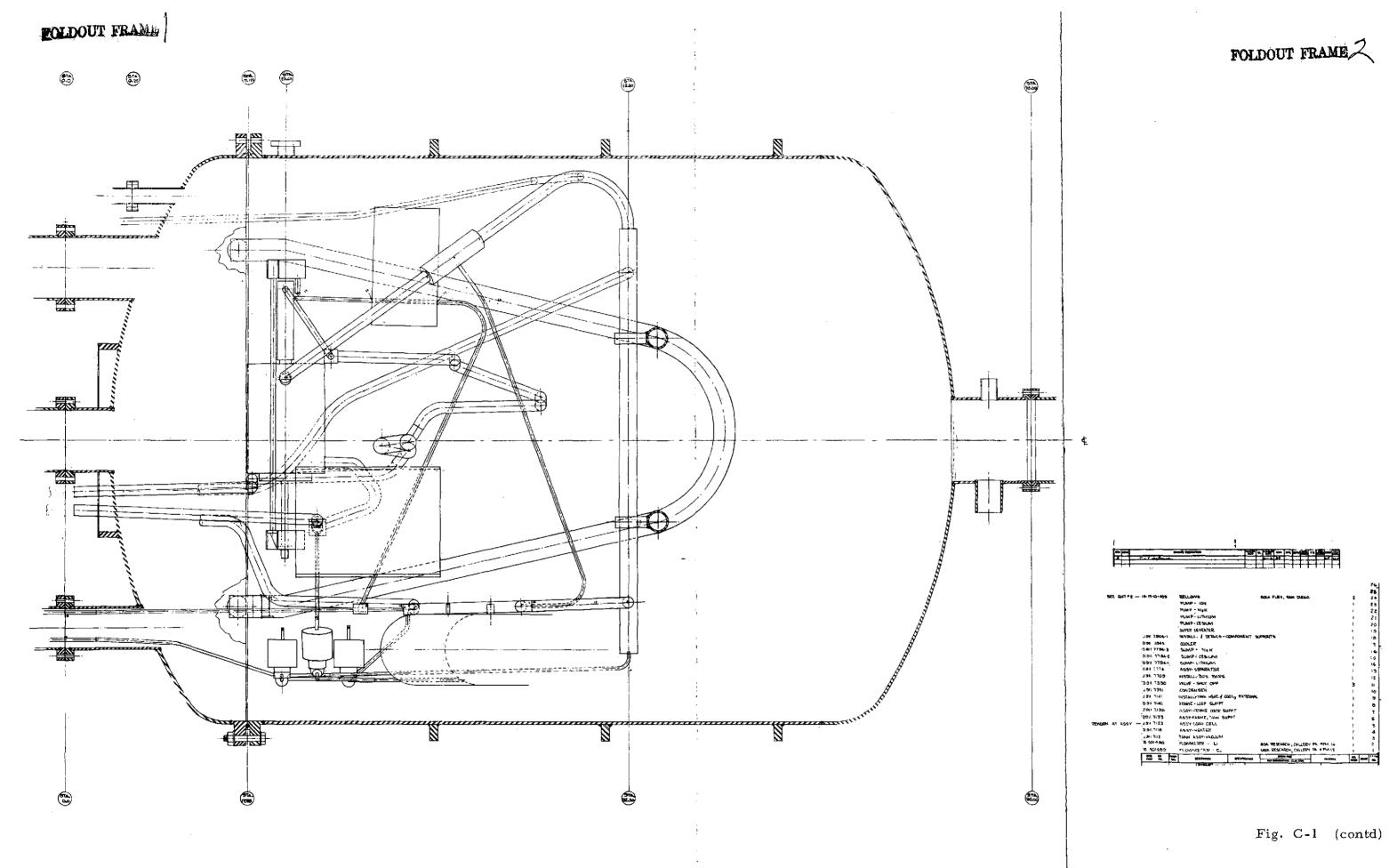
Fig. B-30. Magnetohydrodynamic facility cesium pump schematic diagram

APPENDIX C

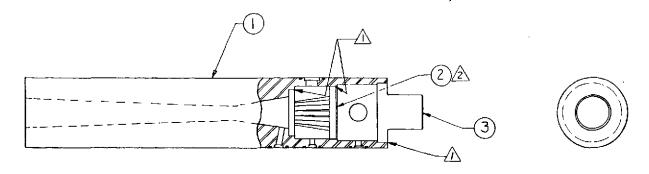
FABRICATION DRAWINGS OF TEST SYSTEM

The fabrication drawings of the cesium-lithium test system are included in this appendix (see Figs. C-1 through C-53). In some cases minor deviations and/or modifications have been made for the reasons discussed in the text. However, the essential features of the components and piping arrangement are identical to the drawings.





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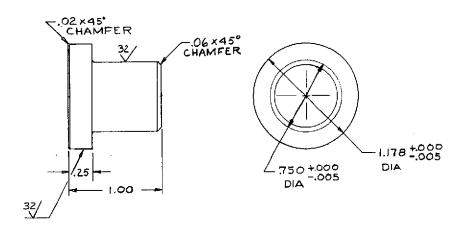


REMOVE APERTURE PLATE FROM NEEDLE ASSY. & WELD IN POSITION, THEN INSTALL NEEDLE ASSY & WELD.

ALL WELDS TO BE ELECTRON BEAM.

C 911	-7274		PLUG, HOUSING				1	3 7
D91	-727	5	NEEDLE ASSY	1				2
J911	-727	3	HOUSING				<u>į L ,</u>	
DW	G OR	DAS		SPECIFICATION	STOCK SIZE	MATERIAL	NO. REOD	FIND
PAF	PART NO.		DESCRIPTION	arecirication [REF DESIGNATION - ELEC DWG	MATERIAL		NQ.

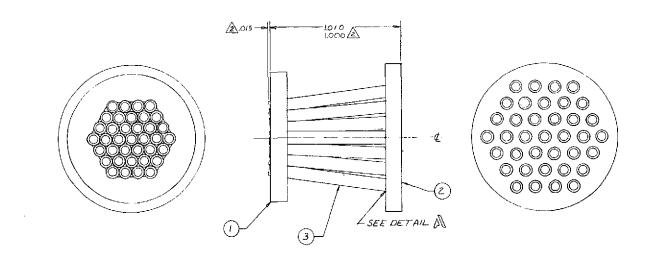
Fig. C-2. Weldment injector assembly



- 3 MACHINE FINISH 125%.
- 2. BREAK CORNERS .005-DIS RAD.
- I MACHINED FILLET RAD. .020.

PLUG		14 DIA 12 LG	Cb-17.Zr
DESCRIPTION	SPECIFICATION .	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL

Fig. C-3. Plug, housing injector assembly



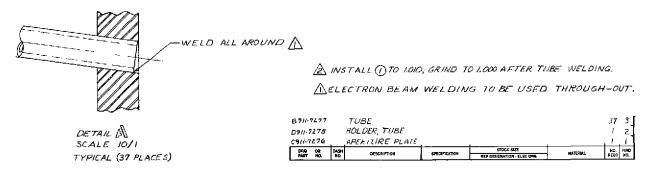
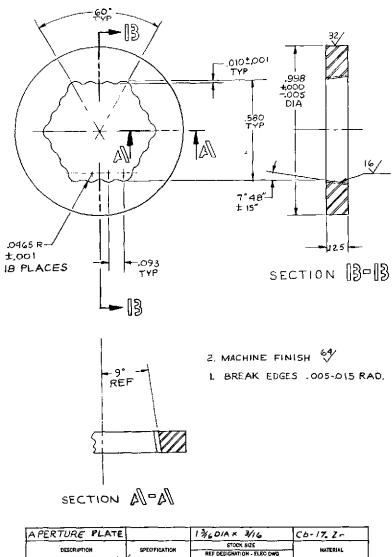


Fig. C-4. Needle assembly



STOCK SIZE
REF DESIGNATION - ELEC DWG

Fig. C-5. Aperture plate



I. CLEAN & DEBURR TUBE ENDS. MEASURE & RECORD I.D. & WALL ON ALL TUBES.

TUBING		0935 O.D. 014 WALL	Cb-17. Zr
DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL

Fig. C-6. Tube, needle assembly

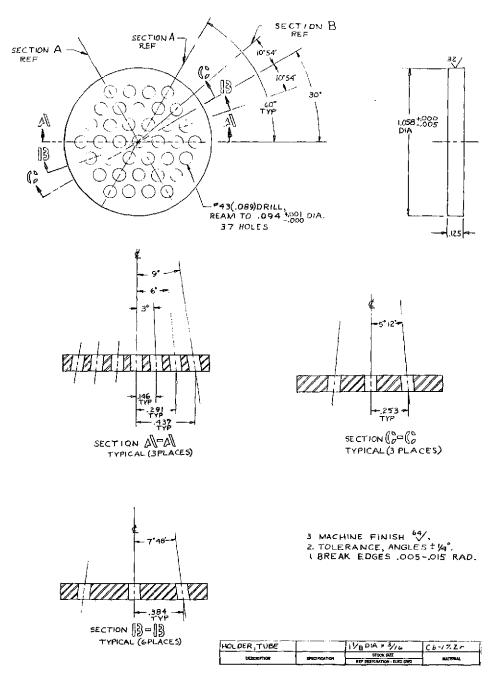
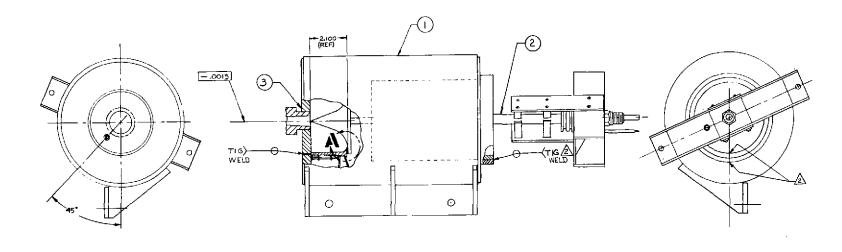
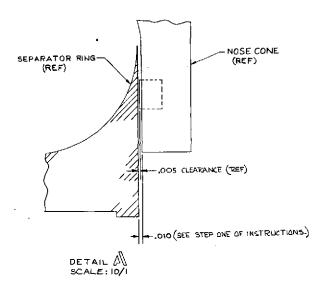


Fig. C-7. Holder, tube





ASSEMBLY INSTRUCTIONS

STEP NO. 1. INSERT @ INTO ① AS SHOWN. THE DIMENSION SHOWN IN DETAIL "A" IS DESIGN DIMENSION AND MUST BE HELD TO ±.001. (USE .010 SHIM STOCK, REMOVE AFTER WELDING). WELD ① & ② AS SHOWN.

STEP NO.2. INSTALL 3 INTO () AND WELD AS SHOWN.

NOTE: PRESS 3 LIGHTLY UNTIL IT BOTTOMS OUT ON THE

STEP OF (). THIS WILL ESTABLISH THE 2:100 REF DIM-

STEP NO.3 COVER OR PLUG ALL PORTS, ETC.

ALIGN INDEX MARKS : USE FIXTURE JOHT802-1 & JOHT802-2.

I. AFTER WELDING STORE IN PROPER CONTAINER TO PREVENT DAMAGE.

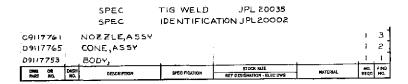


Fig. C-8. Separator - 100-kW erosion loop

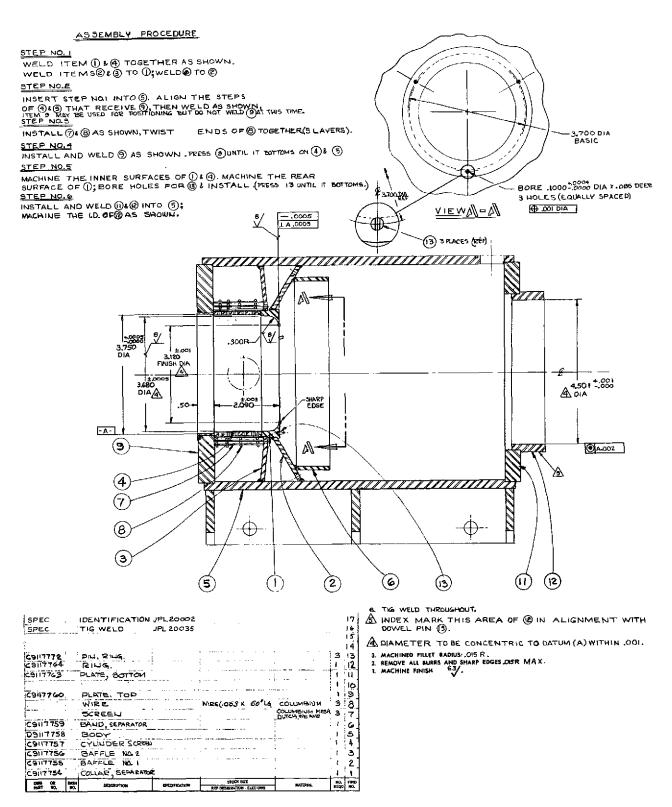
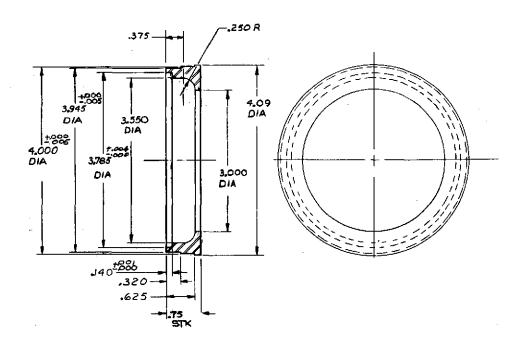


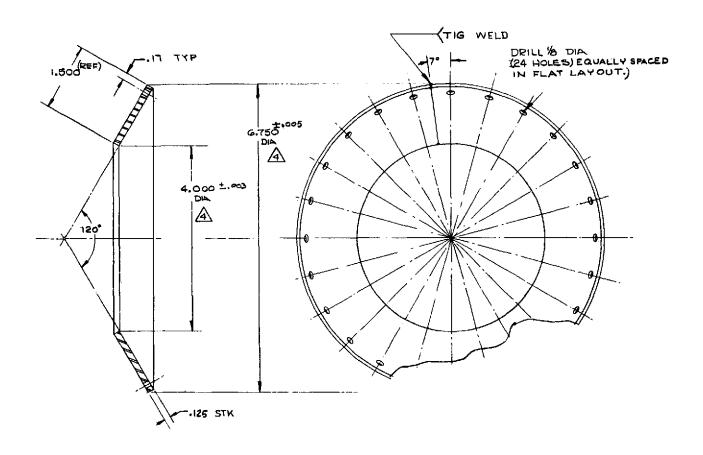
Fig. C-9. Assembly, body, separator - 100 kW erosion loop



- 4 ALL DIAMETERS TO BE CONCENTRIC WITHIN .005, EXCEPT 4.09 DA.
- 3. MACHINED FILLET RADIUS: .005 R
 2. REMOVE ALL BURRS AND SHARP EDGES .010 R .
 1. MACHINE FINISH 63.

SPEC			IDENTIFIC ATION	JPL 2000Z			L	3
								2_
			COLLAR		3/4 ×41/8 DIA	Cb-1% Zr		1
OWG PART	OR NO.	DASH NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NO. REQO	FIND NO.

Fig. C-10. Collar separator - 100-kW erosion loop

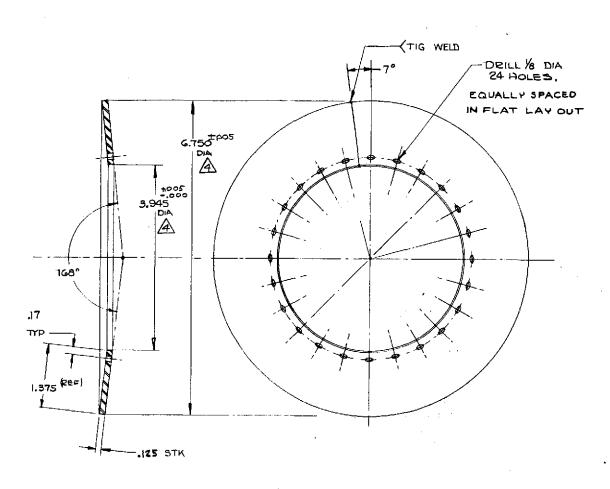


A TO BE CONCENTRIC WITHIN . OOI AFTER WELDING.

- 3. MACHINED FILLET RADIUS:
- 2. REMOVE ALL BURRS AND SHARP EDGES .015 R MAX.
 AACHINE FINISH 63/

SPEC		TIG WELD	JPL 20035				
SPEC		IDENTIFICATION	JPL 20002				
		BAFFLE MI		.125 x 8.25 DIA	Cb - 1% Zr		T
DWG QR PART NO.	DASH MO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	KO. REQD	FIND NO.

Fig. C-11. Baffle I, separator -100-kW erosion loop

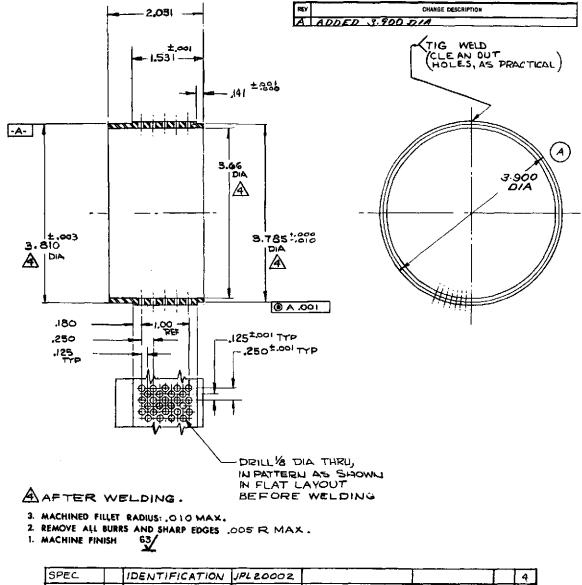


A TO BE CONCENTRIC WITHIN . OO I AFTER WELDING.

- 3. MACHINED FILLET RADIUS:
- 2. REMOVE ALL BURRS AND SHARP EDGES . 0 15 R MAX.
- 1. MACHINE FINISH 63

SPEC			IDENTIFICATION	JPL20002		-	Γ	
SPEC	\Box		TIG WELD	JPL 20035				
			BAFFLE NO. 2		.125 X 7 DIA	Co-18 Zr.		7
DWG GF PART NO		NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	HO, REQD	FIND NO.

Fig. C-12. Baffle 2, separator - 100-kW erosion loop



SPEC			IDENTIFICATION	JPL 20002			T	4
SPEC			TIG WELD	JPL 20035				3
							7	2
			CYLINDER SCREEN		3/16 × 2 1/6 × 12 3/8LG.	Cb-18 Zr	1	Ī
DWG PART	OR NO.	DASH NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NO. REQD	FIND NO.

Fig. C-13. Cylinder screen, separator - 100-kW erosion loop

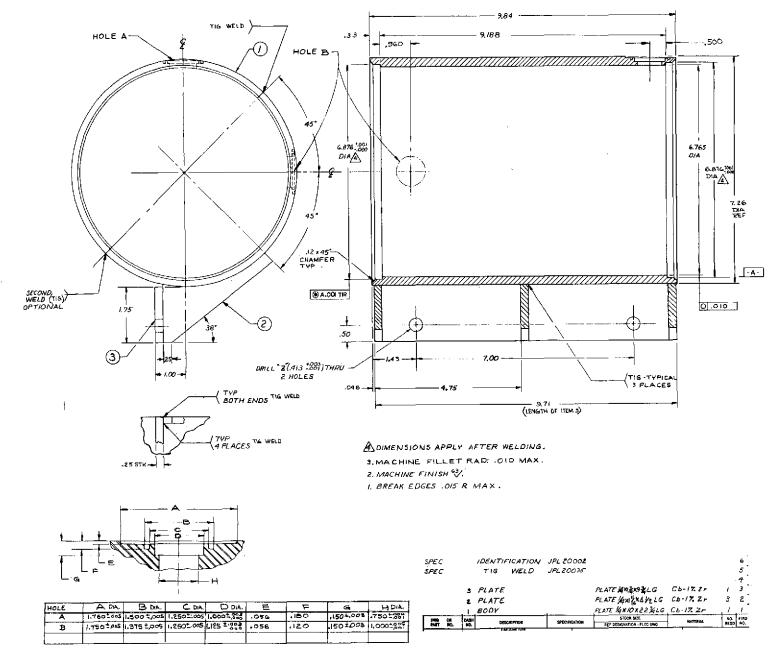
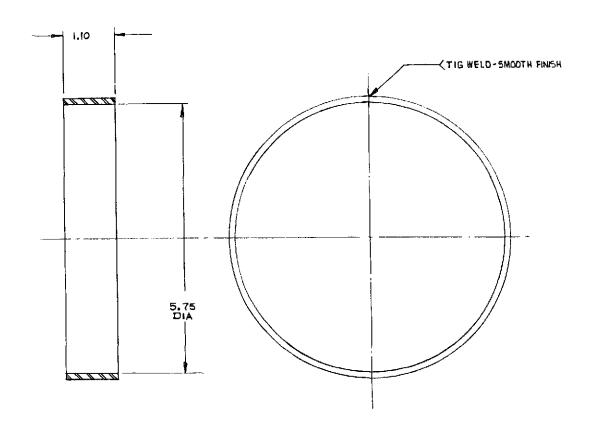


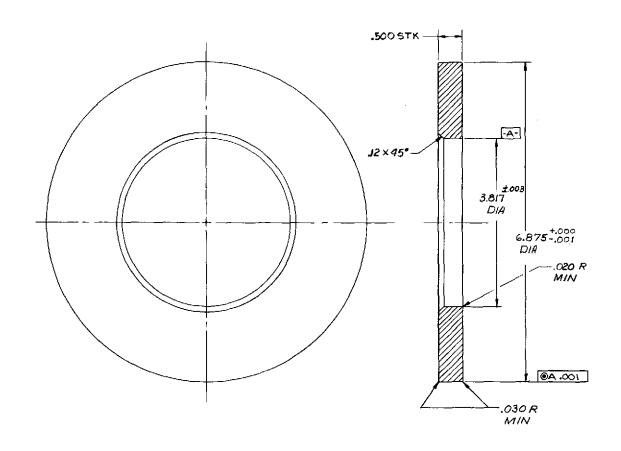
Fig. C-14. Body, separator - 100-kW erosion loop



- 4. DIMENSONS AFTER WELDING.
- 3. MACHINED FILLET RADIUS:
- 2. REMOVE ALL BURRS AND SHARP EDGES .. 03 R MAX.
 1. MACHINE FINISH 63

SPEC			DENTIFICATION	JPL20002				
SPEC			TIG WELD	JPL20035				_
		1	BAND		125 × 1 /8 × 19 LG	Cb-17 Zr		
DWG PART	OR NO.	DASH NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NO. REQD	FIND NO.

Fig. C-15. Band, separator — 100-kW erosion loop



2. BREAK EDGES.OIS R.

1. MACHINE FINISH 63/.

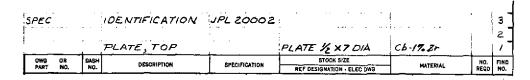


Fig. C-16. Plate, top, separator -100-kW erosion loop

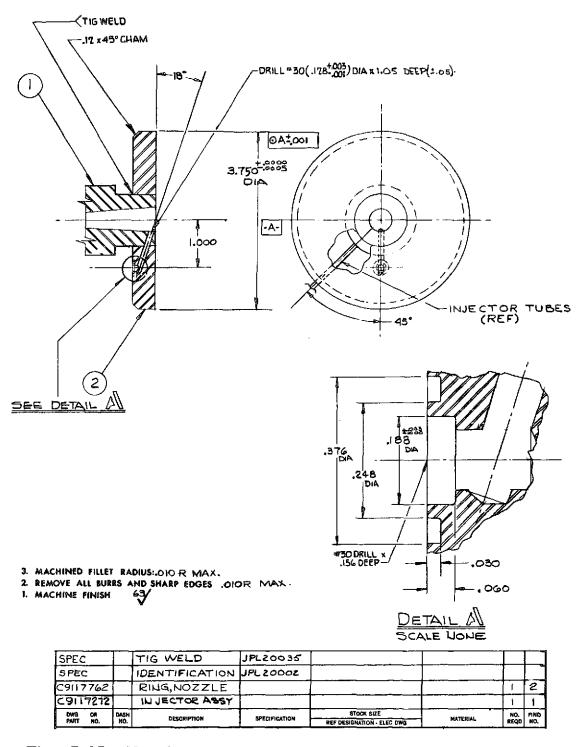
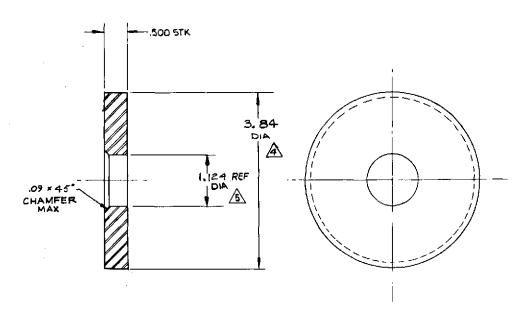


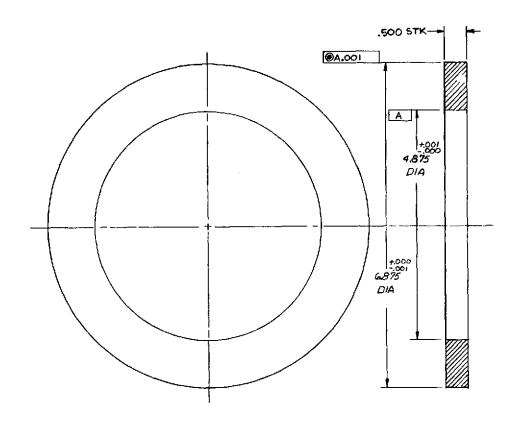
Fig. C-17. Nozzle assembly, separator -100-kW erosion loop



- AMACH. AS REQD TO FIT CONTROL NOTELE.
- MAKE FROM CORE REMOVED FROM C9117763, IF FEASIBLE.
- 3. MACHINED FILLET RADIUS:
 2. REMOVE ALL BURRS AND SHARP EDGES .015R MAX.
 1. MACHINE FINISH 63/

.]	SPEC			IDENTIFICATION	JPL 2000Z				2
A				RING		1/2 X 3 7/8 DIA	Cb-18 Zr		
	DWG PART	OR NO.	DASH OH	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	ND. REQD	FIND HO.

Fig. C-18. Ring, nozzle, separator - 100-kW erosion loop



- 4. THE REMOVED CORE WILL BE USED TO PRODUCE C9117762.
- 3. MACHINED FILLET RADIUS:
- 2. REMOVE ALL BURRS AND SHARP EDGES .030 R MAX .
- 1. MACHINE FINISH 63/

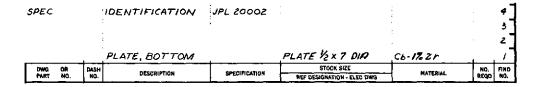
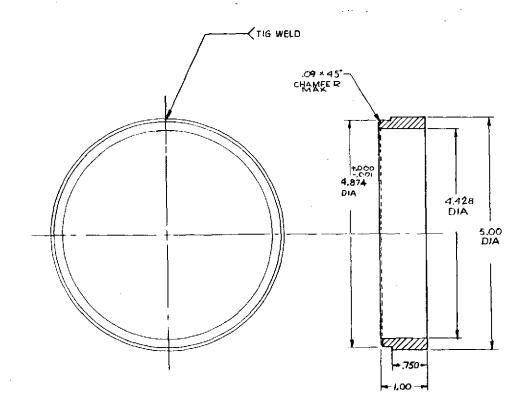


Fig. C-19. Plate, bottom, separator - 100-kW erosion loop



- 3. MACHINED FILLET RADIUS: 030 MAX.
- 2. REMOVE ALL BURRS AND SHARP EDGES .OIS R.
- 1. MACHINE FINISH 63

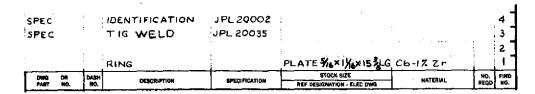


Fig. C-20. Ring, separator - 100-kW erosion loop

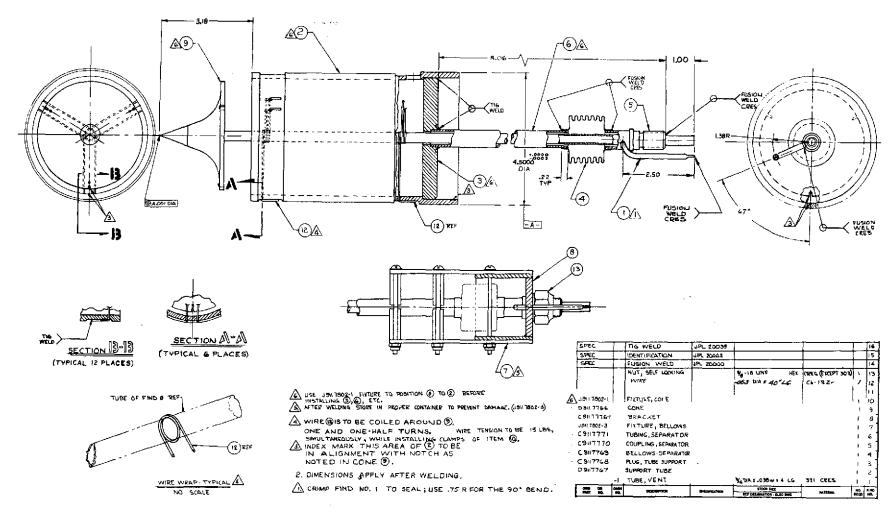


Fig. C-21. Assembly, cone and support, separator - 100-kW erosion loop

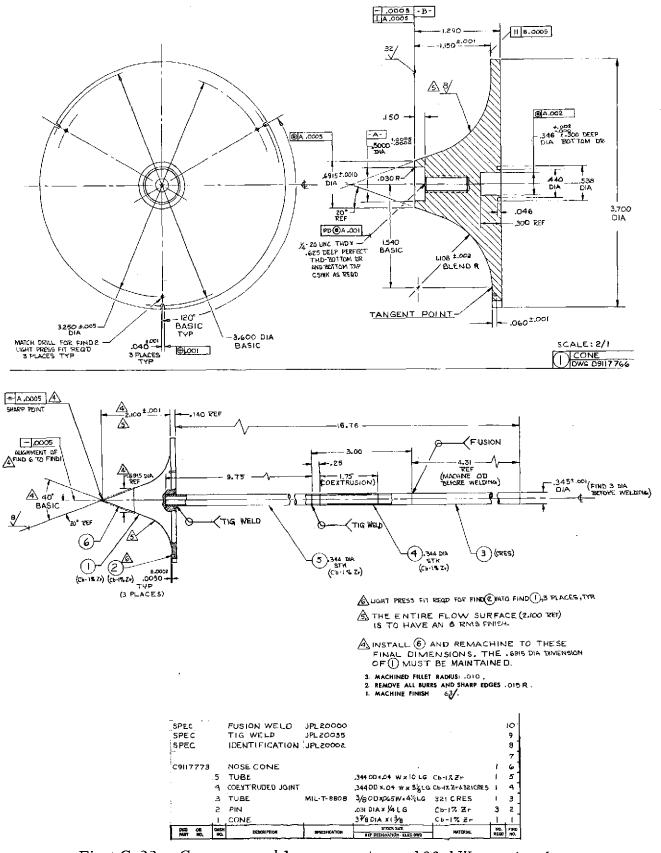


Fig. C-22. Cone assembly, separator - 100-kW erosion loop

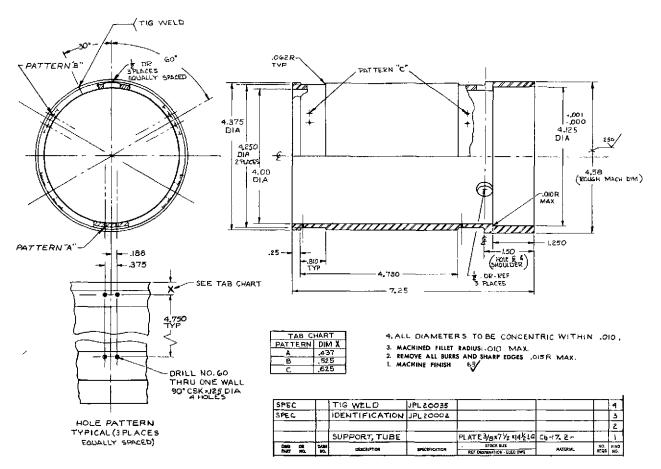
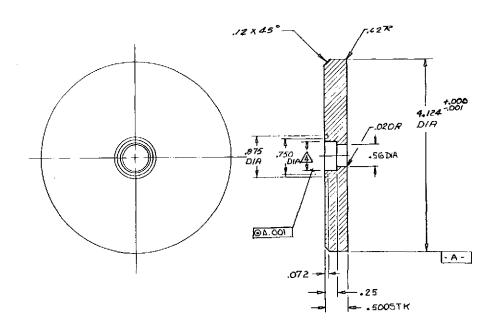


Fig. C-23. Support, tube, separator - 100-kW erosion loop



- 4. MATCH FIT WITH PART NO. C9117771, FOR SNUG FIT.
- 3. MACHINED FILLET RADIUS: . OIO MAX .
 2. REMOVE ALL BURRS AND SHARP EDGES . CHOR MAX .
- 1. MACHINE FINISH

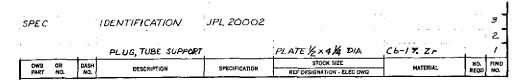
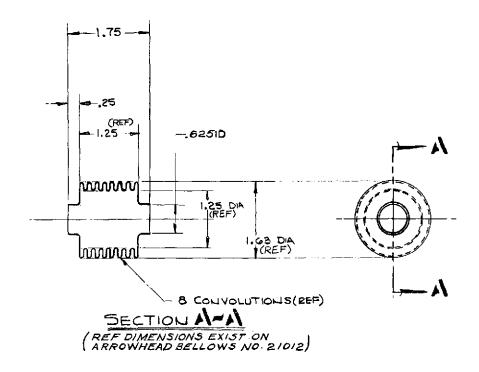


Fig. C-24. Plug, tube support-100-kW erosion loop separator



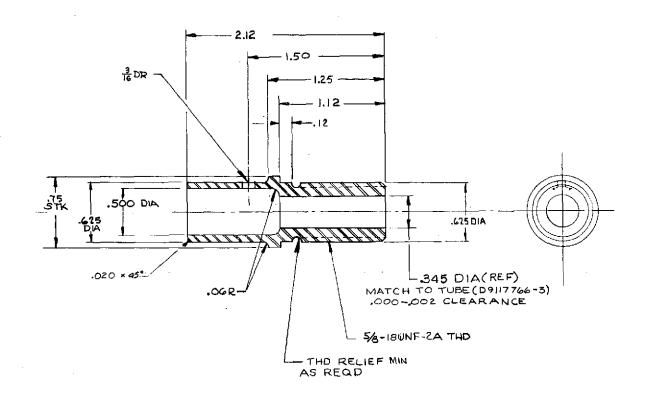
BELLOWS TO HAVE A NO. 6 END CUFF

TERMINATION, REDUCED DIAMETER AS SHOWN
MATERIAL .005; I PLY, 100 PSI AT 800°F,
MAX DEFLECTION .25; SPRING RATE GB/LB IN.;
EFFECTIVE AREA 1.63 SQ.IN.

ASIMILAR TO ARROWHEAD NO. 21012, ARROWHEAD PRODUCTS,
4411 KATELLA AVE.,
LOS ALAMITOS CALIF., OR EQUAL.
(BULLETIN NO. 501-R)

	SPEC		DENTIFICATION	JBF 50005				
\triangle			BELLOWS		SEE 🛆	347 CRES		
	DWG GR PART NO.	DASH NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NO. REQU	FIND NO.

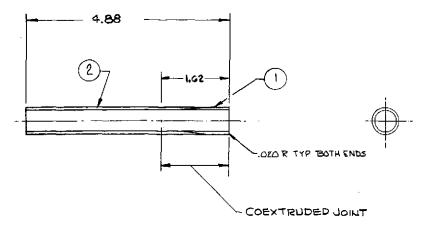
Fig. C-25. Bellows, separator - 100-kW erosion loop



- 3. MACHINED FILLET RADIUS: .040 MAX
- 2. REMOVE ALL BURRS AND SHARP EDGES .015 R MAX
 1. MACHINE FINISH 63/.

5PEC	<u>. </u>	IDENTIFICATION	JPL 20002				
		COUPLING		3/4 DIA X 2 1/2 LG	321CRES		
OWE OR PART NO.	DASH NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NO. REQD	FIND NO.

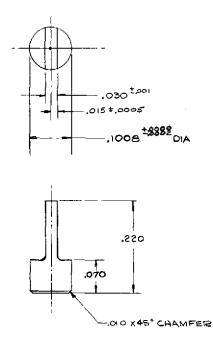
Fig. C-26. Coupling, separator - 100-kW erosion loop



- 3. MACHINED FILLET RADIUS:
 2. REMOVE ALL BURRS AND SHARP EDGES ,OOZ R MAX.
 1. MACHINE FINISH COMU.

SPEC	J .	IDENTIFICATION	JPL20002]]	3
	2	TUBING NA 2		625 00 x.50 I D	321 CRES	1	2
	T	TUBING NO. 1		.625 OD x.50 ID	Cb-122v.	- 1	-
DWG OR PART NO.	DASH No.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NO. REQO	FIND NO.

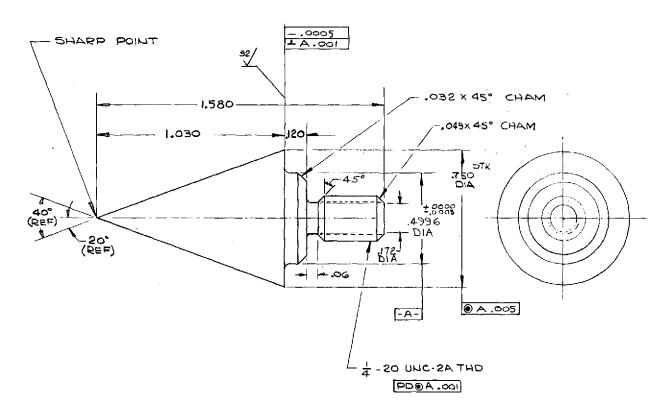
Fig. C-27. Tubing, separator -100-kW erosion loop



- 3. MACHINED FILLET RADIUS: OF R.
 2. REMOVE ALL BURRS AND SHARP EDGES 1005R MAX.
 1. MACHINE FINISH

SPEC		IDENTIFICATION	JPL 20002					
	4_							
		PIL		.125 DIA X	1/2 6	C6-122	L	
DWG OR PART NO.	DASH ND.	DESCRIPTION	SPECIFICATION	STOCK SIZ		MATERIAL	NO. REGD	MU'

Fig. C-28. Pin ring, separator - 100-kW erosion loop



- 4. MATERIAL TO BE DETERMINED BY THE COG. ENGR.
- 3. MACHINED FILLET RADIUS: ,OISR MAX.
- 2. REMOVE ALL BURRS AND SHARP EDGES
 1. MACHINE FINISH 63

SPEC		IDENTIFICATION	JPL 20002		I		6
	5	NOSE COME		34 DIAX 15/4 LG	SEE NOTE 4		5
	4	HOSE COME		34 DIAX 1 96 LG	SEE LIOTE 4		4
_	3	NOSE COME		34 DIA x 15/8 LG	SEE HOTE 4		3
	2	MOSE COME		3/4 DIAX 15/6 LG	SEE NOTE 4		2
	T	MOSE COME		3/4 DIA X 15/8 LG	SEE MOTE 4		1
DWG OR PART NO.	DASH HO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NO. REQD	F(MI NO.

Fig. C-29. Nose cone, separator - 100-kW erosion loop

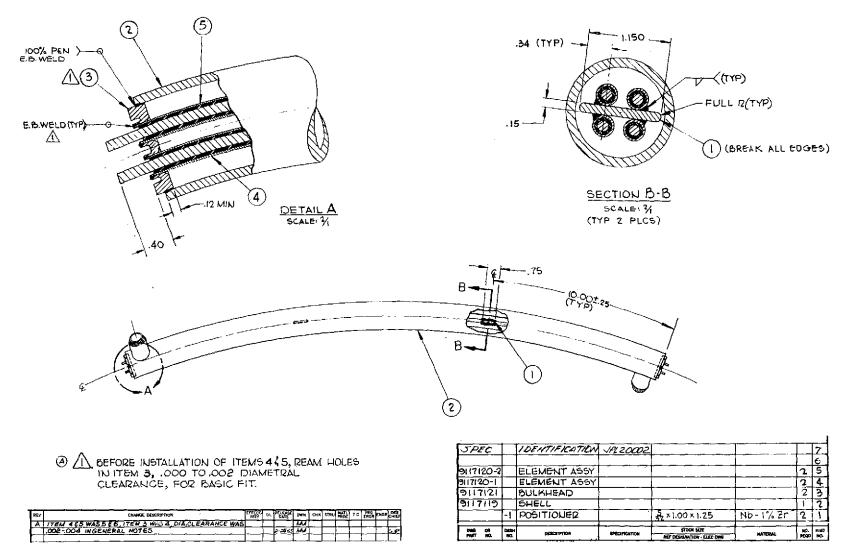


Fig. C-30. Heater assembly - 100-kW erosion loop

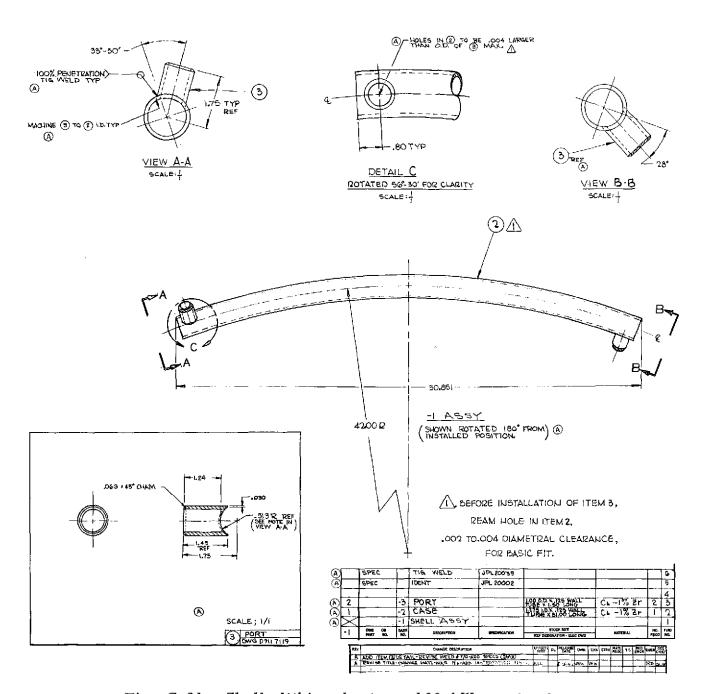


Fig. C-31. Shell, lithium heater -100-kW erosion loop

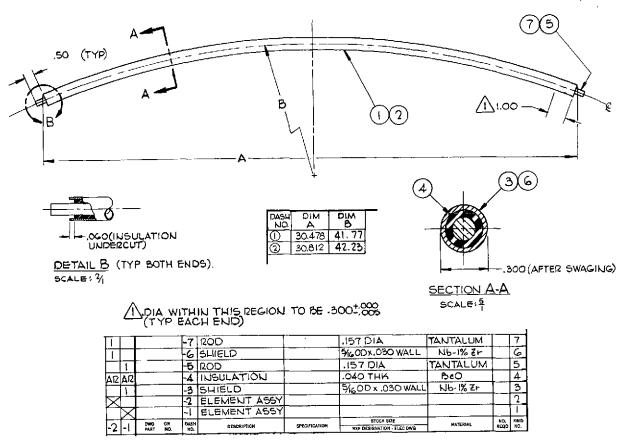


Fig. 32. Element assembly, lithium heater

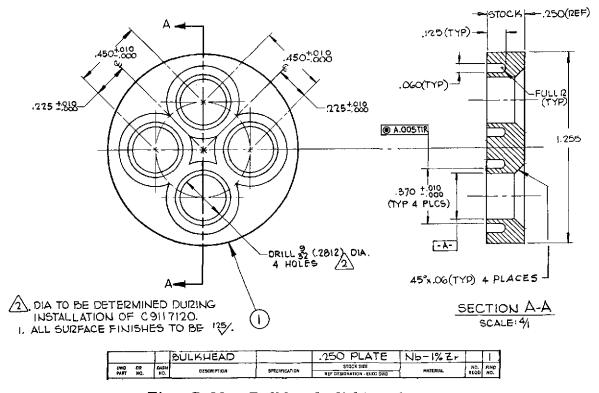
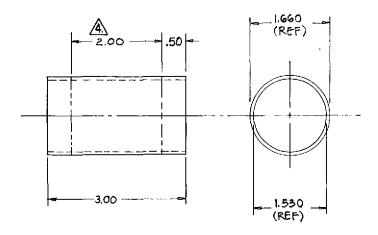


Fig. C-33. Bulkhead, lithium heater

JPL Technical Memorandum 33-633

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PROCURE FROM NUCLEAR METALS INC., CONCORD, MASS., OR EQUAL.

A DIFFUSION BOND LIMITS.

- 3. MACHINED FILLET RADIUS:
- 2. REMOVE ALL BURRS AND SHARP EDGES
- 1. MACHINE FINISH 63/

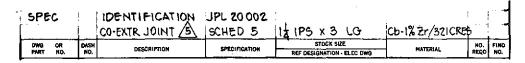


Fig. C-35. Joint, coextruded — erosion loop cesium condenser

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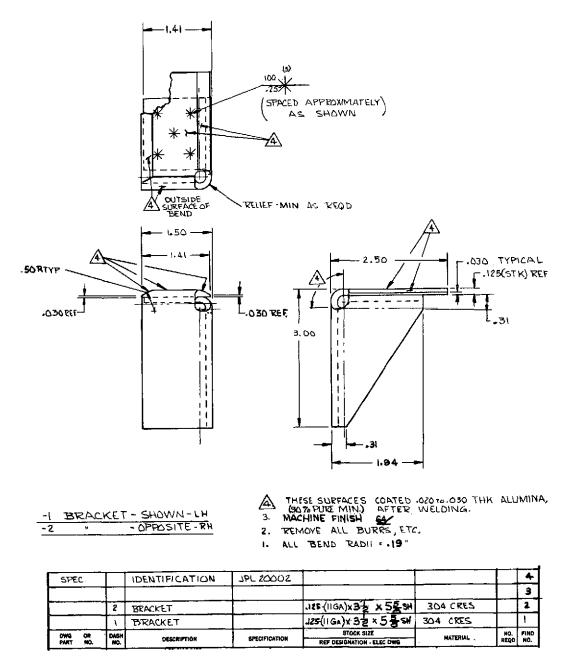
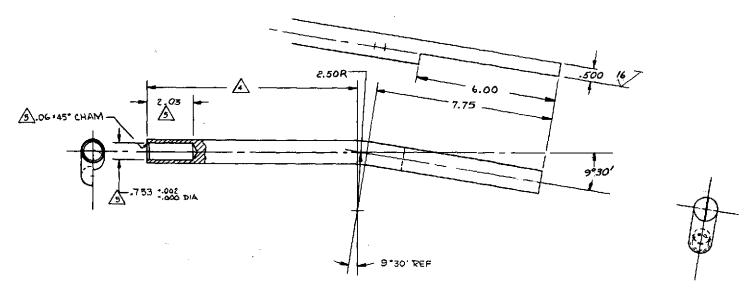


Fig. C-36. Bracket, bus support, inner (LH and RH)



A PERFORM THESE FUNCTIONS AFTER A

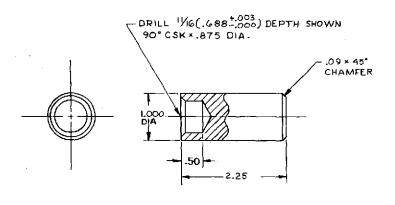
A DETERMINE LENGTH AT NEXT ASSY.

3. MACHINED FILLET RADIUS: . 030 R .

2 REMOVE ALL BURRS AND SHARP EDGES OBOR 1. MACHINE FINISH

ı	392	c	L .	IDENTIFICATION	JPL 20002			66 E	1
. [_		1	BAR		BAR I DIA × 18 4 LG	OFHC COPPER		[
	DWG PART	QR NO.	DASH NO.	DESCRIPTION	SPECIFICATION	8TOCK SIZE REF DESIGNATION - ÉLEC DWG	MATERIAL	NO. REQU	ŀ
				· · · · · · · · · · · · · · · · · · ·					_

Fig. C-37. Bar, bus, lead-in (RH)

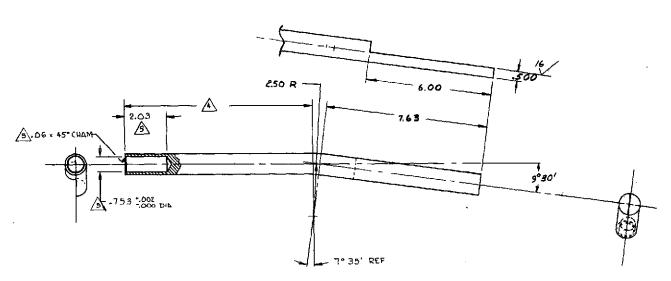


- 3. MACHINED FILLET RADIUS:
- 2. REMOVE ALL BURRS AND SHARP EDGES .DIS R.

 1. MACHINE FINISH 63

	SPEC		 	IDENTIFICATION	JPL 20002			<u></u>	3 1
. ‡			i	ADAPTER, AFT		BAR I"DIA X3 1/2 LG	347 CRES	-	1
	DWG PART	OR NO.	DASH NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	NC. REQD	FIND NO.

Fig. C-38. Adapter, aft



 $\widehat{\triangle}$ PERFORM THESE FUNCTIONS AFTER $\widehat{\triangle}$.

A DETERMINE LENGTH AT NEXT ASSY.

3. MACHINED FILLET RADIUS: .030 R .
2. REMOVE ALL BURRS AND SHARP EDGES .030 R
1. MACHINE FINISH 63

- [SPEC			IDENTIFICATION	JPL 2000 2			REF
ı			1	BAK		I DIA × 18 LG-BAR	OFHC COPPER	1
• •	DWG PART	OR NO	DASH NO.	DESCRIPTION	SPECIFICATION	STOCK SIZE REF DESIGNATION - ELEC DWG	MATERIAL	ND, REQD

Fig. C-39. Bar, bus, lead-in (LH)

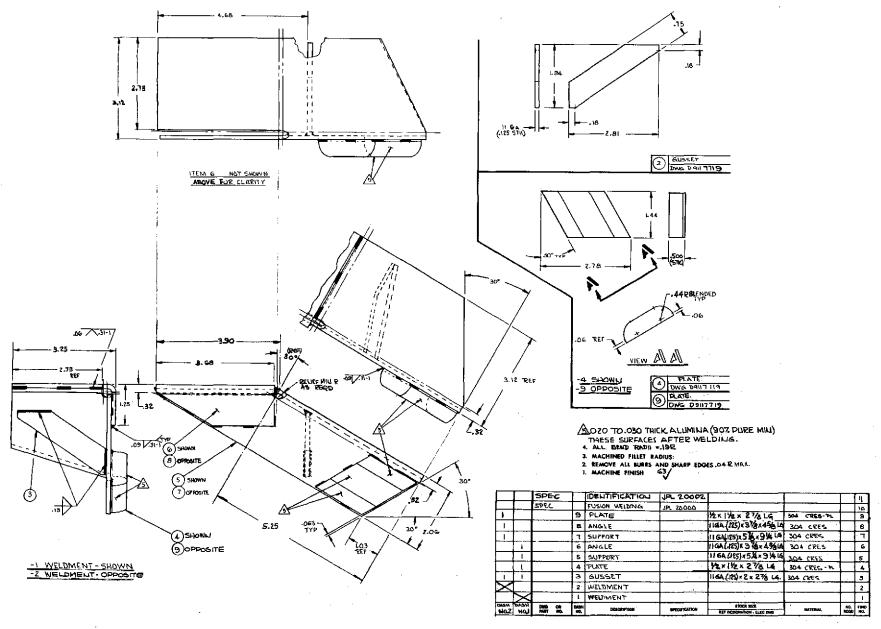


Fig. C-40. Bracket, bus support, outer

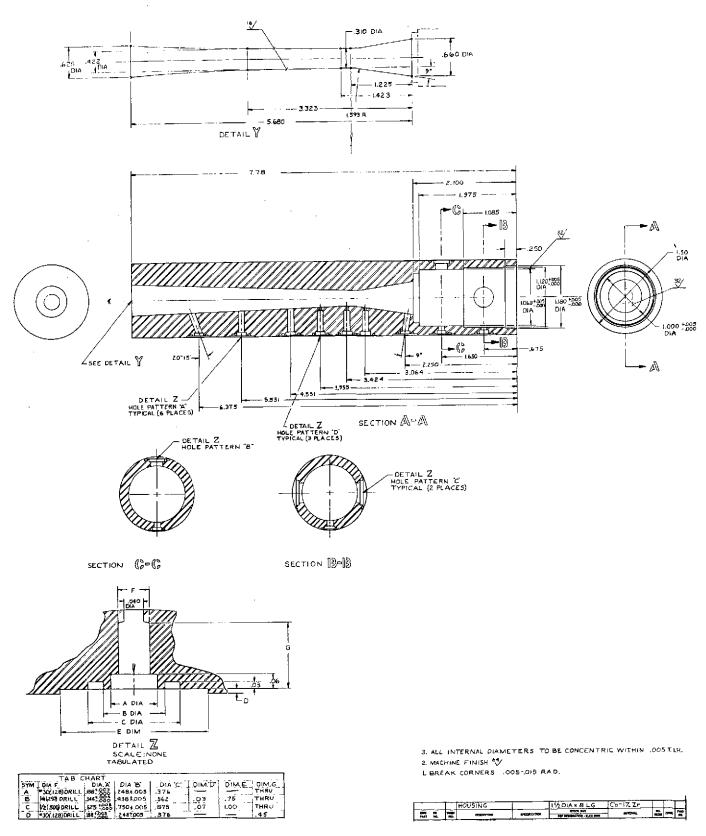


Fig. C-41. Housing, injector assembly

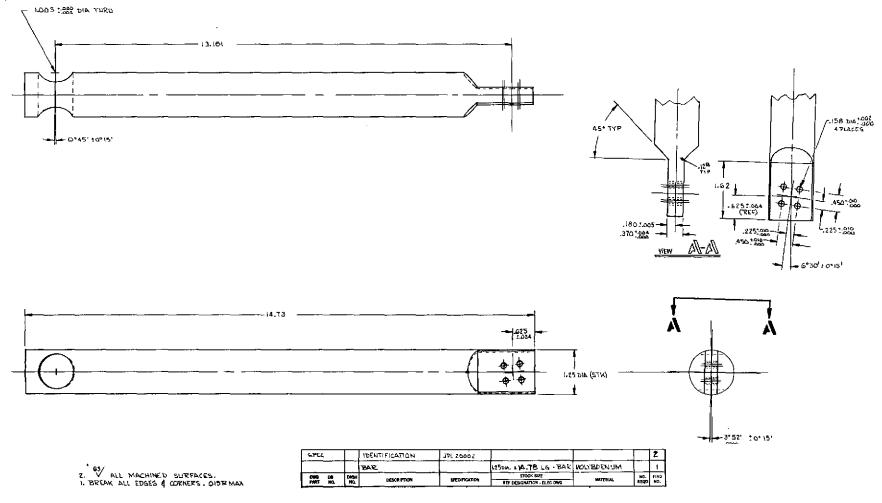


Fig. C-42. Bar, bus transition (LH)

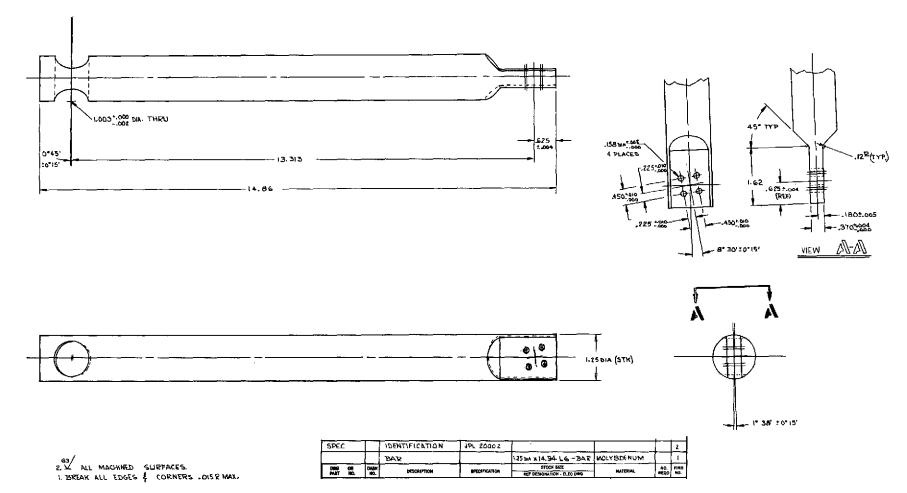
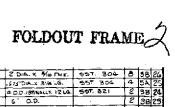
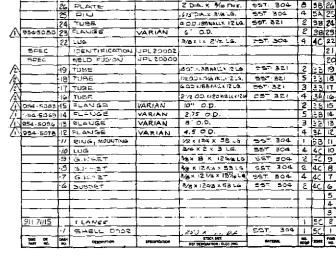


Fig. C-43. Bar, bus transition (RH)





,—.50 ^{Q.}

--406

- - 6 EXTERIOR SURFACE OF DOOR TO BE TRACED WITH CODLING COIL.
 - A DIMEMSION 10.875 RTOP OF DOOR ONE PLACE OULY, ALL OTHERS MOUNTING FLALGES 17.85
 - A REMOVE ALL BURRS & SHARP EDGES
 - MACHINE FINISH D
 - TUBE SALES 2211 TUBEVIAY
 - A VARIAU ASSOCIATES GIL HAUSEN WAY.
 PALO ACTO, CALIF.
 (CONFLAT DISA VACUUM FLANGES)

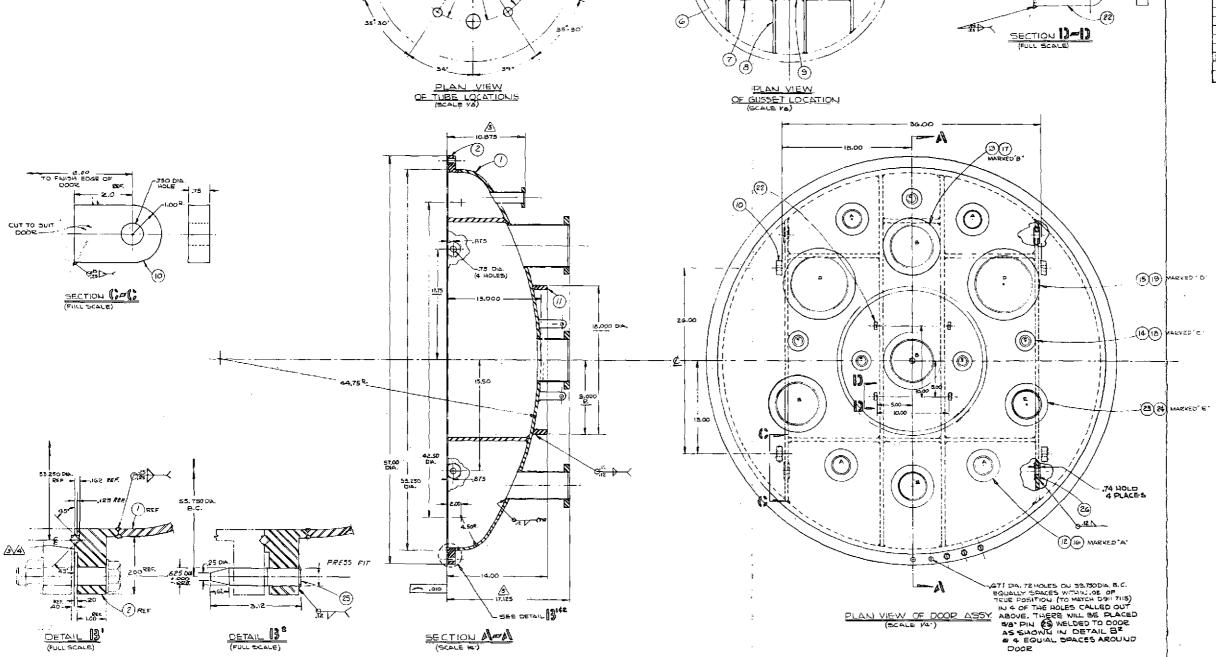


Fig. C-44. Door assembly - 100-kW erosion loop

FOLDOUT FRAME

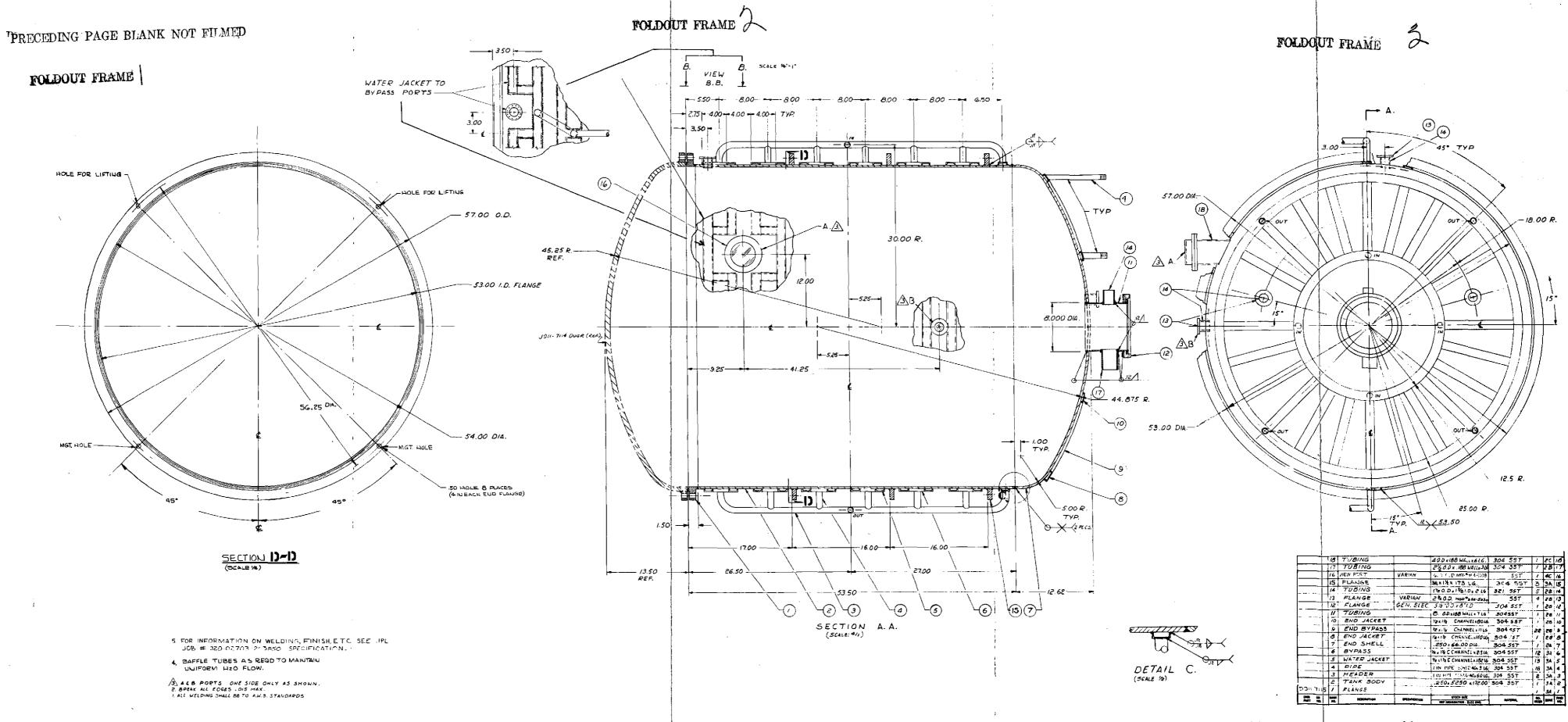


Fig. C-45. Vacuum tank assembly - 100-kW erosion loop

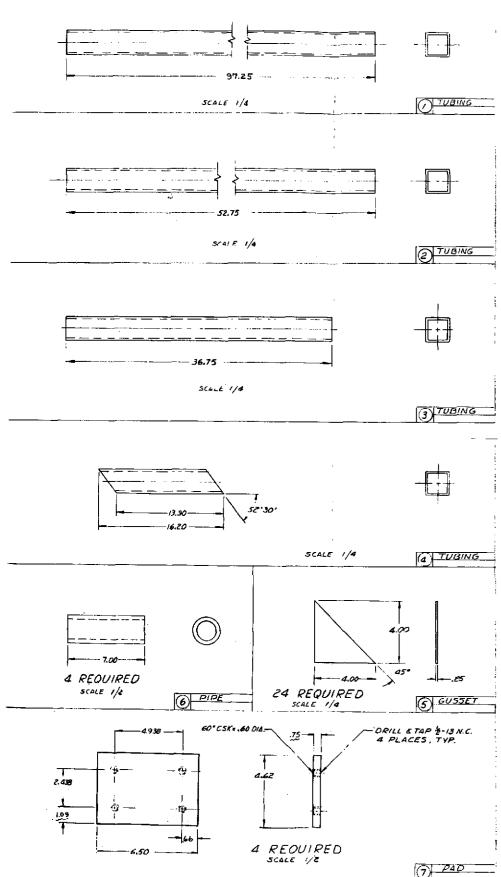
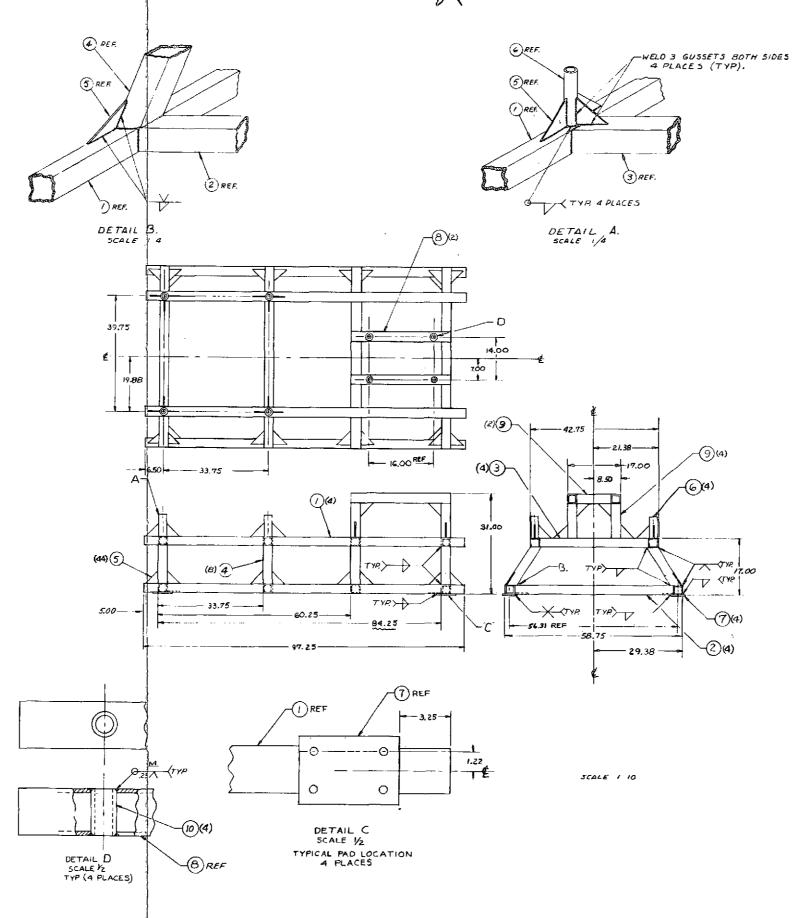
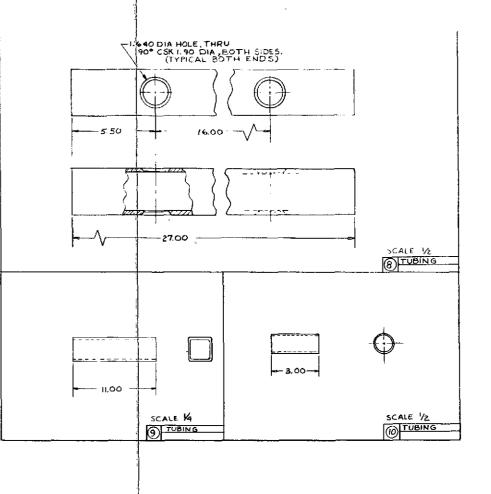


Fig. C-46. Frame, weldment, vacuum tank support





ALL JUINTS OF SQUARE TUBING TO BE WELDED ALL AROUND.
ALL WELDS TO BE 1/4 WIDE AND HAVE A ROOT FEMETRATION
OF 3/6 THE FULL LENGTH OF THE JOINT.

REMOVE ALL BURRS & SHARP EDGES ..

DESCRIPTION	PE	CHICADON	REF DESIGNATION - ELEC DING	POXTEXNS.	ES.	Direct.
TU3:04 5	Q 1/4	WALL	3.3.974 LG	TEEL	.4	.69.
i I		į	3 x 2 x 54. LG	i	3	53
. 11		ł	3 × 3 × 38. LG	1	3	58
TUBINGS	5Q V4	WALL	3 x 3 x 18 LG	STIEL	6	68
GUSSET			1/4×4×4	CR.5.	44	68
TUBING, ROU	ND		増加ないア LG	S 75.574	4	58
240			€x4 %x6½ LG.	C.Z. 5.	4	5 24
TUBING) SO	2 .1/4 V	NALL		STEEL	4	30
TUBING, S	2. <i>14</i> v	1.66	3x3 x 11 LG	STEEL	6	58
TUBING, ROUN			18 + 4 WALL X JLG	C.R.S	4	6 A

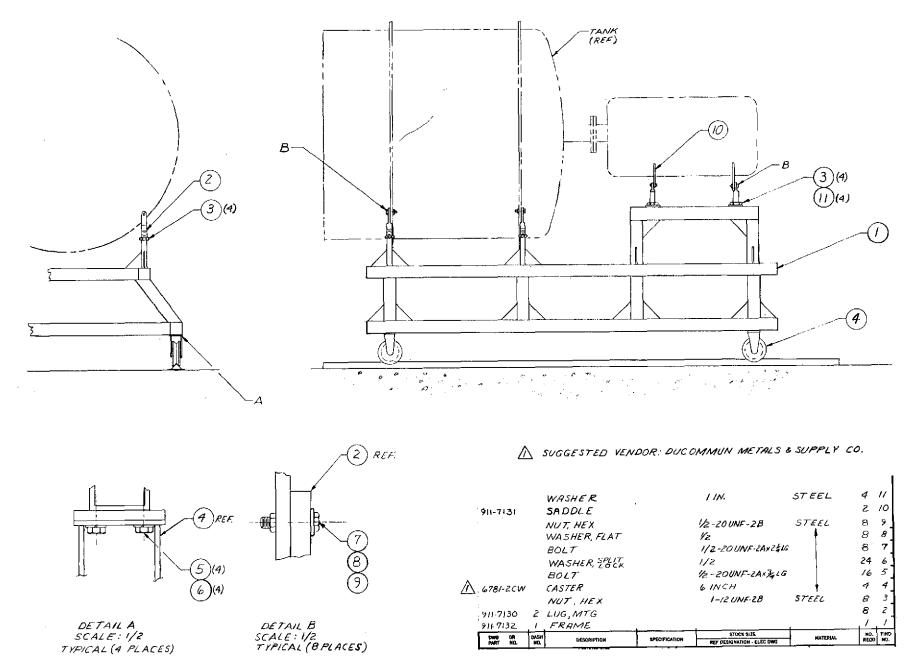


Fig. C-47. Frame, assembly

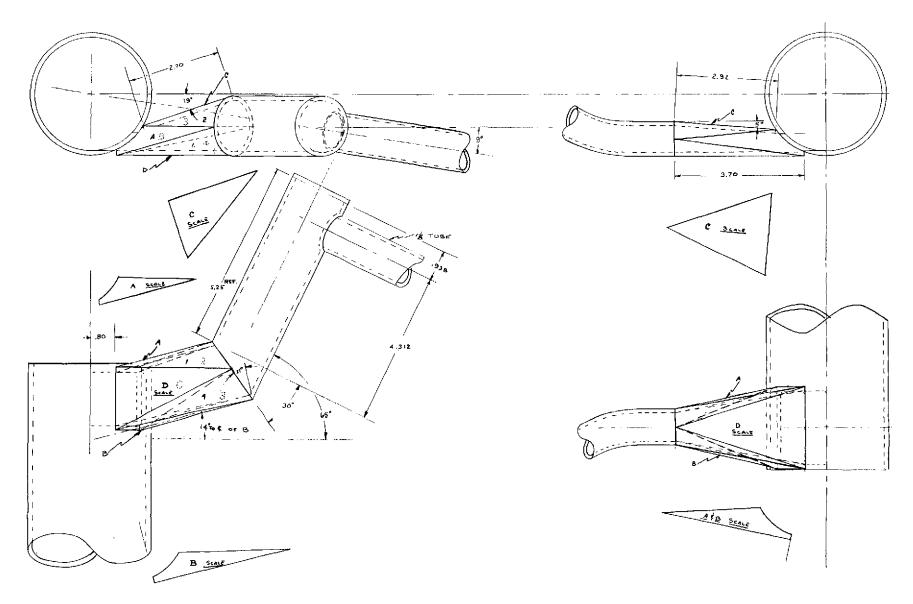
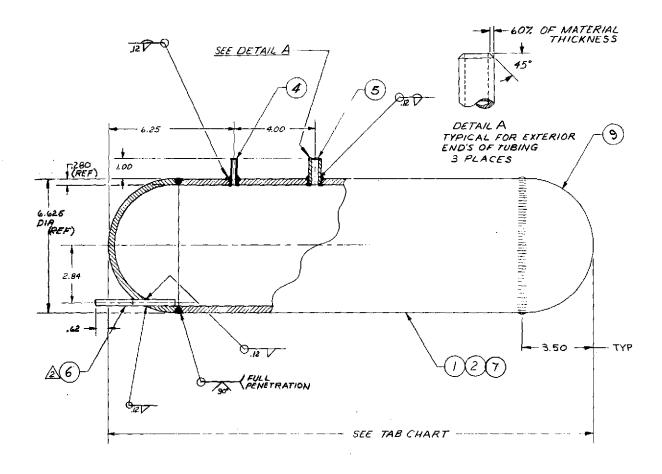


Fig. C-48. Transition pieces, columbium separator



⚠ LENGTH TO BE FURNISHED BY COG. ENGINEER.

LOCATE ITEM 6 AS SHOWN, WITH THE BOTTOM TANGENT TO THE INNER WALL OF THE PIPE.

2. REMOVE ALL BURRS AND SHARP EDGES
1. MACHINE FINISH 63/

	TAB CHA	KT.
SYS	DASH NO.	LENGTH
Li	-1	40.00
C.s	-2	31.00
NaK	-3	<u>A</u>

ĺ	-3	-2	-/	DMG OF PART NO.	DASH NO.	DESCRIPTION	SPECIFICATION	REF DESIGNATION - ELEC DWG	MATERIAL	HO. REDD	FIND NO.
ĺ	_		1		-/	PIPE BODY		6"PIPE BULONG	321 CRE5		1
1	-	1	-		-2	PIPE-BODY		6"PIPE, SCHED 40	321 CRES		2
1										1-	3
ļ	1	1	1		-4	TUBING		5/60.D. 144 LONG	321 CRES		4
Ţ	1	1	1		-5	TUBING		50.D. 194 LONG	321 CRES		5
_	2	2.	2		-6	TUBING		5/60.D . 031 WALL 1 LONG 5/60.D . 262 WALL	32/ CRES	1	6
Δ	1	-	-		-7	PIPE - BODY		6 PIPE- SCHO 40 x A 14	321 CRES	1	7
ſ											a
Ì	2	2	2			CAP, PIPE		G" PIPE SCHED 40	321 CRES	1	9
1			-					 		_	10
ſ	_			SPEC		WELDING	15r 50000				Ü
1		l	1	SPEC	- 1	IDENTIFICATION	JPL 20202	Į.			12

Fig. C-49. Sump weldment - cesium, lithium and NaK (tabulated)

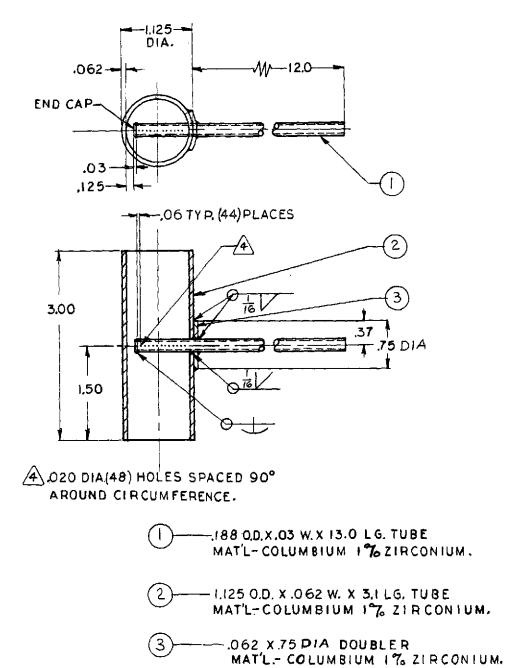


Fig. C-50. Sketch, desuperheater, erosion loop

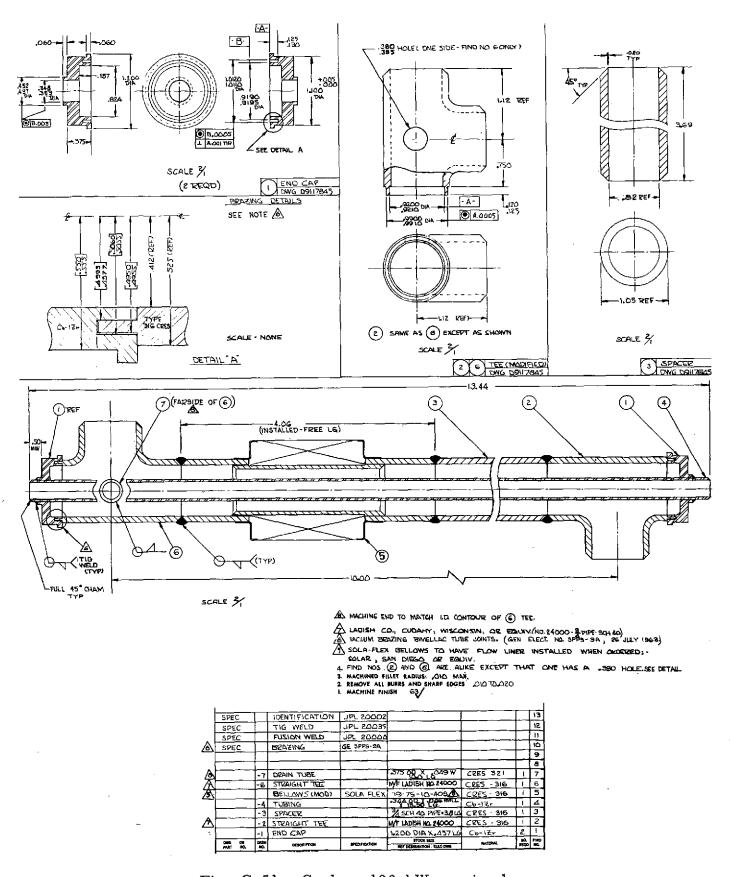


Fig. C-51. Cooler, 100-kW erosion loop

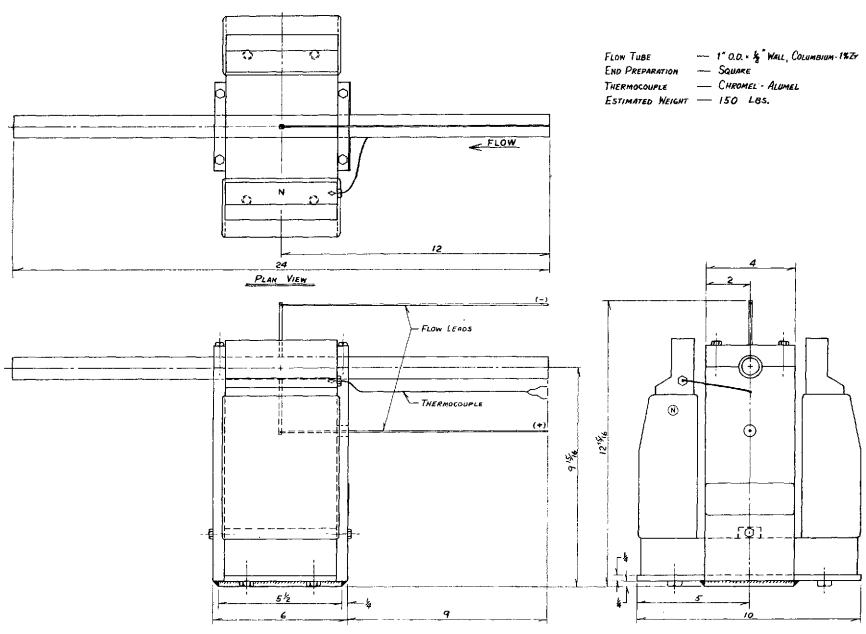


Fig. C-52. Flowmeter FM-14

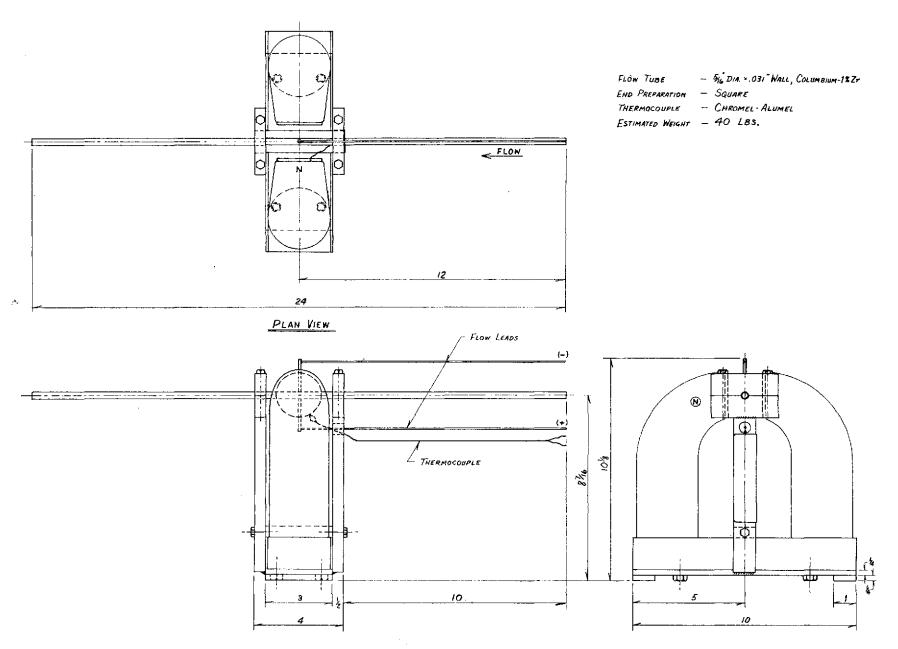


Fig. C-53. Flowmeter FM-12

APPENDIX D

CESIUM-LITHIUM LOOP OPERATING CHARACTERISTICS

The operating characteristics of the Cs-Li loop were determined by modeling the performance of the major components (Li pump, Cs pump, Li heater, Cs condenser, Cs subcooler, bypass valve) and combining the relations together with the hydraulic and heat loss characteristics of the system. The CAL program resulting from this effort is given in this appendix. The results of variation of key parameters over a range of interest is summarized in Fig. D-1. The independent variables are taken to be the pump voltages E_1 and E_2 , the heat rejection rate Q, the NaK pump current I, the lithium heater voltage E_3 , and the number of turns opening of the bypass valve N. The variations of the condenser temperature T_2 , mass ratio r_c , NaK temperature T_3 , and lithium temperature T_1 are shown for individual variations in the independent parameters. At the design point of:

$$T_1 = 1800$$
°F

$$T_2 = 1300 \, ^{\circ} F$$

$$T_3 = 900^{\circ}F$$

$$C_1 = 0.02$$

$$r_c = 10$$

the control variables should have the following settings (from the figure):

$$E_1 = 304 \text{ V}$$

$$E_2 = 283 \text{ V}$$

$$E_3 = 11.3 \text{ V}$$

$$Q = 24.3 \text{ kW}$$

$$T = 18.3 A$$

$$N = 0.45 \text{ turns}$$

The effect of variations of the control parameters from the design point can be determined by following the appropriate curve.

NOMENCLATURE

A1	$^{lpha}{}_{ m B}$	fraction of cesium in lithium at nozzle exit
A2	A	area of loop at highest temperature, ft ²
В1	$^{\beta}{}_{\mathrm{B}}$	fraction of lithium vapor in cesium at nozzle outlet
*C1	C ₀	fractional lithium carryover
C2	Cp _{cs} 10	specific heat of cesium liquid and vapor at T ₁₀ , Btu/lb°F
C3	$^{\mathrm{Cp}_{\mathrm{Li}_{\ell}}}$	specific heat of lithium at T ₁₂
C4	Cp ₁₉	specific heat of lithium and cesium mixture into desuperheater
*Dl	$\Delta p_{ ext{fl}}$	frictional drop in lithium lines, psi
*D2	$\Delta p_{\mathbf{f2}}$	frictional drop in cesium lines, psi
D3	$\Delta T_{ m B}$	drop in bulk temperature in nozzle, °F
El	E ₁	lithium pump voltage
E2	E ₂	cesium pump voltage
E3	E_3	lithium heater voltage
E4	E	emissivity of foil insulation
LI	$^{\rm Lv}{}_{\rm Li}$	latent heat of lithium vapor, cal/g
LZ	$\mathtt{Lv}_{\mathtt{Li}}$	latent heat of lithium vapor, B/lb
L3 .	Lvcs	latent heat of cesium vapor, cal/g
L4	Lvcs	latent heat of cesium vapor, B/lb
Ml	$\dot{ ext{m}}_{ ext{T}}$	total nozzle flowrate, lb/s
M2	$\dot{ ext{m}}_{ ext{Lit}}$	lithium flowrate in nozzle, lb/s
М3	$\dot{ ext{m}}_{ t pl}$	lithium flowrate in pump, 1b/s

NOMENCLATURE (contd)

mass flowrate of dissolved cesium, lb/s M5mass flowrate of lithium vapor, lb/s desuperheater flowrate, lb/s M7 cesium pump flowrate, lb/s M8 number of layers of radiation shielding N1n P0inlet pressure of lithium, psi \mathbf{p}_{0} P1nozzle inlet pressure, psi p_1 P2condenser pressure, atm p_{12} P3condenser pressure, psi p_{12} heat input from lithium pump, kW QΙ Q_1

cesium flow in nozzle, lb/s

- Q2 Q, heat input from cesium pump, kW
- Q3 Q3 heat input from lithium heater, kW
- Q4 Q₄ radiant heat loss, Btu/hr
- Q5 Q5 heat transfer in subcooler
- Q6 Q_4 radiant heat loss, kW
- Q7 Q_R heat rejection date required, kW
- R1 PLi lithium density, lb/ft³
- *R2 r mass ratio of lithium to cesium in nozzle
- R3 ρ_{cs} cesium density, B/ft³
- R4 ρ_{Li} lithium density, g/cm³

M4

NOMENCLATURE (contd)

R 5	ρ _{cs}	cesium density, g/cm ³
*T1	T ₁	nozzle inlet temperature of lithium, °F
*T2	T ₁₂	condenser temperature, °F
Т3	T ₃₄	potassium low temperature, °F
T4	T ₁₂	condenser temperature, °K
Т5	Tl	nozzle inlet temperature, °F, °C
Т6	^T 19	temperature into desuperheater, °F
Т7	^T 10	nozzle exit temperature, °C
Т8	T ₁₂	condenser temperature, °C
Т9	T ₁₀ .	nozzle exit temperature, °K
X1	$^{\mathrm{T}}$ c	temperature of vacuum chamber
X2		temperature factor
X 3		temperature factor
X4		temperature factor
X 5	^T 10	nozzle exit temperature, °F

Cs-Li LOOP PERFORMANCE PROGRAM

```
1:00 DEMAND C1:T2:T1:R0:T3:R2:A3
1:01 T8:(T2:92:0)/1:8+273:16
1 . 011 A2 - 10 . 12
1.012 N1#15
                                                                                     4
1:013 X1:800
1.014 E0a.15
1.02 PZ=10a(3.3629-(3617.76/74)+0.16005+L0G10 (74))
1.03 P3e14.696#P2
1.031 V1e498+P04.288/(P34.178#R24.443)
1.04 M1e.00381*(P04.90)*(R24.47)
1.06 M3*M2*(1.0*C1)
1.07 T5*(71-32.0)/1.8
1-08 R4=-124+(5-306/(10-43-))*(2900-T5)4-5+(4-135/(10-45-))*(2900-T5)
 1.09 R1=62.4*R4
1+11 M4#M1/(1+R2)
1-11 Dramary 14-65 / (R24-515*P34-431)
1.13 A1.(1.985.PQ4.531.P34.889)/(1045)
1.14 81=(.00292*POA:443*R2A:0973)/(P341:02)
1.15 X5.T1.D3
1.16 M5.A1.M2
1+17 TopT3+100.
1:18 M6:81#(M4:M5)
1:19 Y7a(x5-32)/(1:8)
1:20 G2e:0684*(8:032+77)/1045+(7:994+7742)/1048
1.21 TSKT4-273
     C291.0577-(1.2152.78/1044)+(5.3477.7842/1048)
 1:23 C4:(C2)/(1+C1+R2)+(C1+R2+C3)/(1+C1+R2) (3)
1.84 TPaT7+273
1:65 Lin5061-2-(1-19/3173)A-3725
1.26 L2e1.8:L1
1,27 L30147:120(1-T4/2043)4+3547
1.28 [6.1.8.13]
1.23 17:116.02.(XB-T2).416.L2.C1.M5.L4.M2.C1.003.(X8-12)./(C4.(T2.16).L4).
1:30 MBaM4+M7
     ESa.4344(2.495a(1770~T8)4.5)/(1042)4(2.083a(1770=T3))/(1046)
1032 R3462044R5
 1:381 Ufr:2419:10a(5:41921:155:991/(TB:273):1:61506eL0GIO(T5-273))
1.3811 U1=U1/3600
1.322 U1=(11.47*M342)/(R1)>((26.6+115*U14.25)/(M34.20))
1.383 E1. ((PO.P3+D1) +R1)/(-.0347=M3.00274+R1))4.5
 1:324 U2#; 2419×104( -84005+205 -902/T4 - :27958 + L8610 T4)
1.3841 UZ.UZ/3600
 1-325 D264-910164+U23-25+M861-75/R563+46-163+M402/R5+2-34-164-0U26
         .25 = M4 & 1 . 75/35
 1.326 02.02/62.4
 1+33 E2=(((P0+P3+D2)+R3)/(+,3974M8++0022*R3))A+9
1034 Q1 # (4.5 # E1 a 1.72)/(10 a 4)
1034 Q20 (1039 CE2 a 1.72)/(1E4)
1.3%2 X24(M7*C2)+(M2*C1*C3*M7)/(M8)
         X3+T2-100+1.005+(Q2)/((M8+C2)+(M2*C1+C3))
 1.35 G2.(1.39.E241.72)/(1044)
 1+351 L5=147+12+(1+(T5+273)/(2043))4+3547
1.352 L6:1.5.5
1:353 C5:1.0577*(1.2152+75/1E4)*((5:3427*T5:22)/1E8)
 1.354 C6=: 0684-(8.032+T5)/1E5+(7.996+T5+2)/1E8
1.355 X6=T1+(1/((1=A3)+(R2+(1+C1)))-(A3/(1-A3))+((1/(R2+(1+C1)))+1
))+(L6/C5)+((C6/(R2+(1+C1)*C5))+(C1/((1+C1)*C5)))+(T1-X3)
 1.36 Q3=.947+M3+C5+(X6-T1+Q3)=Q1
1.361 E30(11.22003)0.5
1.37 0.0170.E4.02x(([].460].40(X1.460)04)/(N1.1E8)
 1-38 X85(M7+C8)+(M2+C1+C3+M7)/(M8+M7)
1:40 X4:16:100:02/X2
 1:41 Q5eX2*(X3=X4)++947
 +42 D6+04/3413
$1,43,07a01+32+03+96+08 2000
 1:431 U21/(:0035:M81:408::000243)
21:438 X60(07-Q5)*(3413)/(*6554U)?
```

Cs-Li LOOP PERFORMANCE PROGRAM (contd)

```
1.433 M9#1
1.434 X7*(Q7*Q5)*(.947)/(.21*M9)
1.434 X7*(Q7*Q5)*(.947)/(.21*M9)
1.435 X8*(Q5*.947)/(.21*M9)
1.436 X9*(X7)/L9G(1/(1*(X7)/(T2*T3*X8)))
1.437 M9* IF A55((X9*X6)/X6)**Q1 THEN (14;*1)*((X5*X9)/X5)*M9* ELSE

IF A85((X9*X6)/X6)**Q1 THEN M9 ELSE M9
1.438 T0 STEP 1.434 IF AB5((X9*X6)/X6) > 001
1.439 I**(.7**M3*.74
1.449 TYPE E1.E2.E3,PO,P3,T1,T2,D3,C2,M4,L2
1.441 TYPE X6
1.442 Y7*2930*M7/R3
1.443 K**250*(P0*P3)/(R3*Y7*2)
1.444 N**3***.5/K***.5
1.445 TYPE M1,M2,M3,M5,M6,M7,M8
1.46 TYPE G1,Q2,Q3,Q5,Q6,Q7
1.461 TYPE D1,D2
1.47 T0 STEP 1.00
```

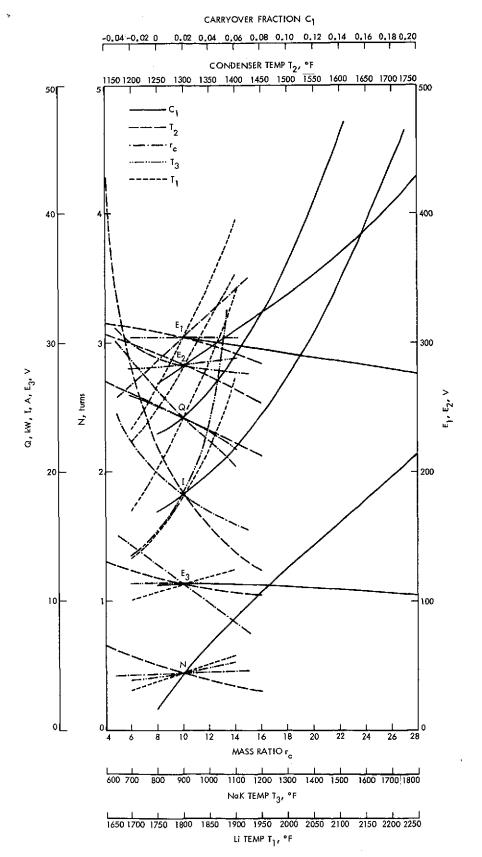


Fig. D-1. Cs-Li loop characteristics